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#### FINAL REPORT

# DEVELOPMENT OF IMPROVED ZINC ELECTRODES FOR SECONDARY BATTERIES

by

A. Himy

prepared for

NATIONAL AERONAUTICS AND SPACE ADMINISTRATION

CONTRACT NAS 3-11830

ASTROPOWER LABORATORY
McDonnell Douglas Astronautics Company
Western Division

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#### ABSTRACT

A new zinc electrode construction was evaluated, based on an inorganic material mixed with zinc oxide, which acted as a binder when the mix was sintered at 850°C. Zirconia was selected over two other inorganic materials; proportions ranging from 2% to 50% were investigated for physical characteristics and from 5% to 20% for electrical characteristics. PbO was investigated as an additive, besides the usual 2% HgO amalgamation. A total of 20 combinations of construction features were electrically tested on three different cycling regimes. In general, zinc shape retention was improved in varying degrees, reflected in longer cycle life over the regular unsintered zinc oxide electrode.

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#### SUMMARY

The objectives of this program are to develop and test particular zinc electrode constructions that may result in long cycle life.

The various fabrication techniques encompass one basic and common feature — the use of a refractory type inorganic material mixed with zinc oxide in a particular ratio and sintered at very high temperatures so as to result in a mechanically strong electrode capable of maintaining its structural integrity during handling and cell assembly. This electrode is expected to perform satisfactorily during electrical testing because of a possible better shape retention resulting from less "slumping."

#### INTRODUCTION

This program consists of two distinct tasks.

Task I covers electrode fabrication techniques and physical characterization. The basic and common feature of the new zinc electrode constructions was the use of refractory type inorganic material (silicate or oxide) mixed with zinc oxide and acting as a binder after sintering the mix at high temperatures. Starting with three different inorganic materials, and several ratios of zinc oxide and inorganic material, the investigation was carried out on pellet-type samples simulating a section of the electrode. Sintering temperatures ranging from 300°C to 1400°C were investigated. The physical characteristics studied were density, absorption, porosity, surface area by BET measurement, and pore size distribution by mercury intrusion. At the

end of this phase, out of all the variables encountered, a selection of 20 combinations was made for use in actual cells for electrical testing on the next task.

Task II covered the testing of approximately 250 cells on three different regimes - 1 hr, 1.5 hr, and 24 hr cycling periods with the first one at 100°C and the others at 25°C.

The cells were first submitted after formation to four deep discharge cycles at various rates ranging from 30 mA to 3 A. Because the test cell was purposely designed to be quickly zinc limited to accelerate failure, the data obtained are indicative only on a relative merit basis. Compared with the control electrode (unsintered zinc oxide), which reached about 500 cycles on the 1.5 hr cycling period, the best electrode among all combinations fully tested completed about 650 cycles. However, the technical performance period of the program was completed before all test data on other combinations were acquired.

The author wishes to acknowledge the valuable contribution of Mr. I. C. Blake, Manager of the Battery Fabrication and Development Department, for the close supervision of the manufacture of cell components and assembly of cells, and of Mr. A. D. Taylor for setting up and following up the cell testing. Special acknowledgement is also given to Mr. G. Boehm who performed the laboratory analytical work and compiled the test data.

#### TASK I - PHYSICAL CHARACTERIZATION

Task I covered electrode fabrication techniques and electrode characterization for physical properties.

The general lines of investigation are as follows:

Three inorganic materials are to be studied. Each is to be blended with zinc oxide in various proportions ranging from 2% to 50% and the mix is to be sintered at a temperature where physical strength of the electrode is attained. The sintering temperature is to range from 300°C to 1400°C. This necessitates making a selection of electrode grid metal (silver melts at 960°C) and, consequently, a selection of the mix process and electrode fabrication technique. In turn, the method of incorporating the additives to be investigated (HgO, PbO) is dependent upon the final temperature selected, since HgO decomposes at 500°C and PbO melts at 888°C.

All phases of this investigation proceeded almost concurrently and are therefore not presented chronologically.

#### Grid Metal Selection

Metals other than silver (melting point 960°C) were first considered for their high melting points, higher than the sintering temperatures of inorganic materials. They were:

Molybdenum: 2610°C Tungsten: 3410°C Tantalum: 2996°C

However, their electrochemical compatibility with zinc must be taken into account.

Potentials of these metals were measured versus a zinc metal strip in various solutions ranging from 30% to 40% pure KOH or zincate saturated KOH at 25°C. The range of values was as follows:

Molybdenum: 0.75 to 0.86 V Tungsten: 0.69 to 0.77 V Tantalum: 0.75 to 0.85 V

Once the metals were zinc plated, all potentials dropped to a few millivolts.

However, when the metals were left in intimate contact with zinc metal in zincate saturated KOH solutions, gassing occurred in varying degrees and continued uninterrupted for the duration of the test (68 hours).

Following is a list of metals in decreasing order of reaction after 68 hours exposure to KOH and zinc:

Metal	Gassing	Metal Weight Loss	Zinc Weight Loss
Tungsten	Heavy	0%	5 9%
Molybdenum	Fine	0%	14%
Tantalum	None	0%	5%

Tantalum showed the greatest ability for the leads to be welded to the collector grid, using parent material. Tungsten was found to be very hard.

Another consideration is the electrical resistance offered by grids made of these metals compared with silver. Their electrical resistivities are:

Molybdenum:  $5.70 \mu\Omega$ -cm Tungsten:  $5.60 \mu\Omega$ -cm Tantalum:  $13.85 \mu\Omega$ -cm Silver:  $1.59 \mu\Omega$ -cm

However, this is a minor cause for rejecting the metal because it is not likely to appreciably affect the electrical performance of the zinc electrode.

Another consideration is the handling of these materials at elevated temperatures. They oxidize very fast and must be handled in special set-ups in inert atmospheres.

In summary, all of these tests showed the unsuitability of the metals considered; the zinc corrosion caused by the metal contact in alkali is certainly the most important factor for rejection.

It appears without going too far in the search for new grid metals that silver remains the preferred material. This justifies the various alternate approaches for sintering processes. Variation of the silver grid structure will be considered rather than variation of the metal.

#### Fabrication Techniques

#### <u>Materials</u>

The three inorganic materials first considered are the following:

Material	$\underline{Code}$
Magnesium silicate complex	OL
Zirconia	$\mathbf{z}$
Magnesia	M

OL is a material previously used on NASA Contract NAS 3-8513\* which showed promising results in terms of cycling performance at 100°C. The zirconia and magnesia were selected on the basis of compatibility with zinc in KOH solution in terms of gassing characteristics and electrochemical stability.

<sup>\*</sup>A. Himy, "Improved Zinc Electrode," Final Report NASA CR-72265, Astropower Laboratory, Missile & Space Systems Division, Douglas Aircraft Company, July 1967.

#### Ratio

The following ratios were considered:

ZnO	Inorganic
98%	2%
90%	10%
80%	20%
65%	35%
50%	50%

However, in an actual cell, it would not be advantageous to go beyond 80/20 because of the excessive decrease in active material amount.

The code adopted for a particular mix is given in the following example: 80/20 Z means 80% ZnO blended with 20% zirconia.

#### Process

#### General

Sintering the mix powder covers a wide range of temperatures that extend from 300° up to 1400°C. Modification of the bond structure may occur at the high temperature range. Therefore, the sintering process will follow two parallel paths.

In the normal process (N), the electrode is first pressed as usual, then sintered at a temperature that must be compatible with the grid metal (no melting or severe distortion due to heat should occur) and with the additives (HgO decomposes at 500°C and PbO melts at 888°C).

In the presintered process (PS), the powder mix is sintered in compacted form, ground fine and sifted. In this step, the sintering temperature can be as high as necessary to create the desired bond structure between particles of different materials.

At this stage two possibilities are offered:

- (a) Blend the additive dry with the mix in the required percentage; press the electrode; then submit it to a relatively low heat treatment (below 500°C because of the presence of HgO) for an extra bond between presintered particles; or,
- (b) Press the electrode first; sinter at the desired temperature; then introduce the additives by a wet process.

However, the possibility (a) was abandoned early in the course of this investigation because the presintered mix failed to develop a bond between particles below 500°C. Consequently, only possibility (b) was adopted.

#### Material Preparation

The preparation of materials and mixes in various percentages involves a long and careful procedure. All blends are done by ball milling with a certain amount of various organic additives for proper processing.

A batch of zinc oxide and inorganic material blend of 1500 grams is mixed with 2000 cm<sup>3</sup> of water to which are added 2% Carbowax, 0.5% dextrine, and 0.01% anti-foam agent. The mixture is then ball milled for 15 hours, then strained through a 325 mesh screen and dried at 105°C for over 72 hours.

The material is then granulated and sifted through -32 to +80 mesh screen in order to keep the size of particle agglomerates in a relatively narrow range.

This general procedure changes very little, only in the quantities of organic additives and water, for each material composition and ratio.

At this point, either the electrode is pressed then sintered, or the powder is sintered then pressed into electrodes. The sintering temperatures are high enough to decompose all organic substances so that the resultant product is purely inorganic.

#### Pellet Fabrication

The physical measurements were done on pellets pressed to the apparent density, thickness, and weight per unit area as those of the final electrode. They were pressed without the use of grid or KT interseparator for the purpose of accurately characterizing the physical magnitudes called out in the work statement, i.e., density, absorption, surface area by the BET method, and pore size by Hg intrusion.

Two sizes were chosen as being practical for the characterization of the physical properties.

Circular pellets 1" in diameter and 0.050" in thickness (identical to electrode thickness) are made for measuring density, porosity, and water absorption.

Square pellets 3/8" x 3/8" x 0.050" are made with the same weight per unit area as the circular pellets for determining surface area by

the BET method and pore size distribution by mercury intrustion because of the maximum size required by the apparatus.

#### Physical Characteristics

Common to all materials and mix ratios are the following measurements and related computations on the 1" diameter pellets.

Before Sintering	
Original diameter	Do
Original thickness	No
Original volume	vo
Original mass	<sup>m</sup> o
After Sintering:	
Diameter	D
Thickness	N
Volume	V
Mass	m
Weight loss percent	W. L. = $\frac{m_0 - m}{m_0} \times 100$
Mass after impregnation with water	m <sup>1</sup>
Water pick-up	$\Delta m = m^{\dagger} - m$
Water absorption %	$a = \frac{\Delta m}{m} \times 100$
Apparent density	$d_a = \frac{m}{V}$
Measured porosity $\%$	$p_{m} = a \cdot d_{a}$
True density (composite)	d <sub>c</sub> (given in Table X)
Calculated porosity %	$p = \frac{d_c - d_a}{d_c} \times 100$

The difference  $\Delta p = p - p_m$  will give the percentage of closed or nonconnected pores, i.e., not accessible to electrolyte.

The shrinkage factor is defined as:

$$\sigma = \frac{V_0 - V}{V_0} \times 100$$

At least two samples per set of conditions were run and averages are presented for the magnitudes defined above for each inorganic material as well as for pure zinc oxide.

The temperatures run in the first stage were 300°C, 500°C, 700°C, 900°C. In the second stage: 1000°C, 1200°C, 1400°C. The sintering time was held constant (1 hour) to avoid introducing another variable.

### Lower Temperature Range

Physical measurements, experimental data and calculated magnitudes, are given in table and graph forms for each material.

Material	Tables	Figures
OL	I, II	1 to 4
Z	III, IV	5 to 8
M	V, VI	9 to 12

Added for reference are Tables VII, VIII and Figures 13 and 14 for sintered pure ZnO.

#### Comments

Weight loss after sintering pellets with material OL and Z is less than 3%, which is approximately the amount of organic material introduced during the ball milling and granulation operations before sintering. For pellets with magnesia (M), the weight loss experienced is greater (when water is added to the mix for ball milling and granulation, magnesia is hydrated). Upon drying at 105°C, only free water is evaporated. Molecularly bonded water is removed only during the high temperature sintering operation. A confirmation of this phenomenon can be found in the good fit of the experimental weight loss percentage with the calculated loss of one water molecule. Selecting the pellets exposed to 900°C for 1 hour and correcting for the loss of organic binders, the data are presented in Table IX. Longer exposure at high temperature would smooth out the small differences if they are not experimental errors.

Pellets are relatively strong in the sintering range of 500° to 900°C with acceptable porosity.

For a given apparent density of the electrode, the water absorption and porosity are constant over a temperature range of 300° to 900°C.

For a given sintering temperature and apparent density, the porosity is constant regardless of the composition of the mix.

TABLE I

Do = 1" PELLET PHYSICAL CHARACTERISTICS

Material: OL

 $\Delta m = m^1 - m$ 

weight =  $\frac{m_o - m}{10ss \%} = 100$ 

			Befor	e Sintering	ing			After	r Sintering	ing		
Material	Ratio	Temp.	N <sub>o</sub> (mils)	V <sub>o</sub> (c. c. )	m o (g)	D (in.)	N (mils)	v (c.c.)	m <sub>(g)</sub> (dry)	m'g) (wet)	<b>A</b> m (g)	Weight Loss %
TO	2/86	300 500 700 900	48.0 48.0 49.0 48.0	0.617 0.617 0.630 0.617	1, 593 1, 585 1, 590 1, 596		48.0 48.0 48.5 48.0	0.617 0.617 0.624 0.617	1.572 1.560 1.566 1.566	disinteg 1.875 1.882 1.893	grated 0.315 0.316 0.323	1.3 1.6 1.5
***************************************	90/10	300 500 700 900	49.0 50.0 51.0 49.0	0.630 0.643 0.656 0.630	1.609 1.599 1.604 1.607		49.0 49.0 49.0 48.0	0.630 0.630 0.630 0.617	1.580 1.569 1.571 1.570	1.879 1.889 1.893 1.873	0.299 0.320 0.322 0.303	1.8 1.9 2.1 2.3
	80/20	300 500 700 900	448.8 48.5 48.5 8.8	0.628 0.624 0.624 0.628	1.600 1.607 1.599 1.600		48.0 48.3 48.3 48.3	0.617 0.621 0.621 0.621	1.571 1.574 1.564 1.562	1.855 1.862 1.859 1.856	0.284 0.288 0.295 0.294	1.8 2.2 2.4
	65/35	300 500 700 900	52.8 50.3 49.5 50.3	0.679 0.647 0.637 0.647	1.572 1.601 1.604 1.604		52.5 50.3 49.3 50.3	0.675 0.647 0.634 0.647	1. 529 1. 551 1. 548 1. 544	1.844 1.830 1.819 1.820	0.315 0.279 0.271 0.276	3.5 3.7 3.7
<i></i>	50/50	300 500 700 900	54.5 53.5 52.5 54.0	0.701 0.688 0.675 0.695	2.027 2.006 1.970 2.019		54.5 53.5 52.5 54.0	0.701 0.688 0.675 0.695	1.973 1.942 1.900 1.944	2. 177 2. 153 2. 116 2. 116 2. 173	0.204 0.211 0.216 0.229	3.6.2.7

$$a = \frac{\Delta m}{m} \times 100$$

 $\mathbf{p} = \frac{\mathbf{d_c - d_a}}{\mathbf{d_c}} \times 100$ 

$$d_a = \frac{m}{V}$$

 $a = \frac{\Delta m}{m} \times 100$   $d_a = \frac{m}{V}$ TABLE II  $D_0 = 1" PELLETS$ PHYSICAL CHARACTERISTICS II

$$p_m = a \cdot d_a$$

Material: OL

 $\Delta p = p - p_{m}$   $\sigma = \frac{V_{o} - V}{V_{o}} \times 100$ 

Material	Ratio	Temp.	a%	da (g/cc)	p <sub>m</sub> %	d <sub>c</sub> (g/cc)	р%	Δ <sub>p</sub> %	σ%	
OL	98/2	300								Disintegrated
		500	20.2	2.53	51.1	5.40	53.2	2.1	0	
		700	20.2	2.51	50.6	5.40	53.5	2.9	1.0	
		900	20.6	2.54	52.3	5.40	52.9	0.6	0	
	90/10	300	18.9	2.51	47.5	5.13	51.1	3, 7	0	
		500	20.4	2.49	50.8	5.13	51.5	0.7	2.0	
		700	20.5	2.49	51.1	5.13	51.4	0.3	4.0	
		900	19.3	2.54	49.1	5.13	50.4	1.3	2.1	
	80/20	300	18.1	2.55	46.0	4.83	47.3	1.3	1.8	
		500	18.3	2.53	46.4	4.83	47.5	1.1	0.5	
		700	18.9	2.52	47.5	4.83	47.9	0.4	0.5	
		900	18.8	2.52	47.3	4.83	47.9	0.6	1.1	
1.	65/35	300 ·	20.6	2.27	46.7	4.45	49.1	2.4	0.6	
		500	18.0	2.40	43.1	4.45	46.1	3.0	0	
		700	17.5	2.44	42.7	4.45	45.1	2.4	0.5	:
		900	17.9	2.39	42.7	4.45	46.4	3.7	0	
	50/50	300	10.3	2.81	29.1	4.12	31.7	2.6	0	
		500	10.9	2.82	30.7	4.12	31.5	0.8	0	
	1	700	11.4	2.81	32.0	4.12	32.0	0	0	
L		900	11.8	2.80	32.9	4.12	32.9	0	0	

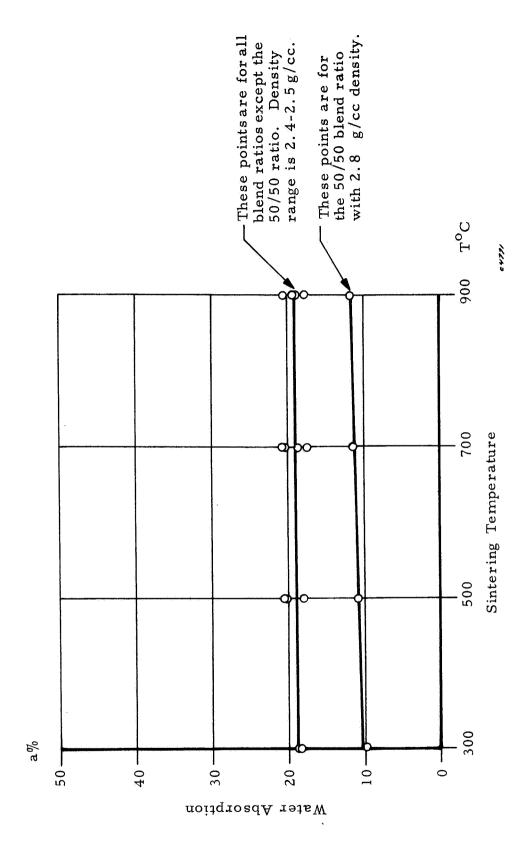
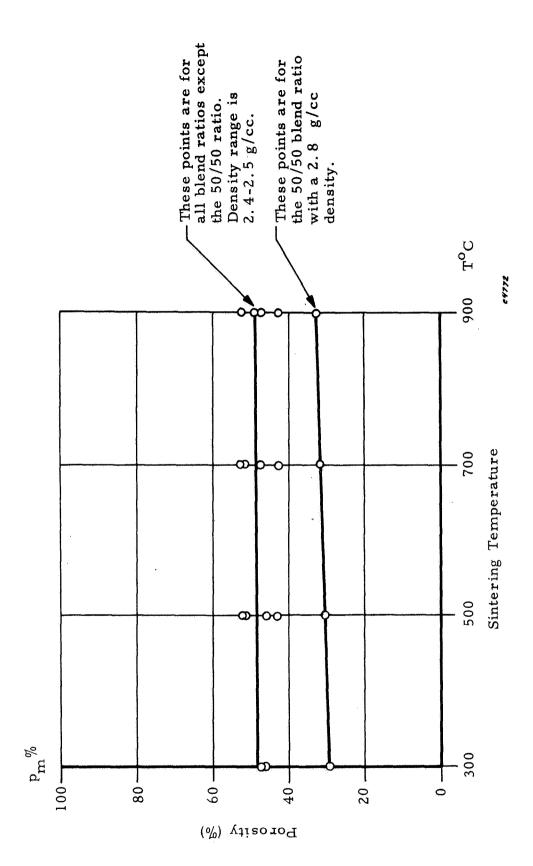
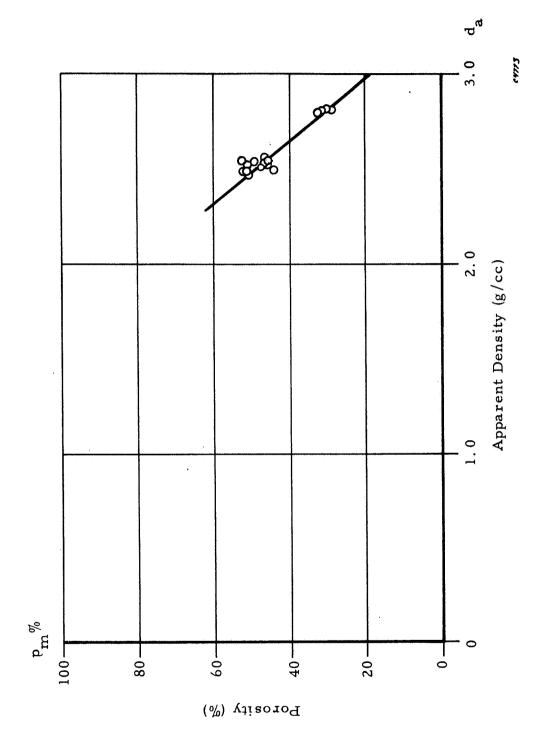


Figure 1. OL-Blends, Absorption vs Sintering Temperature



OL-Blends, Measured Porosity vs Sintering Temperature Figure 2.



OL-Blends, Measured Porosity vs Apparent Density, Sintering Range  $500-900^{\rm o}{\rm C}$ Figure 3.

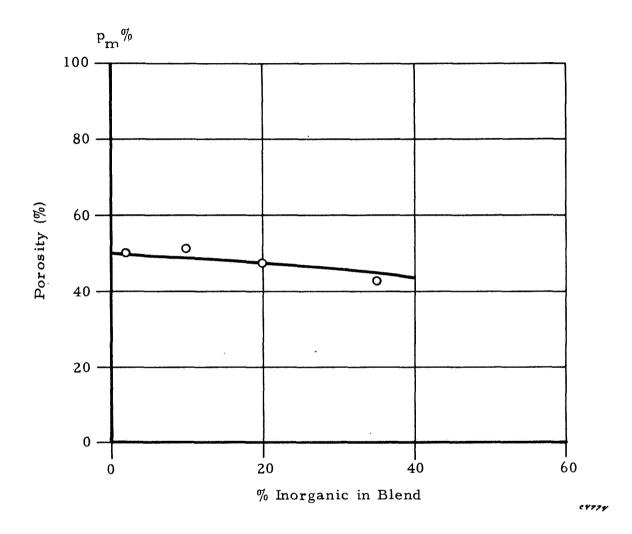


Figure 4. OL-Blends, Measured Porosity vs % Inorganic in Blend Sintered at  $700^{\rm o}$ C with 2.5 g/cc Density

TABLE III

Do = 1" PELLET PHYSICAL CHARACTERISTICS I

Material: Z

 $\Delta m = m' - m$ weight  $\frac{m_o - m}{\log w} \times 100$ 

			Befor	ore Sintering	ing			After	er Sintering	ring		
Material	Ratio	Temp.	N <sub>o</sub> (mils)	V <sub>o</sub> (c.c.)	m o (g)	D (in.)	N (mils)	v (c.c.)	m(g)	m'(g) (wet)	<b>D</b> m (g)	Weight Loss %
Z	98/2	300 500 700 900	49.0 49.0 50.0	0.630 0.630 0.643 0.643	1.590 1.596 1.594 1.594		49.0 49.0 50.0	0.630 0.630 0.643 0.643	1.545 1.548 1.547 1.547	disinte 1.892 1.887 1.896	grated   0.344   0.340   0.349	2.8 3.0 3.0
	90/10	300 500 700 900	49.5 51.0 51.0 50.5	0.637 0.656 0.656 0.650	1.600 1.616 1.598 1.597		50.0 51.0 51.0 51.0	0.643 0.656 0.656 0.656	1.558 1.572 1.553 1.553	disinte 1.909 1.917 1.914	grated 0.337 0.364 0.362	2. 6 2. 7 2. 8 2. 8
	80/20	300 · 500 700 900	49.5 49.5 49.5	0.637 0.637 0.637 0.637	1.606 1.601 1.597 1.602		49.5 49.5 46.5 49.0	0.637 0.637 0.598 0.630	1.569 1.565 1.559 1.563	disinte 1.903 1.858 1.904	grated 0.338 0.299 0.341	2.3 2.4 2.4
	65/35	300 500 700 900	50.5 49.0 49.5 50.0	0.650 0.630 0.637 0.643	2.275 2.275 2.276 2.276		50.0 49.0 49.5 49.5	0.643 0.630 0.637 0.637	2. 225 2. 221 2. 217 2. 213	2. 434 2. 430 2. 429 2. 428	0.209 0.209 0.212 0.215	2.2 2.6 2.8
	50/50	300 500 700 900	49.5 48.0 50.5 47.5	0.637 0.617 0.650 0.611	1.613 1.604 1.606 1.595		49.0 47.5 50.0 47.0	0.630 0.611 0.643 0.605	1.572 1.557 1.560 1.548	disinte 1.862 1.887 1.850	grated 0.305 0.327 0.302	2.9

$$a = \frac{\Delta m}{m} \times 100$$

$$d_{a} = \frac{m}{V}$$

$$p = \frac{d_{c} - d_{a}}{d_{c}} \times 100$$

$$\Delta p = p - p_{m}$$

$$p_{m} = a \cdot d_{a}$$
Material: Z
$$\sigma = \frac{V_{o} - V}{V_{o}} \times 100$$

Material	Ratio	Temp.	a%	d <sub>a</sub> (g/cc)	p <sub>m</sub> %	d c (g/cc)	р%	Δp%	σ%
Z	98/2	300				5.47			Disintegrated
		500	22.2	2.46	54.6	5.47	55.1	0.5	0
		700	22.0	2.41	52.9	5.47	56.0	3.1	0
		900	22.6	2.41	54.3	5.47	56.0	1.7	0
	90/10	300	_			5.47		_	Disintegrated
!		500	21.4	2.40	51.4	5.47	56.2	4.8	0
		700	23.4	2.37	55.5	5.47	56.7	1.2	0
		900	23.3	2.37	55.2	5.47	56.7	1.5	0
	80/20	300			_	5.47			Disintegrated
		500	21.6	2.47	53.1	5.47	55.1	2.0	0
		700	19.2	2.61	50.0	5.47	52.3	2.3	2.3
		900	21.8	2.48	54.1	5.47	54.6	0.5	1.1
•	65/35	300	9.4	3.46	32.5	5.48	36.9	4.4	1.1
		500	9.4	3.52	33.2	5.48	35.7	2.5	0
		700	9.6	3.48	33.3	5.48	36.5	3.2	0
		900	9.7	3.47	33.8	5.48	36.6	2.8	0.9
	50/50	300			_	5.48			Disintegrated
		500	19.6	2.55	49.9	5.48	53.5	3.6	1.0
		700	21.0	2.43	50.9	5.48	55.7	4.9	1.1
		900	19.5	2.56	49.9	5.48	53.3	3.4	1.0

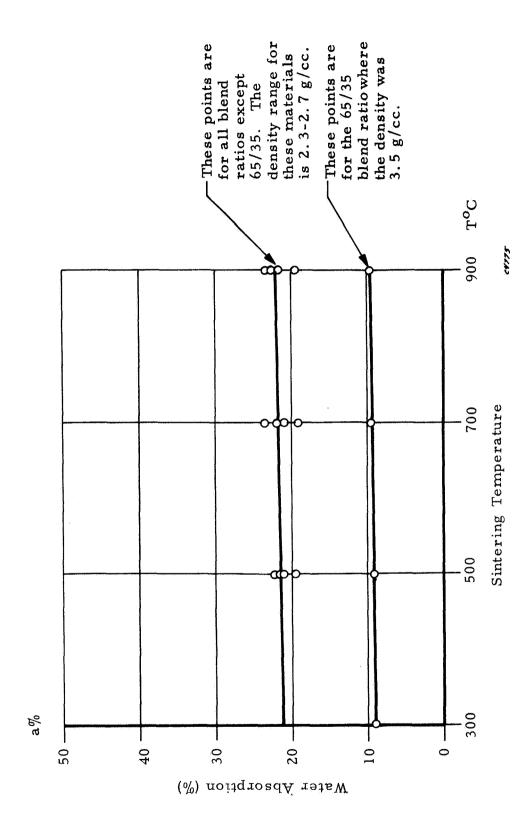
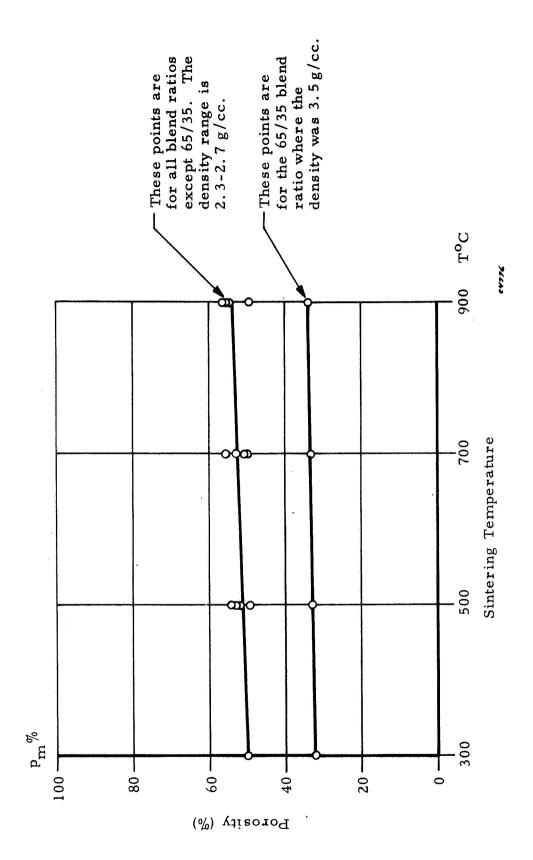


Figure 5. Z-Blends, Absorption vs Sintering Temperature



Z-Blends, Measured Porosity vs Sintering Temperature Figure 6.

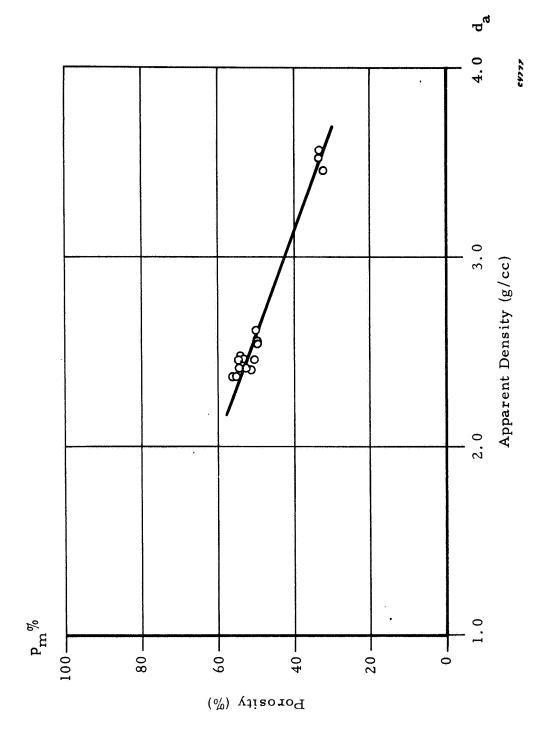


Figure 7. Z-Blends, Measured Porosity vs Apparent Density, Sintering Range 500-900°C

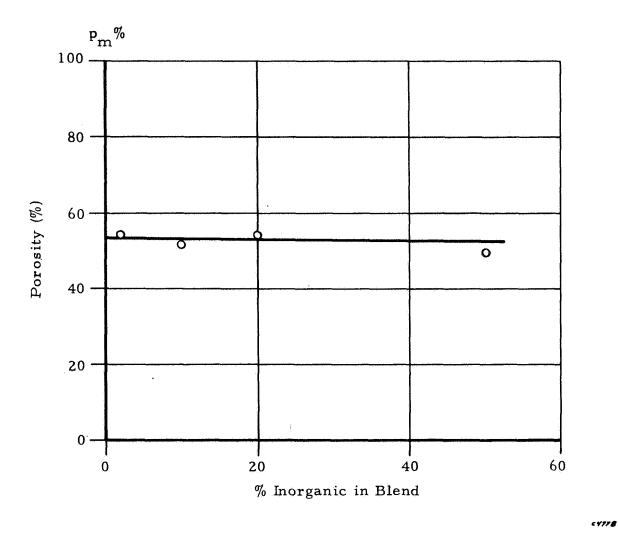


Figure 8. Z-Blends, Measured Porosity vs % Inorganic in Blend - Sintered at 700°C with 2.5 g/cc Density

TABLE V

D<sub>o</sub> = 1" PELLET PHYSICAL CHARACTERISTICS I

 $\Delta m = m' - m$   $\frac{51}{\log s} \frac{m_o - m}{m_o} \times 100$ 

Material: M

			Before	re Sintering	ring			After	Sintering	ng		
Material	Ratio	Temp.	No (mils)	V <sub>o</sub> (c.c)	m o (g)	D (in.)	N (mils)	V (c.c.)	m(g)	m'(g) (wet)	∆m (g)	Weight Loss %
M	98/2	300 500 700 900	49.0 49.0 50.0 50.0	0.630 0.630 0.643 0.643	1.607 1.615 1.610 1.603	1 1	48.0 49.0 48.0 49.0	0.617 0.630 0.617 0.617 0.630	1.572 1.570 1.563 1.563	disinte 1. 899 1. 903 1. 900	isintegrated . 899   0.329 . 903   0.340 . 900   0.347	2.2 2.9 3.1
	90/10	300 500 700 900	48.5 49.0 49.5 48.5	0.624 0.630 0.637 0.624	1.598 1.596 1.599 1.597		49.0 49.0 48.0 48.0	0.630 0.630 0.617 0.617	1.574 1.522 1.507 1.546	disintegrated disintegrated 1.846   0.339 1.827   0.281	grated grated 0.339 0.281	1.5 5.8 3.2
	80/20	300 500 700 900	48.5 49.8 49.8	0.624 0.641 0.641 0.639	1, 593 1, 648 1, 623 1, 628		48.5 49.5 49.5	0.624 0.637 0.637 0.633	1.487 1.510 1.459 1.456	1.750 1.836 1.799 1.792	0.263 0.326 0.340 0.336	6.7 8.4 10.1 10.6
	65/35	300 500 700 900	50.5 .50 51.0 50.0	0.650 0.643 0.656 0.643	1.750 1.744 1.749 1.744	, a a a a	50.5 50.0 49.0 50.0	0.650 0.643 0.630 0.643	1.683 1.565 1.549 1.533	1.888 1.859 1.835 1.818	0.205 0.294 0.286 0.285	3.8 10.3 11.4 12.1
	50/50	300 500 700 900	51.5 51.5 51.0 51.0	0.662 0.662 0.656 0.656	1.503 1.507 1.508 1.504	0.997 $0.982$	51.5 50.5 50.5	0.662 0.646 0.650 0.620	1.453 1.273 1.241 1.216	1.653 1.595 1.572 1.545	0.200 0.322 0.331 0.329	3.3 15.5 17.1 19.1

$$a = \frac{\Delta m}{m} \times 100$$

$$d_a = \frac{m}{V}$$

$$p_m = a \cdot d_a$$

Material: M

$$p = \frac{d_c - d_a}{d_c} \times 100$$

$$\Delta p = p - p_m$$

$$\sigma = \frac{V_o - V}{V_o} \times 100$$

Material	Ratio	Temp. °C	a%	d <sub>a</sub> (g/cc)	p <sub>m</sub> %	d <sub>c</sub> (g/cc)	р%	<b>∆</b> p%	σ%
M	98/2	300	<del></del>	_	· <b>_</b>	5,41		_	Disintegrated
		500	21.0	2.49	52.2	5.41	53.9	1.7	0
	ı	700	21.8	2.53	55.1	5.41	53.2	1.9	4.0
		900	22.3	2.47	55.1	5.41	55.1	0	2.0
	90/10	300	-		_	5.20	_	_	Disintegrated
		500	-	-		5.20	<del></del>	-	Disintegrated
	:	700	22.5	2.44	54.9	5.20	54.9	0	3.1
		900	18.2	2.51	45.5	5.20	51.8	6.3	1.1
	80/20	300	17.7	2.38	42.1	4.95	51.9	9.8	0
}		500	21.6	2.37	51.2	4.95	52.1	0.9	0.6
		700	23.3	2.29	53.4	4.95	53.7	0.3	0.6
		900	23, 1	2.30	53.1	4.95	53.5	0.4	0.9
:	65/35	300	12.2	2.59	31.5	4.62	44.0	12.5	0
		500	18.8	2.43	45.7	4.62	47.3	1.6	0
		700	18.5	2.46	45.4	4.62	46.8	1.4	4.0
		900	18.6	2.38	44.3	4.62	48.4	4.1	0
	50/50	300	13.8	2.19	30.2	4.33	49.3	19.1	0
		500	25.3	1.97	49.8	4.33	54.5	4.7	2.4
		700	26.7	1.91	50.9	4.33	55.9	5.0	0.9
		900	27. 1	1.96	53.1	4.33	54.7	1.6	5. 5

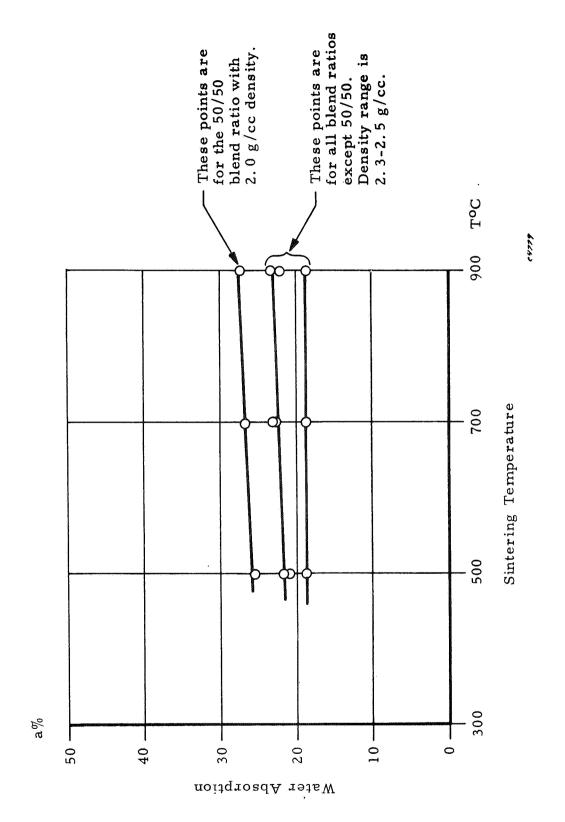


Figure 9. M-Blends, Absorption vs Sintering Temperature

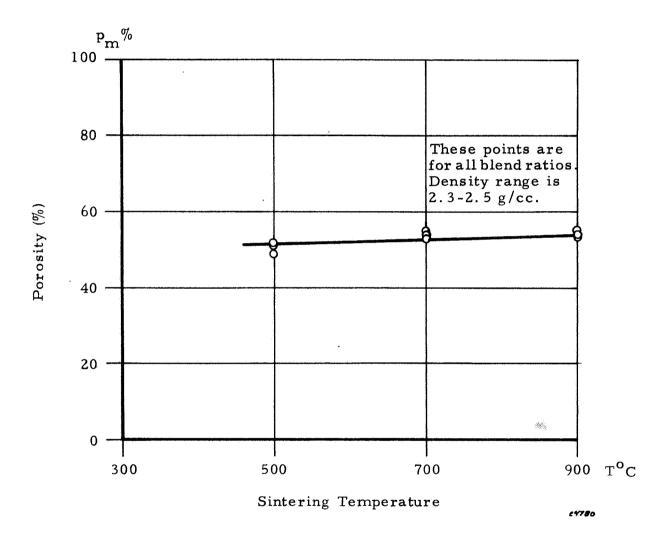


Figure 10. M-Blends, Measured Porosity vs Sintering Temperature

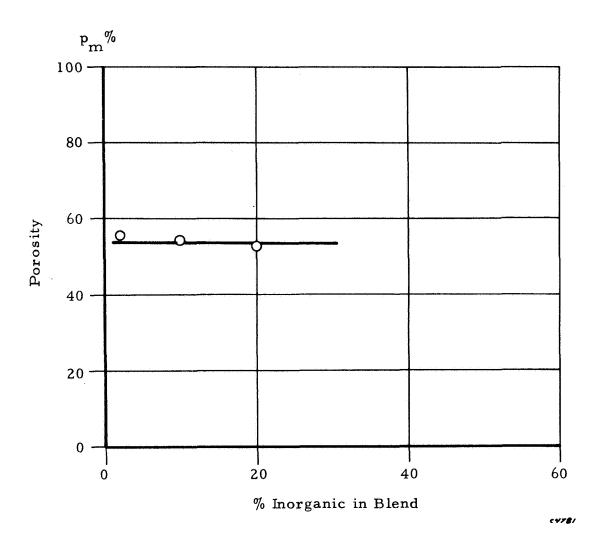


Figure 11. M-Blends, Measured Porosity vs % Inorganic in Blend-Sintered at 700°C with 2.3-2.5 g/cc Density

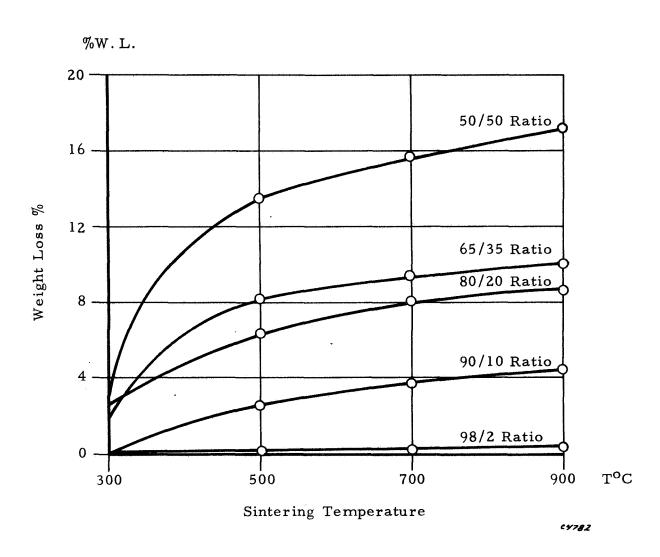


Figure 12. M-Blends, Weight Loss vs Sintering Temperature

TABLE VII

ZnO Material:

**н** ^m = m' - m E 11

x 100

e B weight loss %= 1" PELLET PHYSICAL CHARACTERISTICS ρί

Weight Loss % 1.0.1. 0.351 0.355 0.329 disintegrated 1.929 0.351 1.934 0.355 1.904 0.329 (g) m'g) (wet) After Sintering 1, 579 1, 578 1, 579 1, 575  $m_{(g)}$ 0.643 0.643 0.643 0.617 (c.c) > (mils) 50.0 50.0 50.0 48.0 Z υ (in.) 1.596 1.594 1.598 1.597 m (g) Before Sintering 0.643 0.643 0.643 0.630 (c.c.) (mils) 50.0 50.0 50.0 49.0 z° Temp. 300 500 700 900 100/0 Ratio Material ZnO

x 100 × - pm ا م > leg Ö 0 α, 11 0 უ<sup>თ,</sup> d V ij 11 Q, b Do = 1" PELLETS PHYSICAL CHARACTERISTICS II ZnOTABLE VIII Material:  $a = \Delta m \times 100$ ಧ E #|> ď 11 ಇ ь

100

Disintegrated % 2 0 0 b  $^{0}$ d 0.5 I 0 0 < 55. 1 ~ 3  $\mathbf{p}_{\mathbf{d}}^{\prime\prime}$ 55. 53.  $d_{\rm c}^{\rm d}$ 5.47 5.47 5.47 47 īζ. 55.2 54.6 % 3 53. P<sub>m</sub>  $d_{\mathbf{a}}$ 45 2.46 55 5 2 'n 6 a% 22. 22. 20. Temp. 500 700 006 300 100/0 Ratio Material ZnO

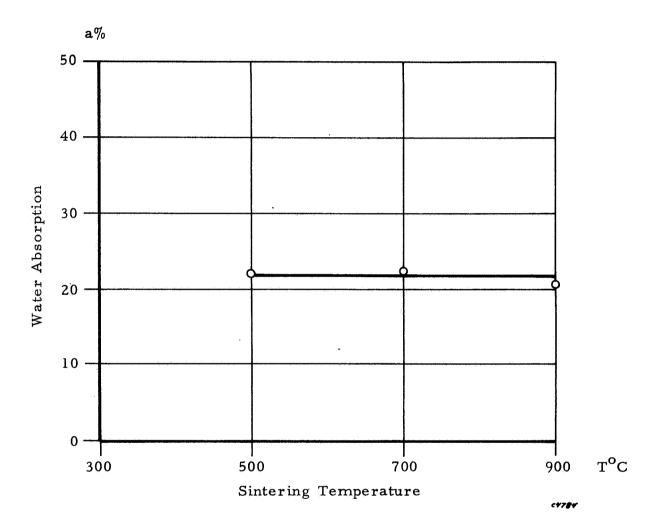


Figure 13. 100% ZnO, Absorption vs Sintering Temperature

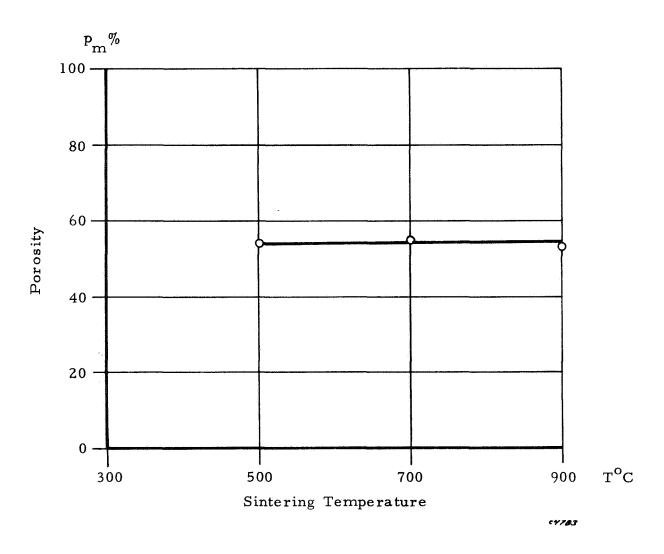


Figure 14. 100% ZnO, Measured Porosity vs Sintering Temperature

# TABLE IX WEIGHT LOSS OF PELLETS WITH MAGNESIA

# . - fraction of Magnesia in the original mix before gir

 $\mu$  = fraction of Magnesia in the original mix before sintering. The calculated weight loss percentage is then:

W. L. % = 
$$\frac{18 \mu}{40.3 + 18 \mu} \times 100$$

Weight Loss

		Exp	perimental
Magnesia Fraction	Calculated	Total	Corrected for Organic Loss
0.50	18.3%	19.1%	17.1
0.35	13.4	12.1	10.1
0.20	8.3	10.6	8.6
0.10	4.3	5.8	3.8
0.02	0.9	3.1	1.1

### TABLE X

### TRUE DENSITY

If  $\zeta$  is the fraction of ZnO (true density 5.47) in a mix of ZnO and inorganic material of true density  $d_i$ , the true density of the composite mix  $d_c$  is related to the other densities by the formula:

$$\frac{1}{d_c} = \frac{\zeta}{5.47} + \frac{1-\zeta}{d_i}$$

The following table gives all composite densities for the selected materials and rations to be investigated.

	Ratio	98/2	95/5	90/10	80/20	65/35	50/50
	OL (d <sub>i</sub> = 3.3)	5 <b>.4</b> 0	5.30	5.13	4.83	4.45	4.12
Material	$Z_{(d_{i} = 5.49)}$	5.47	5.47	5.47	5.47	5.48	5.48
	$M \\ (d_{i} = 3.58)$	5.41	5.33	5.20	4.95	4.62	4.33

The calculated porosities p% are slightly higher than the measured porosities  $p_m\%$  in the temperature range of 500° to 900°C. The difference  $\Delta p$  is probably due to experimental errors rather than to the contribution of pores inaccessible to liquid.

On the basis of the limited test data generated at this point, optimum criteria to look for are (not necessarily in order of priority):

Strength of the electrode

A range of approximately 50% porosity

No closed pores

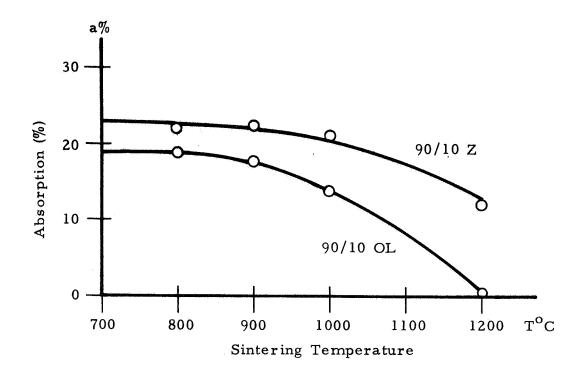
No weight loss (This condition not fulfilled by Magnesia militates against its choice because of the instability of the matrix structure in the electrolyte medium.)

Other constraints were added as higher sintering temperatures were investigated.

### Higher Temperature Range

The second range of temperature is defined as over 900°C up to 1400°C. It was soon established that, as expected, the physical properties would be very much dependent on the sintering temperature, particularly beyond 1000°C. The absorption and porosity drop sharply (Figure 15) due to the excessive shrinkage (Figure 16). Consequently, the physical measurements on the 1" diameter pellets were limited to two selected materials, OL and Z, using selected ratios of ZnO and inorganic and a range of sintering temperature from 800°C to 1200°C for continuity purposes. Tables XI and XII give all pertinent data. Included is a set of data regarding pure ZnO submitted to the same process and sintering temperature for reference purposes.

Although the actual zinc oxide mix electrode will not be sintered at over 900°C, it may be useful to sinter the mix itself at higher temperatures with the intent of modifying the binding of zinc oxide particles with inorganic material particles. Blends sintered at temperatures of 1000°C, 1200°C, and 1400°C respectively were compared with the same blends of powders sintered separately at the same temperatures. Starting with ZnO, Z material and a blend of 80% ZnO and 20% Z, each material was sintered separately at each temperature. Then, a blend of 80% sintered ZnO and 20% sintered Z was prepared (for each sintering temperature used). The blends sintered as blends were compared with the mixes where materials were presintered then blended in the same ratio. X-ray diffraction and reflection (color) under ultraviolet light showed a more pronounced change with increased sintered temperature. It was speculated that a solid solution was formed, at



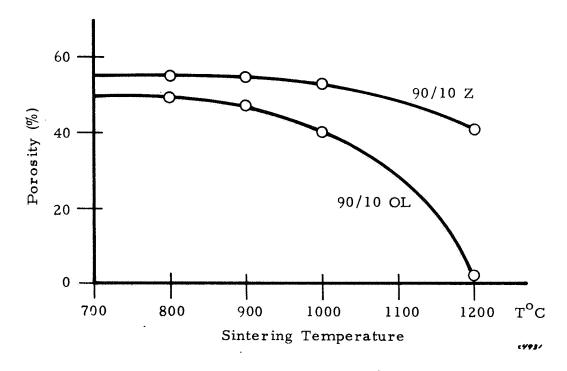


Figure 15. Absorption and Porosity vs Sintering Temperature

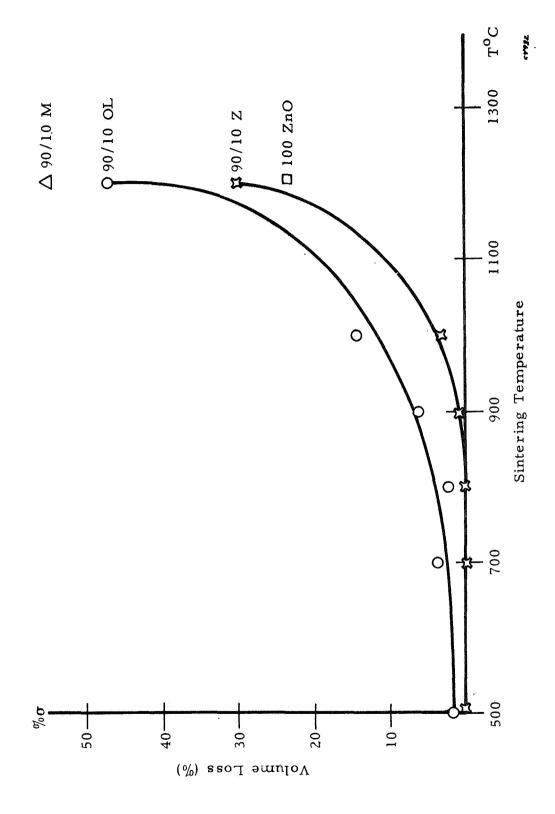


Figure 16. Volume Loss vs Sintering Temperature

TABLE XI

Do = 1" PELLET PHYSICAL CHARACTERISTICS I (AVERAGE OF 3 PELLETS)

			Before	e Sintering	ring			Af	After Sintering	ering		
Material	Ratio	Temp.	N <sub>o</sub> (mils)	V <sub>o</sub> (c. c.)	mo (gm)	O (ii)	N (mils)	v (c. c.)	m(gm) (dry)	m(gm) (wet)	Am (gm)	Weight Loss %
OL	95/5	800	51.5	0.662	1.595	0.997	50.0	0.639	1.581	1.848	0.267	6.0
	90/10	800 900 1000	48.0 48.8 49.8	0.617 0.628 0.641		1.000 0.979 0.944	47.0 47.8 47.8	0.605 0.589 0.548	1. 551 1. 564 1. 566	1.849 1.846 1.785	0.298	2.1
	80/20	1200	50.3	0.630	1,617	0.807	40.8	0.630	1.583	1.871	0.300	1.9
<del>y'-p-v-l</del>	65/35	1200	50.2	0.656	1.593	1.000	51.0	0.656	1.554	1.852	0.298	2.5
Z	95/5	800	51.0	0.656	1.590	1,000	51.0	0.656	1.564	1.926	0,362	1.6
	90/10	800	49.0	0.630	1		49.0	0.630	1.573	1.919	0.346	1.0
***************************************		1000	50.3 52.8	0.647	1.600 1.612	0.988 0.894	50.0 46.5	0.628	1.567	1.899	0.196	2.2
<del>, a daga da a</del>	80/20	800	50.0	0.643	1.593	1.000	50.0 45.5	0.643	1.564 1.570	1.906	0.342	1.8
<b></b>	65/35	800	50.0	0.643	1.594	1.000	50.0	0.643	1.565	1,903	0.338	1.8
×	80/20	1200	51.8	0.666	1,608	0.766	39.0	0.294	1.425	1.425	0	11.4
ZnO	100/0	1200	51.2	0.659	1.610	0.904	47.5	0.499	1.588	1.784	0.196	1.4

 $\Delta m = m' - m$ Weight Loss % =  $\frac{m_o - m}{m_o} \times 100$ 

$$a = \frac{\Delta m}{m} \times 100$$
$$a = m/V$$

## TABLE XII

# Do = 1" PELLETS PHYSICAL CHARACTERISTICS II (AVERAGE OF 3 PELLETS)

 $p_m = a \cdot d_a$ 

 $p = \frac{d_{c} - d_{a}}{d_{c}} \times 100$   $\Delta p = p - p_{m}$   $\sigma = \frac{V_{o} - V}{V_{o}} \times 100$ 

Material	Ratio	Temp. °C	a%	d <sub>a</sub> (g/cc)	p <sub>m</sub> %	d <sub>c</sub> (g/cc)	p%	<b>∆</b> p%	σ%
OL	95/5	800	16.9	2.47	41.8	5.30	53.3	11.5	3.5
	90/10	800	19.2	2.56	49.3	5.13	50.0	0.7	1.9
		900	18.0	2.66	47.9	5.13	48.2	0.3	6.2
		1000	14.0	2.86	40.0	51.3	44.3	4.3	14.5
		1200	0.4	4.64	2.1	5.13	9.5	7.4	47.3
	80/20	800	19.1	2.49	47.6	4.83	48.4	0.8	0
		1200	4.0	4.00	15.8	4.83	17.4	1.6	39.3
	65/35	800	19.2	2.37	45.4	4.45	46.8	1.4	0
Z	95/5	800	23.1	2.38	55.2	5.47	56.4	1.2	0
	90/10	800	22.0	2.50	54.9	5.47	54.9	0	0
		900	22.6	2.43	55.0	5.47	55.6	0.6	0.9
		1000	21.2	2.50	52.9	5.47	54.3	1.6	2.9
		1200	12.4	3.30	41.0	5.47	41.0	0	29.6
	80/20	800	21.9	2.43	53.2	5.47	55.5	2.3	0
		1200	12.9	3.18	40.9	5.47	41.9	1.0	22.0
	65/35	800	21.6	2.43	52.6	5.48	55.6	3.0	0
М	80/20	1200	0	4.85	0	4. 95	2.0	2.0	55.9
ZnO	100/0	1200	12.3	3.18	39.3	5.47	41.8	2.4	24.3

least on the surface of the particles, although a quantitative analysis could not be performed to determine the depth of that layer. The sintering time was again held constant (1 hour). It may be desirable eventually to consider a longer sintering time to establish in the electrical tests if the formation of more solid solution is beneficial.

If, therefore, the presintering of the mix helps in any way, the mix can be used in the normal procedure (addition of binders, ball milling, drying, granulating) for the fabrication of the electrode, which can then be sintered below 900°C. Pellets were made using ratios of 90/10 for OL and Z and also 100% ZnO, following the two procedures (normal and presintering). Tables XIII and XIV give their physical characteristics.

### Surface Area and Pore Size Measurements

### First Series

A few samples of sintered pellets were submitted to other measurements, surface area and pore size. The samples were 80/20 OL, 80/20 Z, and 80/20 M sintered at 700°C (normal process). The tests were made on three different physical samples of each material.

The specific surface area was determined by the standard BET technique using either nitrogen or krypton as the adsorbate. The results are as follows:

Sample	Surface Area (m <sup>2</sup> /g)	Adsorbate
80/20 OL	3.32	Kr
80/20 Z	3.53	Kr
80/20 M	20.70	N

The pore size was determined by the mercury penetration method up to 50,000 psia. The pore size distribution is shown in Figures 17, 18, and 19, and in Table XV. It is worth noting that the so-called water absorption, as previously defined, corresponds to the portion of void consisting of pores over a certain dimension. The original data curves giving penetration volume in cc/g versus the pressure in psia may be found in Appendix A.

### Second Series

In agreement with the NASA Program Manager, a few other combinations were selected for surface area and pore size measurements.

TABLE XIII

Do = 1" PELLET PHYSICAL CHARACTERISTICS I (AVERAGE OF 3 PELLETS)

 $- \times 100$ weight  $\frac{m - m}{loss} = \frac{1}{m}$  $\Delta m = m' - m$ ,|E°

			Befor	Before Sintering	ring			Af	After Sintering	ering		
Material Ratio	Ratio	Temp.	No (mils)	V <sub>o</sub> (c. c.)	m <sub>o</sub> (gm)	D (in)	N (mils)	V (c. c.)	m(gm) (dry)	m'(gm) (wet)	<b>∆</b> m (gm)	Weight Loss %
Normal	Normal Procedure	lure									1	
OL	90/10	850	49.7	0.639 1.598 0.992	1.598	0.992	49.7	0.629 1.569	1.569	1.896	0.327	1.8
Z	90/10	850	52.5	0.675 1.605 0.992	1.605	0.992	52.0	52.0 0.668 1.589	1.589	1.986	0.379	1.0
ZnO	100/0	850	50.0	0.643 1.603 0.988	1.603	0.988	50.0	0.643	1.584	1. 925	0.341	1.2
Blend F	Presinte	Blend Presintered at 1400°C then Normal Procedure Followed	400°C t	hen No	rmal P	roceduı	re Foll	owed				
OL	90/10	850	52.5	0.675 1.583 0.997	1.583	0.997	52.2	0.667	1.557	1.897	0.340	1.6
Z	90/10	850	46.5	0.598	0.598 1.587 0.997	0.997	46.8	0.598	1.559	1.871	0.312	1.8
ZnO	100/0	850	47.5	0.611	1.605	0.611 1.605 0.998	47.5	0.609 1.582	1.582	1.872	0.290	1.4

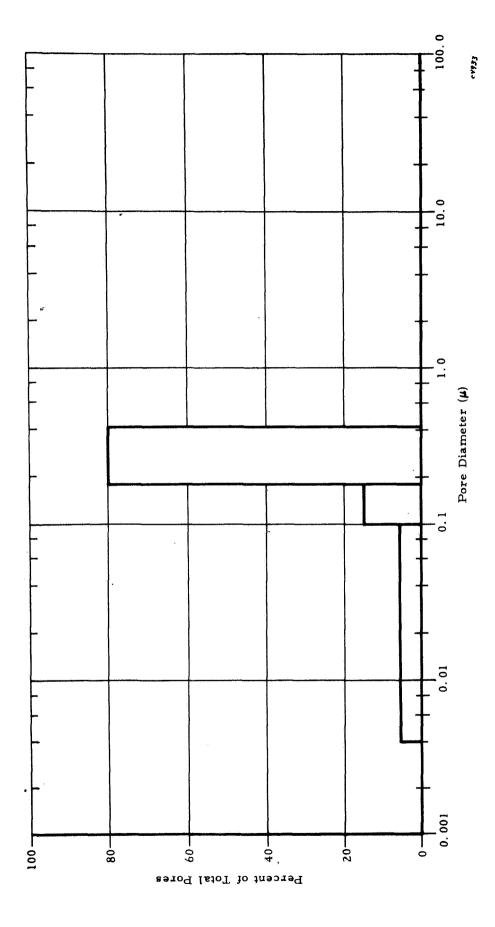


Figure 17. Pore Size Distribution of 80/20 OL Material

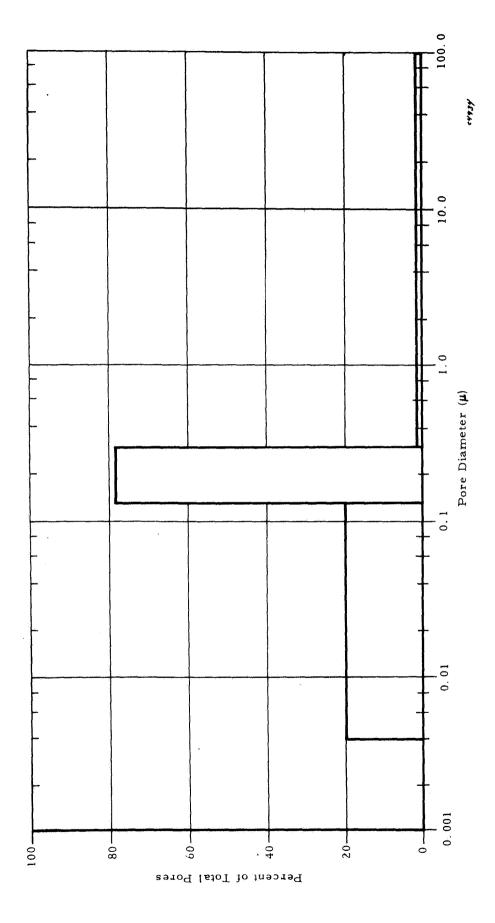


Figure 18. Pore Size Distribution of 80/20 Z Material

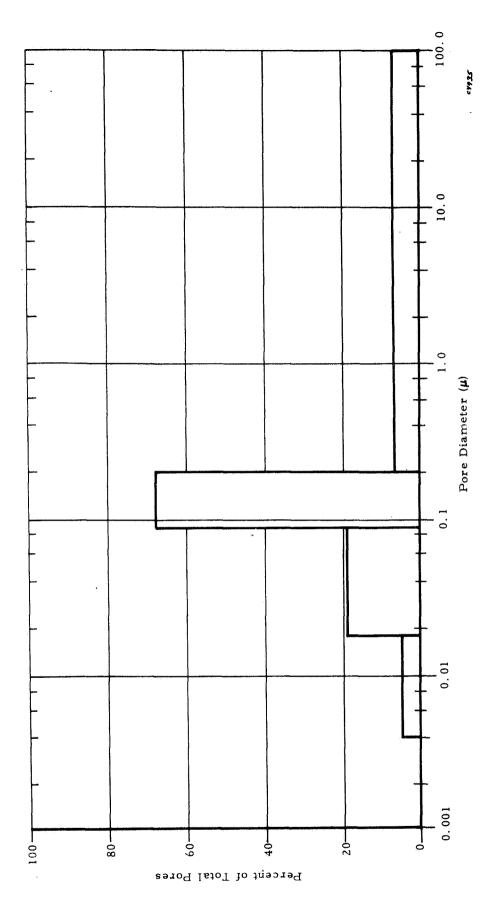


Figure 19. Pore Size Distribution of 80/20 M Material

TABLE XV
PORE SIZE DISTRIBUTION

	(1)	(2)	(3)			
	Penetration Volume (a)		•	Pore Diameter		of Total e Volume
Sample	$(\frac{\text{cc}}{\text{g}} 100)$	(b) ( <u>cc</u> 100)	$\frac{b}{a}$ 100	Diameter D (µ)	Per Range	Cumulative
80/20 OL				D > 0.42	0	0
	17.5	14	80	0.42-0.18	80	80
				D < 0.18	20	100
				D > 0.29	1.5	1.5
80/20 Z	20.0	16	80	0.29-0.13	79	80.5
				D < 0.13	19.5	100
				D > 0.18	7.5	7.5
80/20 M	21.5	16	75	0.19-0.09	67	75
				D < 0.09	25.5	100

- (1) Determined under 50,000 psia pressure.
- (2) Value at the end of the linear portion of the curve of penetration vs pressure.
- (3) Fraction percentage of total void volume where absorption takes place. Compare to second line of "Pore Volume, Cumulative."

The choice of combinations was restricted by the maximum number imposed by the work statement and by the elimination of the candidates least likely to be used. For instance, magnesia (material M) was not considered immediately suitable because of its excessive weight variation following wetting, drying, sintering, rewetting (hydroxide formation). Ratios of inorganic material too low or too high were temporarily set aside in order to keep a fixed medium range, chosen to be 90% ZnO and 10% inorganic, as a comparative basis. As the maximum strength of the pellets was developed at the highest sintering temperature (below 900°C), the selected temperature was fixed at 850°C. Since the two processes evolved (normal and presinter) have equal possibilities at this point, both will be considered.

This screening narrows down the choice to the following combinations:

Materials: OL, ZRatio: 90/10 Sintering Temperature:  $850^{\circ}$ C

Process: Normal (N), Presinter (PS)

Table XVI gives a summary of pore size distribution and pertinent information for all seven combinations. A few remarks are in order:

- (a) It appears that the presinter process (PS) cuts down on surface area and spreads the pore distribution when compared with the normal process. It can be speculated what effect this will have on the zinc electrode performance: on one hand, the reduction of zinc exposure to electrolyte may delay its corrosion; on the other hand, reduction in electrolyte accessibility may cause premature poor performance due to dryness.
- (b) The effect of higher sintering temperature is known to be shrinkage of pores which entails less electrolyte absorption. It can be seen that the percentage of pores corresponding to electrolyte absorption decreases from 93% (for the selected materials OL and Z) to 85%. However, this is not considered a problem since all pellets were originally made to the same specifications of weight, size, and thickness, starting with the same apparent density regardless of the subsequent treatment. The electrode can be originally designed so that it ends up with the desired porosity and electrolyte absorption percentages after the sintering operation.

TABLE XVI

SURFACE AREA AND PORE SIZE DISTRIBUTION

Sintering Temperature		2000L			85(	850°C	1
Ratio		80/20			106	90/10	
Material	OL	Z	M	OL		Z	
Process	Z	Z	Z	Z	PS	Z	PS
Specific Surface Area (m <sup>2</sup> /g)	3.32	3,53	20.7	3,85	2.28	1.82	1.63
Pore Size Range		Percentage of	ntage	of Por	Pores (%)		
177 µ to 1 µ	0	0.5	3	0	2.6	3,5	3.3
1 to 0.5	0	0		0	ю	0	8.6
0.5 to 0.1	93	92.5	72	85.5	77	81	69.5
0.1 to 0.006	Ŋ	5.5	22	12	15.1	15.5	18.1
0.006 to 0	2	1,5	2	2.5	2.2	0	0.5
Total pore volume	100	100	100	100	100	100	100
Percentage of pores (%) down to 0.1 $\mu$ corresponding to electrolyte absorption	93%	93%	76%	85.5	82.6	84.5%	81.4%
Percentage of pores (%) smaller than 0.5 $\mu$	100%	99.5%	%96	100%	94.4	96.5%	88.1%

### Incorporation of Additives

As the sintering temperature of the electrode will be higher than the decomposition temperature of HgO and PbO, it was necessary to develop a method for introducing such additives in controlled quantity and uniformly throughout the mass of the sintered zinc oxide electrode.

The principle is as follows: The electrode is dipped in an acetic acid solution where HgO or PbO has been dissolved. The amount of mercuric or lead acetate solution picked up within the pores of the electrode is enough to leave the desired percentage of HgO or PbO in the electrode when the wet electrode has been dried and submitted to approximately 150°C for 6 to 8 hours to decompose and drive off the acetic acid and acetates. Several analyses of controlled weight pellets impregnated with controlled concentration solutions gave the predicted HgO or PbO percentages. The concentration may be adjusted so that one dipping is enough to leave the desired amount of HgO or PbO in the electrode after drying and decomposing the acetate salts at high temperature. A typical procedure is given here.

The sintered pellet (or electrode) of known absorption is dipped for 4 minutes in a 10% acetate solution of desired additive and desired concentration, then dried for 1/2 hour at 100°C, then heat-treated at 150°C for 6 hours.

Using pellets of various compositions and materials, the absorption was calculated rather than measured (the two absorptions are found to be very close) to determine the desired concentration of the additive in the acetic solution. The calculated absorption is given by the formula

$$a_c\% = 100 \left( \frac{1}{d_a} - \frac{1}{d_c} \right)$$

where  $d_a$  is the apparent density easily determined by simple measurements of dimensions and weight and  $d_c$  is the composite density (or true density) as defined in Table X.

Tables XVII and XVIII give a summary of final determinations of HgO and PbO in several samples. Aiming at 2% additive, the results are reproducible within a very narrow margin. HgO was determined by chemical titration and PbO by electroplating and gravimetry.

### TASK II - ELECTRICAL CHARACTERIZATION

This task deals with the fabrication, testing and evaluation of the cells using various selected electrode compositions.

TABLE XVII
MERCURIC OXIDE INCORPORATION

		ui O¤Η ½	HgO Content in Pellet	in Pellet
Pellet Composition	Calculated Absorption	10% Acetic Solution	% of total weight	% of Zinc Oxide Weight
100% ZnO	20%	%L . 7	2.31	2.3
90/10 OL	20%	7.0	1.70	1.9
80/20 Z	20%	6.2	1.56	2.0
80/20 OL	20%	6.2	1.52	1.9

TABLE XVIII
LEAD OXIDE INCORPORATION

		ni Oda %	PbO Content in Pellet	in Pellet
Pellet Composition	Calculated Absorption	10% Acetic Solution	% of total weight	% of Zinc weight
100% ZnO	20%	0.6	2.01	2.0
90/10 Z	25	9.9	1.81	2.0
90/10 Z	24	8.9	1.83	2.0
80/202	22	9.9	1.74	2.2
80/20 OT	19	7.3	1.66	2.1

### Preliminary Cell Tests

Preliminary cell tests were started to verify a few critical milestones and establish a good basis for recommending the statistical distribution of variables to be tested within the limits imposed by the work statement.

The cell test design is certainly a critical factor in evaluating the zinc electrode. In the spirit of the work statement, two positive and one negative electrodes were used in order to make the cell zinc-limited and thus run an accelerated test to more quickly bring out the shortcomings of the zinc electrode. Rigid organic separator 3420-09 will be used as specified in the work statement. When the zinc electrode is sandwiched between two separators forming a negative wafer, the separator cracking caused by the expansion of zinc during its cycle life is very often the failure mode of silver-zinc cells using this type of construction. The reverse construction, namely the positive wafer where silver electrodes are sandwiched and zinc is left outside is not conducive to separator cracking. Thus, the zinc electrode can be fully evaluated on its own merits without extraneous factors contributing to failure. Variation of design is therefore another variable.

The wet process of HgO incorporation in the zinc electrode had to be tested in actual cells to firmly establish that it is not causing any unexpected effect.

Various ratios of inorganic to ZnO had to be scanned quickly to narrow down the choice of the variables. This ratio varied from 5% to 20%.

The design characteristics are as follows:

Positive: Dimensions: 1.6" x 1.6" x 0.22"

Silver Weight: 4.5 g

Negative: Dimensions: 1.6" x 1.6" x 0.070"

(including KT)

Mix Material: 6 g

HgO: 2%

The cells were cycled at 100% depth as follows:

Charge: 100 mA to 2.10 V

Discharge: 600 mA to 1.0 V

Two groups of cells were fabricated (each variation includes three cells), covering a total of 24 cells.

### Series ZN-25: Encapsulated Negatives

This series includes five groups of three cells each (all of the negative encapsulated type design).

Group A Control: Regular zinc oxide electrode (not sintered)

Group B Sintered electrode: 100% ZnO

Group C Sintered electrode: 95% ZnO, 5% zirconia

Group D Sintered electrode: 90% ZnO, 10% zirconia

Group E Sintered electrode: 80% ZnO, 20% zirconia

All electrodes had the same amount of mix material regardless of composition.

The cells were submitted to eight deep discharge cycles at 0.6 A to 1.0 V. The 80/20 Z material electrode output is lower than 80% of that of the control on every cycle. The outputs of other electrodes are very close to one another, even after eight cycles. The same holds true for the average plateau voltages. They were then placed on the automatic cycling regime No. 2, as described in the work statement, viz. discharge at 1.2 A for 1/2 hour; charge at 0.66 A for 1 hour.

After a certain number of cycles, the cells were not able to sustain such a high rate regime and were switched to a lower rate regime (discharge at 0.8 A for 1/2 hour; charge at 0.5 A for 1 hour).

Tables XIX and XX give all cycles at various rates and other pertinent information.

### Series ZN-31: Encapsulated Positives

This series includes three groups of three cells each (all of the positive encapsulated design type).

Group A Control: Regular zinc oxide electrode (not sintered)

Group B Sintered electrode: 100% ZnO

Group C Sintered electrode: 90% ZnO, 10% zirconia

The cells were submitted to seven deep discharge cycles at 0.6 A to 1.0 V then placed on the automatic cycling regime No. 2 described above.

TABLE XIX

TEST DATA OF ZN-25 CELLS WITH NEGATIVE WAFER

Discharge: 600 mA to 1.0 V Charge: 100 mA to 2.10 V

Average Capacity (Ah)	4h)		:						
					Cycle			3	
Variation	Group	1	2	3	4	īΩ	9	7	8
Control ZnO	¥	2.8 Ah	2.3	2.5	2.3	2.3	2.2	1.8	2.1
Sintered 100% ZnO	Ф	2.5	2.3	2.2	2.1	2.2	2.2	2.0	2.0
95/5 Z	υ	2.5	2.2	2.1	2.0	2.2	2.0	2.0	2.0
90/10 Z	Д	2.4	2.1	2.0	1.9	2.1	1.9	1.9	1.9
80/20 Z	闰	2.0	1.7	1.5	1,5	1.5	1.4	1.4	1.3
Average Plateau Voltage (Volts)	ltage (V	olts)		:					
Control ZnO	Ą	1.42 V	1,41	1.41	1.41	1.42	1,43	1.42	1.40
Sintered 100% ZnO	В	1.42	1.40	1.38	1,39	1,39	1.40	1.42	1.39
95/5 Z	υ	1.41	1.40	1.39	1.39	1,38	1,41	1.39	1.40
90/10 Z	Д	1.38	1,38	1.39	1,39	1,38	1.39	1.40	1.40
80/20 Z	泊	1.36	1.33	1.35	1,36	1.36	1,36	1.38	1.36

TABLE XX

CYCLING CAPABILITY OF CELLS WITH NEGATIVE WAFER

(ZN-25 Series)

	Last Capacity Check	Ah (	2.0 (317)	1.3 (210)	1.7 (301)	0.4 (198)	0.5 (197)	0.3 (197)	0.4 (199)	0.6 (200)	0.7 (197)	0,3 (215)	0.3 (201)	0.4 (203)	1.0 (109)	1.0 (148)	0.9 (148)
	Wet	(days)	29	64	29	13	78	80	89	89	48	7.1	7.1	20	99	89	89
	Total	Cycles	317+	328+	301+	276	311	232	199	200	197	215	201	203	109+	148+	148 <sup>†</sup>
	0.5 A for 1 hr	0.8 A for 1/2 hr	100+	51+	85+	78	113	34	-	2	0	125	111	118	50+	74+	+62
Cycles at Indicated Regime	0.66 A for 1 hr	1.20 A for 1/2 hr	*602	264*	208*	190	190	190	190	190	189	82	82	7.2	51	99	61
Cycles at	0.1 A to 2.10 V	0.6 A to 1.0 V	8	<b>∞</b>	.00	8	<b>∞</b>	8	8	<b>∞</b>	8	8	∞	<b>∞</b>	8	∞	80
	Charge	Discharge															·
	;	No.	-1	2	33	4	Ŋ	9	7	∞	6	10	7	12	13	14	15
	Group	and Variation	Ą	(Control	ZnO)	B	(Sintered)	(SnO)	O	(65/5 Z)		Ω	(90/10 Z)		ы	(80/20 Z)	

 $^{st}$  Switched to other regime before failure.

<sup>+</sup> Cells still capable of limited cycling.

Tables XXI and XXII give a summary of their cycling data.

As suspected, the high rate charge of this regime (22 mA/cm<sup>2</sup>) imposes a severe penalty on the cells; cycle life falls then in the range of 200 cycles. This was demonstrated on several 5 Ah Ag-Zn cells of the NASA contract NAS 3-10924\* where a similar regime with prorated charge and discharge currents, called regime E, gave the same type of results (data obtained were erratic and ranged from 55 to 400 cycles, with a representative average of 250 cycles).

It was recommended that this regime be revised as being in conflict with other cell design features. The separator used or to be used is known to be satisfactory only at relatively low rates; the plate area called out is such that the current density is ipso facto very high on discharge and on charge; this in turn causes an inordinate amount of gassing because of the necessary overcharge to keep the cell cycling.

All these factors obviously give erratic cycling results and may blur the value of a new zinc electrode composition.

### Selection of Combinations of Variables

The variables and variable levels to be considered would lead to a high number of combinations of electrode construction features. A discriminative selection was made jointly with the NASA Program Manager in order to limit this number to 20 as required by the work statement with two control groups, A and B (defined later). Under the direction of the NASA Program Manager, the cells were fabricated in different groups at various times of the program, as data were generated.

Prior to fabrication, it was decided not to consider the inorganic binder OL because it was recognized that the presence of iron in its composition would cause undesirable gassing in the zinc electrode. Only one inorganic binder (zirconia) was used.

The variables and levels selected were narrowed down to the following:

A. Himy, Development and Testing of a Five Ah Silver-Zinc Cell, Final Report NASA CR-72551, Astropower Laboratory, McDonnell Douglas Astronautics Company, Western Division, July 1969.

TABLE XXI

TEST DATA OF ZN-31 CELLS WITH POSITIVE WAFER

Discharge: 0.6 A to 1.0 V Charge: 100 mA to 2.10 V

	Aver	age Car	Average Capacity (Ah)	Ah)		4	
				Cycle	le.		
Variation	Group	H	7	3	4	5	9
Control ZnO	A .	22	2.7	2.4	2.1	2.1	2.1
Sintered 100% ZnO	В	2.1	8.2	2.2	2.1	2.3	2.1
90/10 Z	ک	2.2	2.6	2.2	2.1	2.3	2.2
	Average Plateau Voltage (volts)	Plateau	Voltage	(volts			
Control ZnO	Ą	1.36	1.36 1.40	1.41	1.42	1.40	1.42
Sintered 100% ZnO	В	1.37	1.38		1.40 1.38	1.39	1.40
90/10 Z	U	1.39	1.39	1.40	1.40 1.40	1.40	1.40

TABLE XXII

# CYCLING CAPABILITY OF CELLS WITH POSITIVE WAFERS

(ZN-31 Series)

			Cycles at In	Cycles at Indicated Regime				
Group	;	Charge	0.1 A to 2.10 V	1 A to 2.10 V 0.66 A for 1 hr 0.5 A for 1 hr	0.5 A for 1 hr	Total	Wet	Last Capacity
and Variation		No. Discharge	0.6 A to 1.0 V	1.2 A for 1/2 hr	1.2 A for 1/2 hr 0.8 A for 1/2 hr	0	(days)	(days) Ah (Cycle No.)
A			7	229		236	54	0.7 (236)
(Control	2		7	230	133	370	80	0.7 (237)
ZnO)	33		7	230	91	253	69	0.7 (253)
В	4		7	273	126	406	71	0.5 (406)
(Sintered	5		7	274*	188	469	73	0.9 (216)
ZnO)	9		2	274*	96	377	29.	0.8 (377)
O	7		7	206	1	213	64	J
(60/10 Z)	∞		7	227	l	284	65	1.0 (234)
	6		2	206	1	213	64	-

 $^{st}$  Switched to other regime before failure.

Inorganic Binder: Zirconia (Z)

Ratio: 95/5, 90/10, 80/20

Process: Normal (N), Presinter (PS)

Additives (Hg, Pb): (2%, 0%), (2%, 1%), (2%, 2%)

Grid in zinc electrode: Exmet 5 Ag-14-1/0 (flat structure)

Distex 5 Ag-38-1/0 (honeycomb)

Design: Encapsulated negative or

negative wafer (-) w Encapsulated positive or positive wafer (+) W

Separator: 3420-09, 3420-25

The following were maintained constant:

The sintering temperature (850°C)

The electrolyte concentration (30% KOH)

The negative and positive interseparators (10 mil-KT)

The electrode thickness, weight and porosity.

All combinations and control groups are listed in Table XXIII, although not in chronological order. The successive tests were as follows:

- (a) Combinations 1 to 4 were intended to screen out minor variables. Using one binder material Z, one ratio (90/10), one process (normal), a standard amount of amalgamation (2%), and separator 3420-09, the variations were carried out on the grid (Exmet 5 Ag-14-1/0, which presents a flat structure and Distex 5 Ag-38-1/0, which presents a honeycomb structure) and on the electrode pack assembly design (encapsulated negative contrasted to encapsulated positive). Control group A used standard zinc oxide electrodes, made with unsintered zinc oxide mix containing 2% HgO and using the Distex grid and the encapsulated negative design.
- (b) Combinations 5 through 12 had one important change besides electrode compositions: NASA Technical Direction No. 2, dated 1/22/69, and No. 3, dated 1/10/69, ordered the use of separator 3420-25. Control group B is essentially the same as control group A except the change in separator.
- (c) Combinations 13 through 20 used the former separator, 3420-09, as redirected by NASA Technical Direction No. 5, dated 4/23/69.

TABLE XXIII COMBINATIONS OF ELECTRODE VARIABLES

Comb. No.	Separator	Grid	Design (wafer)	Ratio (ZnO/Binder)	Process	Additive (PbO %)
A	3420-09	Distex	(-) w	100/0	Not sintered	0
1	11	Exmet	(+) w	90/10	N	0
2	11	Exmet	(-) w	11	N	0
3	11	Distex	(+) w	11	N	0
4	1.1	Distex	(-) w	1.3	N	0
13	11	Exmet	Ħ	11	N	1
14	11	13	31	ti	N	2
15	11	11	ff.	11	PS	1
16	11	11	11	11	PS	2
17	†1	Fit	11	80/20	N	1
18	11	11	.†1	1.1	N	2
19	11	11	11	11	PS	1
20	11	it	11	11	PS	2
В	3420-25	Distex	(-) w	100/0	Not sintered	0
5	11	Exmet	11	90/10	N	0
6	11	11	1.1	11	N	1
7	11	11	1.1	1,1	PS	0
8	11	11	11	11	PS	1
9	.11	tt	11	95/5	N	0
1.0	11	'n	11	11 -	N	1
11	11	11	11	l n	PS	0
12	11	11	11	1,1	PS	1

Constant:

Binder:

Zirconia

Sintering Temp: 850°C Amalgamation: 2% HgG

2% HgO

Each combination or group consisted of nine cells to be tested in subgroups of three cells on three different regimes.

The breakdown of the number of cells (limited by the work statement to a maximum of 250) is as follows:

Preliminary cell tests:	24
20 combinations and 2 control groups:	198
Repeat of 2 combinations:	24
Zinc efficiency tests:	4
	250

### Testing

All cells were first tested identically. After a formation cycle, they were submitted to four deep discharge cycles, each at a different rate.

After these five manual cycles, they were divided in groups of three cells each, which were submitted to different automatic cycling regimes.

The manual cycling consisted of a formation at 100 mA charge to 2.10 V cut-off (maximum time limited to 24 hours) and 600 mA discharge to 1.0 V, followed by four cycles each at a different rate to 0.9 V cut-off:

30 mA

600 mA

1.5 A

3.0 A

The automatic cycling covers three regimes defined as follows:

Regime	1	2*	3
Temperature	100°C	25°C	25°C
Period	l hour	1.5 hours	24 hours
Discharge	$0.60\mathrm{A/0.5hr}$	0.9A/0.5hr	1.2  A/1.2  hr
Charge	$0.66\mathrm{A/0.5hr}$	$0.50\mathrm{A/lhr}$	$70\mathrm{mA/22.8hr}$

<sup>\*</sup>The original regime No. 2 (discharge at 1.2 A for 1/2 hour, charge at 0.66 A for 1 hour) was modified by NASA Technical Direction No. 3. dated 1/10/60.

The cells were cycled continuously and stopped about every 100 cycles for a capacity check on Regimes 1 and 2, corresponding to 4 days cycling on Regime 1 and 6 days on Regime 2. The capacity check of cells on Regime 3 was done only every 30 cycles, corresponding to 30 days cycling time. The tables presenting cycling data refer to this operation as check points.

When a technical failure occurred (discharge voltage dropping below 1.0 V before the end of the discharge period), the cell was recharged and its capacity checked. If it was found to be over the cycling capacity requirement, the cell was put back on cycling. The tables presenting cycling data refer to this operation as cycling failures. In several instances, however, in the later part of the program, it was found desirable to avoid repeated and frequent 100% depth-of-discharge cycles which may cut down on the performance of the cell cycling on a particular regime. Therefore, in agreement with the NASA program manager, it was decided to give the cell two consecutive charge periods (skipping a discharge) if it reaches a cycling failure; the cell was then left cycling if it resumed its normal cycling performance.

When the cell failed completely, the failure was classified as technical failure (TF) if the cell could not meet the cycling capacity requirement on a capacity check, or catastrophic failure (CF) if the cell could not cycle or accept charge.

### Control Group A and Combinations 1 through 4

### Manual Cycling

The data of the five manual deep cycles given to each combination (group of nine cells) are presented in Tables XXIV through XXVIII.

Capacity and plateau voltage variation with discharge rates are shown graphically in Figures 20 through 23. Figure 24 shows a typical set of discharge curves at various rates.

The cells of combinations 1 through 4, destined to be placed on automatic regimes 1 and 2, were discontinued after approximately 200 cycles for regime No. 1 (because they were by error cycled at room temperature instead of 100°C) and approximately 80 cycles for regime No. 2 (because the discharge rate, originally 1.2 A, was modified to 0.9 A by NASA Technical Direction No. 3). Consequently, the 24 cells involved were discontinued. The automatic cycling data of these cells are presented in Tables XXIX to XXXII.

New cells were fabricated for the correct tests. Tables XXXIII to XXXVI give the manual cycling data of the new cells noted A affixed to

TABLE XXIV

PRECYCLING TEST DATA Control Group A (3420-09)

	Form (0.	Formation (0.6 A)	Cycle 1 (30 mA)	le l nA)	Cyc (0.6	Cycle 2 (0.6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Output	th.	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
2.1 Ah	ц	1,41 V	2.4 Ah 1.52 V	1.52 V	1.8 Ah	1.42 V	1.8 Ah	1, 30 V	1.5 Ah	1.17 V
2. l Ah	된	1.41 V	2.6 Ah	1.52 V	1.8 Ah	1.42 V	2.0 Ah	1.31 V	1.8 Ah	1.18 V
2.0 Ah	면	1.41 V	2.5 Ah	1.52 V	1.9 Ah	1.42 V	1.8 Ah	1.29 V	1.7 Ah	1. 16 V
2. 1 Ah	-प	1.41 V	2.6 Ah	1.52 V	2.0 Ah	1.43 V	2.0 Ah	1.31 V	1.7 Ah	1. 19 V
1.9 Ah	.g	1.41 V	2.4 Ah	1.52 V	1.9 Ah	1.43 V	2.0 Ah	1.32 V	1.7 Ah	1.19 V
2.0 Ah	ج-	1.42 V	2.4 Ah	1.52 V	1.9 Ah	1.41 V	1.9 Ah	1.31 V	1.7 Ah	1.17 V
2.0 Ah	-4	1.42 V	2.5 Ah	1.52 V	2.0 Ah	1.43 V	2.0 Ah	1.32 V	1.8 Ah	1.20 V
2.0 Ah	-4	1.42 V	2.5 Ah	1.52 V	1.9 Ah	1.42 V	2.1 Ah	1.31 V	1.7 Ah	1.18 V
2.0 Ah	ų,	1.42 V	2.6 Ah	1.52 V	1.9 Ah	1.43 V	2. 1 Ah	1,32 V	1.8 Ah	1.19 V
2.0 Ah	Ah	1.42 V	2.5 Ah	1.52 V	1.9 Ah   1.42 V	1.42 V	2.0 Ah	1,31 V	1.7 Ah	1, 18 V
				-						

TABLE XXV

	Formati (0.6 Al	ormation (0.6 Ah)	Cyc (30)	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cycle (1.5	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
111	2.3	1.42	2.3	1.50	2.3	1.40	2.0	1.30	1.9	1.18
112	2.3	1.41	2.3	1.50	2.2	1.36	1.7	1.30	1.8	1.17
113	2.3	1.42	2.3	1.50	1.9	1.34	1.8	1.30	1.8	1.19
121	2.3	1.40	2.3	1.50	2.3	1.39	1.8	1.28	1.9	1.18
122	2.3	1.41	2.3	1.50	2.3	1.40	2.0	1.31	1.9	1.17
123	2.3	1.41	2.3	1.50	2.1	1.36	1.7	1.28	1.8	1.16
131	2.3	1.42	2.3	1.50	2.3	1.40	2.0	1.32	1.8	1.19
132	2.3	1.42	2.2	1.50	2.1	1.39	2.0	1.30	1.9	1.19
133	2.3	1.41	2.2	1.50	2.3	1.38	1.8	1.30	1.9	1.20
Avg	2.3	1.41	2.3	1.50	2.2	1.38	1.8	1.30	1.8	1.18

TABLE XXVI

	Formati (0.6 A	Formation (0.6 A)	Cyc (30	Cycle 1 (30 mA)	Cyc (0.	Cycle 2 (0.6A)	Cyc (1.	Cycle 3 (1.5 A)	Cyo (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
211	2.3	1.37	2.4	1.48	2.2	1.40	1.8	1.33	1.5	1.18
212	2.3	1.36	2.2	1.49	2.3	1.40	1.7	1.32	1.5	1.14
213	2.3	1.39	2.3	1.46	2.3	1.42	2.1	1.32	1.9	1.20
221	2.3	1.37	2.4	1.48	2.1	1.40	1.7	1.30	1.5	1.19
222	2.3	1.36	2.4	1.49	2.3	1.39	1.7	1.30	1.2	1.16
223	2.3	1,35	2.4	1.49	1.9	1.39	1.7	1.29	1.2	1.15
231	2.3	1.37	2.3	1.47	2.3	1.41	2.0	1.30	1.8	1.19
232	2.3	1.33	2.4	1.50	2.2	1.39	1.7	1.28	1.2	1.10
233	2.3	1.32	2.4	1.50	2.0	1.40	1.8	1.30	1,5	1.16
Avg	2.3	1.36,	2.4	1.49	2.2	1.40	1.8	1.29	1.5	1.16

TABLE XXVII

	Form (0.	Formation (0.6A)	Cyc (30)	Cycle 1 (30 mA)	Cyc (0.	Cycle 2 (0.6 A)	Cycle (1.5A	Cycle 3 (1.5A)	Cycle (3 A)	ycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)								
311	2.3	1.39	2.4	1.50	2.1	1.40	2.0	1.31	2.0	1.20
312	2.3	1.40	2.3	1.50	2.3	1.42	2.3	1.32	2.3	1.24
313	2.3	1.40	2.3	1.50	2.3	1.41	2.2	1.32	2.3	1.24
321	2.3	1.40	2.3	1.50	2.1	1.40	2.1	1.31	2.0	1.20
322	2.3	1.41	2.2	1.50	2.2	1.30	2.2	1.31	2.3	1.20
323	2.3	1.41	2.2	1.50	2.3	1.40	2.1	1.30	2.2	1.22
331	2.3	1.40	2.3	1.50	2.1	1.39	1.9	1.30	2.0	1.16
332	2.3	1.40	2.4	1.50	2.1	1.40	2.0	1.30	2.0	1.20
333	2.3	1.40	2.4	1.50	2.1	1.40	1.9	1.30	2.0	1.16
Avg	2.3	1.40	2.3	1.50	2.2	1.40	2.1	1.31	2.1	1.20

TABLE XXVIII

	Forn (0.	Formation (0.6A)	Cycle (30 mA	Cycle 1 (30 mA)	Cyc (0.	Cycle 2 (0.6A)	Cyc (0.	Cycle 3 (0.5A)	Cyc (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
411	2.3	1.39	2.4	1.50	1.8	1.36	1.7	1.28	1.5	1.12
412	2.3	1.36	2.4	1.50	1.9	1.38	1.6	1.30	1.5	1.16
413	2.3	1.38	2.4	1.50	1.9	1.36	1.7	1.30	1.5	1.16
421	2.3	1.38	2.4	1.50	2.1	1.38	1.8	1.30	1.8	1.20
422	2.3	1.36	2.4	1.50	1.8	1.36	1.8	1.29	1.2	1.10
423	2.3	1.36	2.3	1.50	1.9	1.38	1.7	1.30	1.5	1.16
431	2.3	1.40	2.4	1.50	2.0	1.39	1.7	1.32	1.5	1.18
432	2.3	1.38	2.4	1.50	1.9	1.36	1.6	1.31	1.5	1.18
433	2.3	1.36	2.4	1.50	1.9	1.38	1.8	1.31	1.8	1.18
Avg	2.3	1.38	2.4	1.50	1.9	1.37	1.7	1.30	1.5	1.16

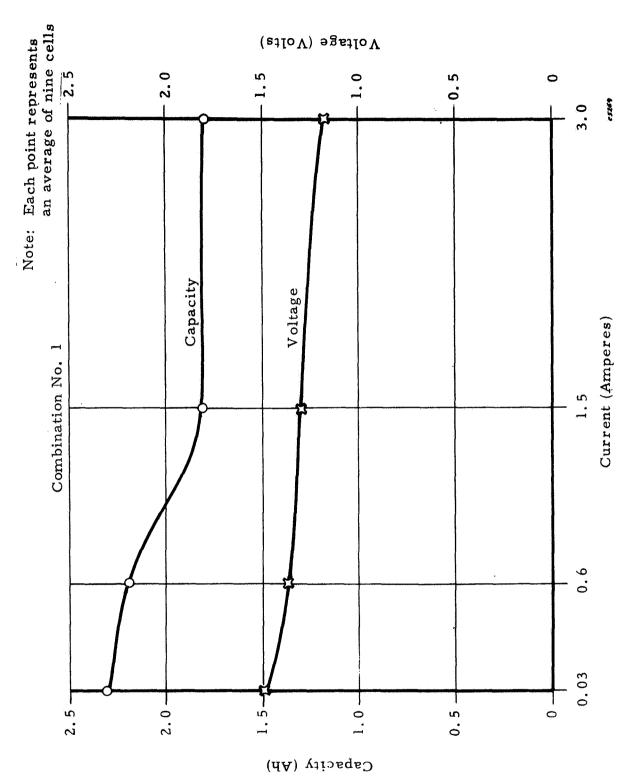
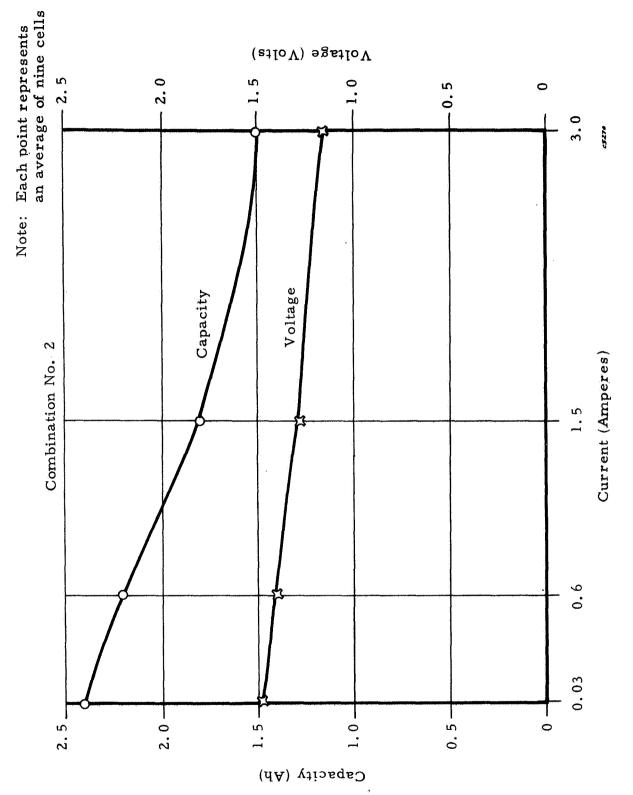
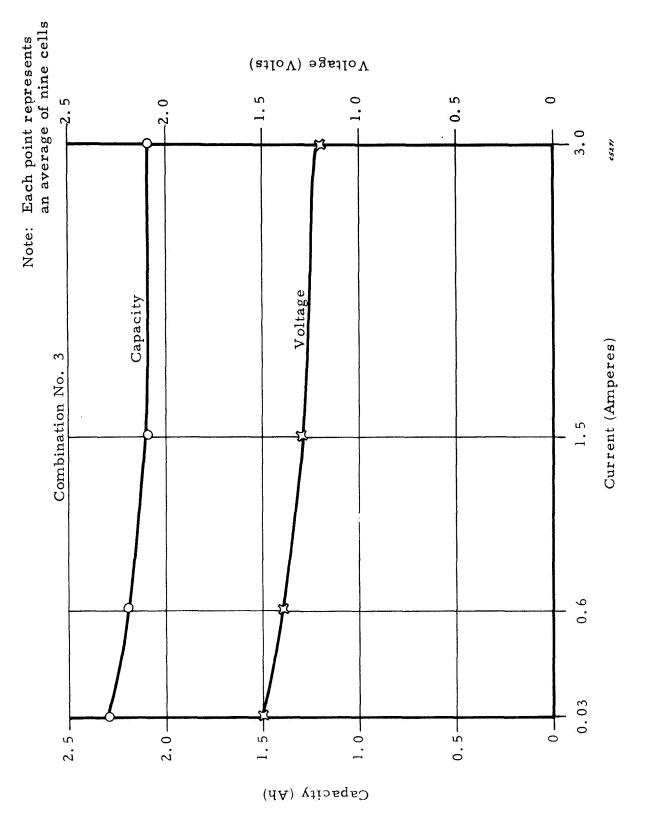


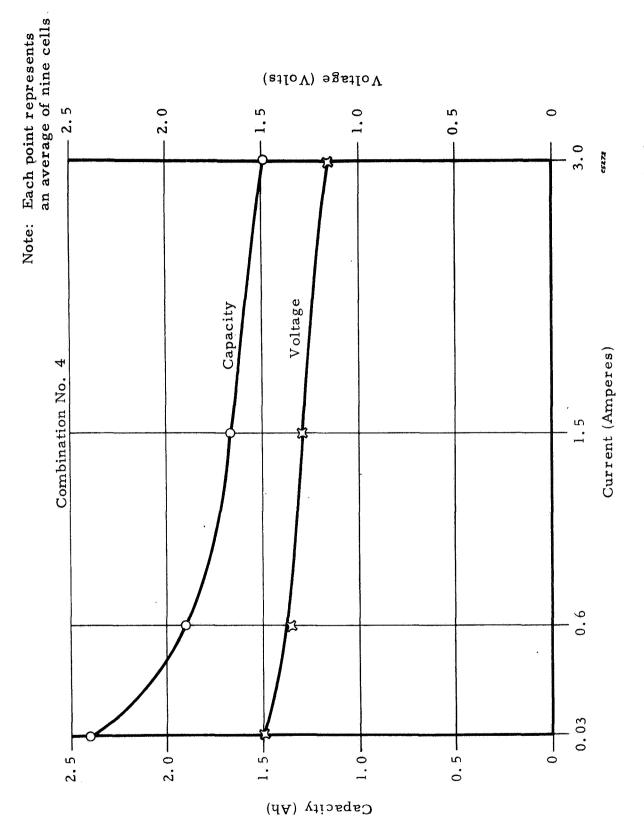
Figure 20. Capacity and Plateau Voltage During First Four Cycles



Capacity and Plateau Voltage During First Four Cycles Figure 21.



Capacity and Plateau Voltage During First Four Cycles Figure 22.



Capacity and Plateau Voltage During First Four Cycles Figure 23.

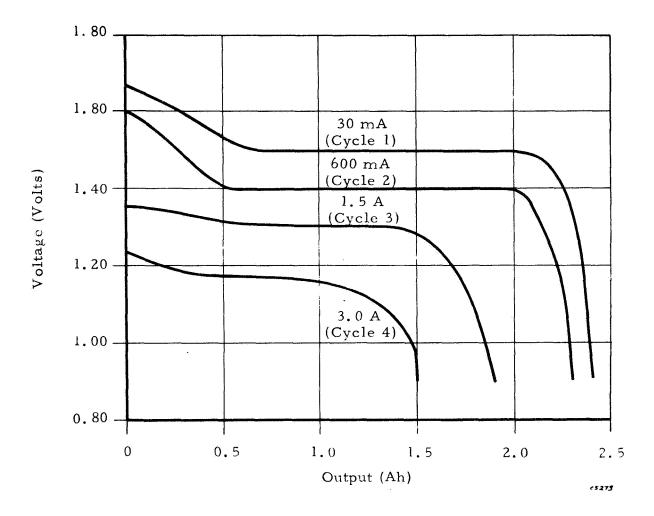


Figure 24. Typical Discharge Curves of Test Cells
During the First Four Cycles

TABLE XXIX

# TEST DATA ON COMBINATION NO. 1 (ORIGINAL)

Regime 1:	Run at 25°C by error	instead of 100-C; cells were discontinued and replaced with new ones.		Regime 2:	Run at the original 1.2 A	by NASA to 0.9 A; cells	replaced with new ones.		
. 2 A)	123		53 (1, 4)					53	(+)
Regime 2 (1.2 A)	122		84 (1.4)					84	(+)
Reg	121		88 (1.3)					88	(+)
(2)	113		104(1.4)   104(1.4)   88(1.3)   84(1.4)   53(1.4)	181 (1.2)		-		181	(+)
Regime 1 (25°C)	112		104 (1.4)	197 (1.3)   181 (1.2)	-			197	(+)
Reg	111		104 (1.6)	171 (1.4)				171	(+)
	Cell No.	Capacity Checks	1. N(Q)	2. N(Q)	3. N(Q)	4. N(Q)	5. N(Q)	Status Cycle	Failure Mode

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. .ii TF

Catastrophic Failure - Cell cannot accept charge or cycle. H  $\mathbf{C}^{\mathbf{H}}$ 

Cycle Number (Capacity) H (Q)N Cell still cycling when stopped at indicated cycle. 11 <del>(</del>±)

TABLE XXX

# TEST DATA ON COMBINATION NO. 2 (ORIGINAL)

Regime 1:	Run at 25°C by error instead of 100°C; cells	were discontinued and replaced with new ones.	•	Regime 2:	Run at the original 1.2 A discharge rate modified	by NASA to 0.9 A; cells were discontinued and	replaced with new ones.		
2 A)	223	•	84 (1.4)					84	(+)
Regime 2 (1.2 A)	222		89 (1.3)					89	(+)
 Reg	221		59 (1.4)					59	(+)
 (2)	213		104 (1.9)	200 (1.4)				200	(+)
Regime 1 (25°C)	212		104 (1.4)   104 (1.9)   59 (1.4)   89 (1.3)   84 (1.4)	179 (1.4) 200 (1.4)				179	(+)
Reg	211		104 (1.6)	125 (1.4)				125	(+)
	Cell No.	Capacity Checks	1. N(Q)	2. N(Q)	3. N(Q)	4. N(Q)	5. N(Q)	Status Cycle	Failure Mode

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. II ΤF

Catastrophic Failure - Cell cannot accept charge or cycle. 11 CF

Cycle Number (Capacity) 11 (a)N

Cell still cycling when stopped at indicated cycle. 11 <del>(</del>+

TABLE XXXI

# TEST DATA ON COMBINATION NO. 3 (ORIGINAL)

Regime 1:	Run at 25°C by error instead of 100°C; cells	were discontinued and		Regime 2:	Run at the original 1.2 A	by NASA to 0.9 A; cells	replaced with new ones.		
. 2 A)	323	•	53 (1.4)					53	(+)
Regime 2 (1.2 A)	322		118(1.4)					118	(±)
Reg	321		118(1.2)				:	118	(+)
°C)	313		51 (2.0) 100 (1.7) 118(1.2) 118(1.4) 53 (1.4)					100	(+)
Regime 1 (25 <sup>o</sup> C)	312		51 (2.0)	120 (1.5)	<del></del>	· · · · · ·		120	(+)
Reg	311		100 (1.4)					100	(+)
	Cell No.	Capacity Checks	1. N(Q)	2. N(Q)	3. N(Q)	4. N(Q)	5. N(Q)	Status Cycle	Failure Mode

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. Ц TF

Catastrophic Failure - Cell cannot accept charge or cycle. н  $\mathbf{CF}$ 

Cycle Number (Capacity) 11 (Q)Z

Cell still cycling when stopped at indicated cycle. 11 <del>(</del>+)

TABLE XXXII

# TEST DATA ON COMBINATION NO. 4 (ORIGINAL)

Regime 2 (1.2 A) Regime 1:	421 422 423 Run at 25°C by error instead of 100°C; cells	were discontinued and replaced with new ones.	104 (1.4)   104 (1.5)   89 (1.1)   54 (1.7)   86 (1.3)	Regime 2:	Run at the original 1.2 A discharge rate modified	by NASA to 0.9 A; cells were discontinued and	replaced with new ones.	89   54   86	
-,,-,-			) 89 (1.1) 54 (						(+)
413	211		104(1.5	178(1.2				178	(+)
	412		104 (1.4)	200(1.2) 178(1.2)				200	(1)
Reg	411		104(1.5)					104	
	Cell No.	Capacity Checks	1. N(Q)	2. N(Q)	3. N(Q)	4. N(Q)	5. N(Q)	Status Cycle	

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. 'n  $\mathrm{TF}$ 

Catastrophic Failure - Cell cannot accept charge or cycle. 11 CF

Cycle Number (Capacity) ij (Ø)N

Cell still cycling when stopped at indicated cycle. 11 <del>(+)</del>

TABLE XXXIII

PRECYCLING TEST DATA Combination No. 1 (Repeat)

le 4 A)	Plateau Voltage	1.20 V	1.17 V	1.13 V	1.19 V	1.13 V	1.10 V	1,15 V
Cycle 4 (3 A)	Output	1.26 V 1.1 Ah 1.20 V	1.21 V 1.1 Ah	1.0 Ah	1.3 Ah	1.0 Ah	1.18 V 1.0 Ah	1.1 Ah
Cycle 3 (1.5 A)	Plateau Voltage	1.26 V	1.21 V	1.20 V	1.27 V	1.20 V	1.18 V	2.3 Ah 1.50 V 2.0 Ah 1.38 V 1.5 Ah 1.22 V 1.1 Ah 1.15 V
Cyc (1.	Output	1.5 Ah	1.4 Ah	1.4 Ah	1.7 Ah	1.37 V 1.3 Ah	1.36 V 1.4 Ah	1.5 Ah
Cycle 2 (0.6 A)	Plateau Voltage	1,38 V	1.37 V	1.37 V	1.40 V	1.37 V	1.36 V	1,38 V
Cyc (0.6	Output	2.0 Ah	2.0 Ah	1.8 Ah	2. 1 Ah	1.9 Ah	2.0 Ah	2.0 Ah
Cycle 1 (30 mA)	Plateau Voltage	2.3 Ah 1.50 V 2.0 Ah	2.3 Ah 1.50 V	1.51 V	1.50 V	2.3 Ah   1.51 V	2.3 Ah   1.51 V   2.0 Ah	1,50 V
Cycle 1 (30 mA)	Output	2.3 Ah	2.3 Ah	2.3 Ah	2.3 Ah	2.3 Ah	2.3 Ah	2.3 Ah
rmation (0.6 A)	Plateau Voltage	1.39 V	1.39 V	1.39 V	1.39 V	1,39 V	1,38 V	1.39 V
Formation (0.6 A)	Output	2.2 Ah	2.1 Ah	2.1 Ah	2.2 Ah	2.2 Ah	2.1 Ah	2.15 Ah 1.39 V
	Cell Number	111 A	112 A	113 A	121 A	122 A	123 A	Average

TABLE XXXIV

PRECYCLING TEST DATA Combination No. 2 (Repeat)

	Form (0.	Formation (0.6 A)	Cyc (301	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
. 211 A	2.2 Ah	1.40 V	2.5 Ah	1	1.52 V 2.1 Ah 1.37 V	1.37 V	2.0 Ah	2.0 Ah 1.24 V	1.0 Ah	1.0 Ah 1.17 V
212 A	2. 1 Ah	1.39 V	2.5 Ah	1.52 V	1.9 Ah	1.36 V	1.9 Ah	1.9 Ah 1.27 V	1.0 Ah	1.18 V
213 A	2.2 Ah	1,38 V	2.5 Ah	1,52 V	2.0 Ah	1.38 V	1.4 Ah	1.4 Ah 1.20 V	1.0 Ah	1.0 Ah 1.15 V
221 A	2.2 Ah	1,38 V	2.5 Ah	1,51 V	1.51 V 2.1 Ah	1,35 V	1.6 Ah	1.6 Ah 1.23 V	0.9 Ab	1.08 V
222 A	2.2 Ah	1,38 V	2.4 Ah	1,52 V	2.0 Ah	1.36 V	1.4 Ah	1.18 V	0.9 Ah	1.08 V
223 A	2.0 Ah	1.40 V	2.5 Ah	1.52 V	1.52 V 1.8 Ah	1.42 V	1.9 Ah	1.9 Ah 1.25 V	1.2 Ah	1.2 Ah 1.15 V
Average	2.2 Ah	1.39 V	2.5 Ah	1, 52 V	1.52 V 2.0 Ah 1.37 V 1.7 Ah 1.23 V	1.37 V	1.7 Ah	1.23 V	1.0 Ah	1.0 Ah 1.14 V

TABLE XXXV

Combination No. 3 (Repeat)

	Form (0.	Formation (0.6 A)	Cycle (30 mA	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cyc (1. !	Cycle 3 (1.5 A)	Cycle 4 (3 A)	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
311 A	2.3 Ah	2.3 Ah 1.39 V	2.3 Ah	2.3 Ah 1.52 V 2.0 Ah	2.0 Ah	1,38 V	1.5 Ah 1.24 V	1.24 V	1.0 Ah	1.0 Ah 1.22 V
.312 A	2.1 Ah	1.39 V	2.3 Ah	2.3 Ah 1.52 V 2.0 Ah	2.0 Ah	1.36 V	1.3 Ah	1.19 V	0.9 Ah	0.9 Ah 1.12 V
313 A	2.1 Ah	1.39 V	2.3 Ah	2.3 Ah 1.51 V 2.1 Ah	2.1 Ah	1.38 V	1.6 Ah	1, 19 V	1.0 Ah	1.16 V
321 A	2.1 Ah	1.38 V	2.3 Ah	2.3 Ah   1.51 V   1.9 Ah	1.9 Ah	1.35 V	1.2 Ah	1.18 V	1.0 Ah	1.10 V
322 A	2.2 Ah	1.39 V	2.3 Ah	2.3 Ah 1.51 V 2.0 Ah	2.0 Ah	1.38 V	1.4 Ah	1.19 V	1.0 Ah	1.14 V
323 A	2.2 Ah	1.39 V	2,3 Ah	2.3 Ah 1.51 V 2.1 Ah	2.1 Ah	1.38 V	1.38 V 1.5 Ah 1.21 V	1,21 V	1.0 Ah	1.0 Ah 1.18 V
Average	2.2 Ah	1,39 V	2.3 Ah	2.3 Ah 1.51 V 2.0 Ah	2.0 Ah	1.37 V	1.37 V 1.4 Ah 1.20 V	1.20 V	1.0 Ah	1.0 Ah 1.15 V

TABLE XXXVI

PRECYCLING TEST DATA Combination No. 4 (Repeat)

For:	Formation (0.6 A)	Cycle 1 (30 mA)	le 1 nA)	Cycle 2 (0.6 A)	Cycle 2 (0.6 A)	Cycle 3 (1.5 A)	le 3 5 A)	Cycle (3 A)	Cycle 4 (3 A)
Plateau Output Voltage	Ö	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
2.2 Ah 1.39 V	2	.4 Ah	1.51 V	2.4 Ah 1.51 V 2.2 Ah 1.40 V	1.40 V	1.8 Ah 1.26 V	1,26 V	1.1 Ah	1.1 Ah 1.13 V
2.2 Ah   1.36 V   2	_ 7	2.4 Ah	1.51 V	1.51 V 2.0 Ah	1.37 V	1.3 Ah	1.20 V	0.9 Ah	1, 13 V
2.2 Ah   1.37 V   2	-	2.4 Ah		1.51 V 2.1 Ah	1.39 V	1.5 Ah 1.24 V	1.24 V	0.9 Ah	1.16 V
2.3 Ah   1.38 V   2	-	2.3 Ah	1.51 V   1.9 Ah	1.9 Ah	1.37 V	1.3 Ah 1.23 V	1.23 V	0.9 Ah	1, 16 V
2.2 Ah   1.39 V   2		2.4 Ah	1.52 V 2.0 Ah	2.0 Ah	1.39 V	1.3 Ah 1.22 V	1.22 V	1.0 Ah	1, 18 V
2.2 Ah 1.38 V 2	-	.4 Ah	1,51 V	2.4 Ah 1.51 V 2.0 Ah	1,38 V	1.5 Ah 1.22 V	1.22 V	1.0 Ah	1, 18 V
2.2 Ah 1.38 V 2		.4 Ah	1.51 V	2.4 Ah 1.51 V 2.0 Ah 1.38 V	1,38 V	1.5 Ah	1.5 Ah   1.23 V	0.9 Ah	0.9 Ah 1.16 V

their respective code to indicate that the tests are carried out on repeat cells of the same design.

### Automatic Cycling

The data are presented in Tables XXXVII to XLI. The status of each cell at the end of the program is also indicated.

### Control Group B and Combinations 5 through 12

This category used the separator 3420-25. The manual deep cycles presented in Tables XLII through L give mixed results. As these cells were the first built with the rigid separator 3420-25, the charge regime of constant current to a cut-off voltage of 2.10 V appeared to be excessive for this separator (it is known that zinc penetration is promoted by overcharge). Consequently, about half of the cells shorted between two and five cycles. The cells that reached five cycles safely were not considered worth placing on automatic cycling.

### Combinations No. 13 to 20

In this category, the fabrication reverted to the separator 3420-09.

### Manual Cycling

The data of the manual deep cycles are presented in Tables LI through LVIII.

### Automatic Cycling

The data are presented in Tables LIX through LXVI with the status of each cycling cell at the end of the program.

### Failure Analysis

The zinc electrode degradation is due to two factors — loss of active material with cycling, and reduction of efficiency of the overall electrode material. It was, therefore, necessary to determine the extent of each one.

The physical loss of active material was determined by comparing the original weight with the final weight after the cell had failed. All weights were compared on a ZnO basis. The percentage (5%) of residual active material was thus computed.

TABLE XXXVII

## TEST DATA ON SERIES A

### Control Electrode

		Regime 1			Regime 2	:		Regime 3	
Cell No.	A-11	A-12	A-13	A-21	A-22	A-23	A-31	A-32	A-33
Capacity Checks									
1. N(Q)	107 (1.0) 107	107 (1.5)	107 (1.7)	104(1.1)	104 (0.8)	(1.5)   107 (1.7)   104 (1.1)   104 (0.8)   104 (0.9)   28 (2.0)   28 (2.0)   28 (2.1)	28 (2.0)	28 (2.0)	28(2.1)
2. N(Q)	205(0.2)	205	205 (0.4)	204 (0.7)	204 (0.5)	(0.5) 205(0.4) 204(0.7) 204(0.5) 204(0.7) 58(1.0) 60(1.2) 63(1.4)	58 (1.0)	60(1.2)	63 (1.4)
3. N(Q)		303 (0.2)	302 (0.2)	308 (0.6)	307 (0.5)	307(0.6)			
4. N(Q)				403 (0.8)	402 (0.6) 402 (0.8)	402 (0.8)			
5. N(Q)				503 (0.6)	503 (0.6)   502 (0.4)   502 (0.4)	502 (0.4)			
6. N(Q)				598 (0.6)	:				
Status Cycle	236	303	302	298	502	502	58	09	£9
Failure Mode	TF	TF	TF	(+)	TF	TF	TF	£L	ЯL

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. н ΉH

Catastrophic Failure - Cell cannot accept charge or cycle. н GF

N(Q) = Cycle Number (Capacity)

(+) = Cell still cycling at end of program.

TABLE XXXVIII

# TEST DATA ON COMBINATION NO. 1

		Dogimo 1			Regime 2			Regime 3	
		TACETING			0				
Cell No.	1111A	112A	113A	121A	122A	123A	131	132	133
Capacity Checks									
1. N(Q)	100(1.2)	100 (1.2)   100 (1.1)   100 (1.1)   101 (1.4)   101 (1.2)   101 (1.3)	100(1.1)	101(1.4)	101 (1.2)	101 (1.3)		31 (1.7) 31 (1.7)	
2. N(Q)	199 (1.4)	199 (1.4)   199 (1.4)   199 (1.4)   201 (1.5)	199 (1.4)	201 (1.5)	199 (1.3)   193 (1.4)	193 (1.4)		38(1.5)	60 (1.7)
3. N(Q)	299 (1.2)	299 (1.2) 299 (0.4) 299 (0.4) 303 (1.4) 301 (1.4) 295 (1.1)	299 (0.4)	303 (1, 4)	301 (1.4)	295(1.1)	88 (2. 1)   46 (1. 4)	46 (1.4)	88 (1.8)
4. N(Q)	400 (0.6)	400 (0.6) 400 (0.4) 400 (0.4) 403 (0.6) 401 (0.5) 393 (0.6) 118 (1.4)	400 (0.4)	403 (0.6)	401 (0.5)	393 (0.6)	118(1.4)		124 (1.6)
5. N(Q)	498 (0.1)	498 (0.1) 500 (0.1) 500 (0.2) 503 (0.5) 501 (0.6) 492 (0.8)	500 (0.2)	503 (0.5)	501 (0.6)	492 (0.8)			
6. N(Q)			-	591 (0.4)	591 (0.4) 606 (0.7)	592 (0.4)			<del></del>
7, ' N(Q)					635(0.5)				
Status Cycle	498	500	500	591	635	592	118	46	124
Failure Mode	TF	TF	TF	TF	TF	J.L	TF	TF	(+)
1									

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. ΤF

Catastrophic Failure - Cell cannot accept charge or cycle. П GF

N(Q) = Cycle Number (Capacity)

(+) = Cell still cycling at end of program.

TABLE XXXIX

TEST DATA ON COMBINATION NO. 2

		Regime 1			Regime 2			Regime 3	
Cell No.	211A	212A	213A	221A	222A	223A	231	232	233
Capacity Checks 1. N(Q)	100 (1, 9)	100 (1.9) 100 (1.7) 100 (1.9)	100 (1.9)	79 (1.5)	101 (1.5)	79 (1.5) 101 (1.5) 100 (1.2) 31 (1.7) 31 (1.7) 31 (1.6)	31 (1.7)	31 (1.7)	31 (1.6)
2. N(Q)	199 (1.9)	199 (1.7) 199 (1.8)	199 (1.8)	101 (1.5) 203 (1.4) 202 (0.7) 60 (1.8) 51 (1.5)	203(1.4)	202 (0.7)	60 (1.8)	51 (1.5)	53 (1.7)
3. N(Q)	299 (0.5)	299 (0.2) 299 (0.5)	299 (0.5)	194 (1.1)   306 (1.1)   301 (0.8)	306 (1.1)	301 (0.8)		90(1.4) 60(1.5)	60 (1.5)
4. N(Q)	400 (0.4)		400(0.3)	297 (0.9) 406 (0.6)	406 (0.6)	400 (1.0)			71 (1.4)
5. N(Q)	499 (0.2)		500 (0.2)	500 (0.2) 397 (0.5) 495 (0.9)	495 (0.9)	500 (0.5)			<del>- 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1 - 1</del>
6. N(Q)				486 (0.8)	595 (0.8)				
7. N(Q)				586 (0.5) 687 (0.5)	687 (0.5)				
Status Cycle	499	299	500	629	289	500	06	62	71
Failure Mode	TF	TF	TF	$\mathrm{TF}$	TF	TF	TF	TF	TF

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. TF

Catastrophic Failure - Cell cannot accept charge or cycle. 11 CF

N(Q) = Cycle Number (Capacity)

TABLE XL

TEST DATA ON COMBINATION NO. 3

		Regime 1		K	Regime 2			Regime 3	
Cell No.	311A	312A	. 313A	321A	322A	323A	331	332	333
Capacity Checks  1. N(Q)  2. N(Q)  3. N(Q)  4. N(Q)  5. N(Q)  6. N(Q)  7. N(Q)	100 (1.1) 199 (1.7) 299 (0.6) 388 (0.4) 487 (0)		97 (1.1) 100 (1.2) 199 (1.7) 199 (1.5) 299 (0.4) 299 (0.2) 388 (0.3) 487 (0)		77 (1.3) 101 (1.3) 190 (1.4) 288 (1.4) 392 (0.6) 492 (0.8) 593 (0.4)	101 (1.1) 193 (1.4) 294 (1.4) 398 (0.6) 498 (1.0) 598 (0.5)	31(1.7) 60(1.8) 91(1.5) 121(1.3)	31(1.7) 31 (1.5) 31 (1.7) 60(1.8) 36 (1.4) 57 (1.4) 91(1.5) 21(1.3)	31 (1.7) 57 (1.4)
Status Cycle	487	487	299	594	593	630	121	36	57
Failure Mode	CF	CF	TF	TF	TF	TF	TF	TF	TF

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. ΤF

Catastrophic Failure - Cell cannot accept charge or cycle.

N(Q) = Cycle Number (Capacity)

TABLE XLI

TEST DATA ON COMBINATION NO. 4

		Regime 1		<u></u>	Regime 2			Regime 3	
Cell No.	411A	412A	413A	421A	422A	423A	431	432	433
Capacity Checks  1. N(Q)  2. N(Q)  3. N(Q)  4. N(Q)  5. N(Q)  6. N(Q)  7. N(Q)	100 (2. 1) 100 ( 199 (1.6) 199 ( 286 (0) 299 (		1.7) 100 (1.9) 1.1) 199 (1.5) 0.1) 299 (0.2)	101 (1.6) 203 (1.0) 302 (0.6) 402 (0.5) 493 (0.8) 581 (0.4)	101 (1.6) 101 (1.4) 101 (1.0) 203 (1.0) 203 (1.2) 198 (0.9) 302 (0.6) 303 (0.6) 297 (0.6) 402 (0.5) 403 (0.5) 395 (0.6) 493 (0.8) 493 (1.0) 485 (0.8) 581 (0.4) 594 (0.6) 570 (0.5)	101 (1.0) 198 (0.9) 297 (0.6) 395 (0.6) 485 (0.8) 570 (0.5)	31 (1.7) 33 (1.8) 42 (1.6) 52 (1.5)	31 (1.7) 38 (1.7) 45 (1.6) 48 (1.4)	31 (1.7) 50 (1.4)
Status Cycle	286	299	565	581	959	570	52	48	50
Failure Mode	CF	TF	TF	TF	TF	TF	TF	TF	TF

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. #1 ΤF

Catastrophic Failure - Cell cannot accept charge or cycle. CF =

N(Q) = Cycle Number (Capacity)

TABLE XLII

### PRECYCLING TEST DATA Control Group B (3420-25)

	Forn (0.	Formation (0.6 A)	Cycle 1 (30 mA)	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
B-11	2.1 Ah	1.44 V	2.5 Ah	1, 52 V	2.0 Ah	1,45 V	1.8 Ah	1.37 V	1.8 Ah	1.27 V
B-12	2.0 Ah	1.44 V	2, 5 Ah	1.52 V	2.0 Ah	1.44 V	1.6 Ah	1.36 V	1.4 Ah	1.26 V
B-13	2.1 Ah	1,44 V	2.5 Ah	1.52 V	2.0 Ah	1,43 V	1.6 Ah	1.34 V	1.4 Ah	1.24 V
B-21	2.1 Ah	1.44 V	2.5 Ah	1.52 V	1.8 Ah	1.43 V	1.6 Ah	1.33 V	1.6 Ah	1.25 V
B-22	2.1 Ah	1.44 V	2.5 Ah	1,52 V	2.0 Ah	1.45 V	1.8 Ah	1.36 V	1.6 Ah	1.27 V
B-23	2.0 Ah	1.44 V	2.5 Ah	1.52 V	1.8 Ah	1.43 V	1.6 Ah	1.33 V	1.4 Ah	1.24 V
B-31	2.0 Ah	1.44 V	2.5 Ah	1.52 V	1.6 Ah	1.41 V	1.6 Ah	1.33 V	1.2 Ah	1.23 V
B-32	2.0 Ah	1.44 V	2.6 Ah	1.52 V	1.9 Ah	1,43 V	1.6 Ah	1.34 V	1.4 Ah	1.25 V
B-33	2, 1 Ah	1.44 V	2.5 Ah	1.52 V	2.0 Ah	1,43 V	1.9 Ah	1,36 V	1.5 Ah	1.26 V
Average	2, 1 Ah	1,44 V	2.5 Ah	1,52 V	1.9 Ah	1,43 V	1.7 Ah	1.34 V	1.4 Ah	1.25 V

TABLE XLIII

	Form (0.	Formation (0.6 A)	Cycle 1 (30 mA)	le l nA)	Cycle 2 (0.6 A)	le 2 A)	Cyc (1.!	Cycle 3 (1.5 A)	Cycle 4 (3 A)	le 4 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
511	2.1 Ah	1.42 V	2.4 Ah	1.51 V	1.8 Ah	1,43 V	1.6 Ah	1,36 V	1.4 Ah	1.24 V
512*	2.2 Ah	1.43 V	2.4 Ah	1.51 V	1.7 Ah	1.43 V	1.7 Ah	1.37 V	1.5 Ah	1.24 V
513*	2.3 Ah	1.44 V	2.3 Ah	1.51 V	2.0 Ah	1,43 V	2.1 Ah	1.37 V	1.7 Ah	1.23 V
521	2.2 Ah	1.44 V	2.3 Ah	1.51 V	2.1 Ah	1.44 V	2.0 Ah	1.39 V	1.8 Ah	1.25 V
522*	2.2 Ah	1.43 V	2.3 Ah	1.51 V	1.7 Ah	1.43 V	1.5 Ah	1.36 V	*	
523	2.2 Ah	1.44 V	2.3 Ah	1.51 V	1.9 Ah	1,44 V	1.7 Ah	1.37 V	0.6 Ah	1.20 V
531*	2.0 Ah	1.44 V	2.4 Ah	1.51 V	2.0 Ah	1,44 V	2.0 Ah	1,37 V	1.7 Ah	1.25 V
532	2.2 Ah	1.44 V	2.4 Ah	1,51 V	1.7 Ah	1.44 V	1.6 Ah	1.39 V	1.1 Ah	1.24 V
533*	2.2 Ah	1,45 V	2.4 Ah	1.51 V	*					
Average	2.2 Ah	1.44 V	2.3 Ah	1.51 V	1.9 Ah	1.44 V	1.8 Ah	- 1	1.37 V 1.4 Ah 1.24 V	1.24 V

\* Failed on recharge at indicated cycle or after last cycle.

TABLE XLIV
PRECYCLING TEST DATA
Combination No. 6

	Form (0.	Formation (0.6 A)	Cycle (30 mA	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
611*	2.2 Ah	1.44 V	2.4 Ah	1, 52 V	1.6 Ah	1,42 V	1.1 Ah	1,35 V	*	
612*	2.1 Ah	1.44 V	2.5 Ah	1.52 V	1.6 Ah	1.42 V	1.3 Ah	1.34 V	0.9 Ah 1.21 V	. 1.21 V
613	2. 1 Ah	1.44 V	2.5 Ah	1.52 V	1.7 Ah	1.42 V	1.1 Ah	1.32 V	0.8 Ah	1.20 V
621*	2.2 Ah	1.44 V	2.4 Ah	1.52 V	1.5 Ah	1.41 V	1.4 Ah	1.34 V	*	
622*	2.2 Ah	1.45 V	2.3 Ah	1.52 V	1.7 Ah	1.42 V	1.3 Ah	1.34 V	*	
623*	2.1 Ah	1.41 V	2.4 Ah	1.52 V	1.9 Ah	1.43 V	1.3 Ah	I,35 V	*	
631*	2. l Ah	1.44 V	2.4 Ah	1.52 V	1.8 Ah	1,42 V	1.3 Ah	1.35 V	*	<del>,                                    </del>
632	2.2 Ah	1.40 V	2.4 Ah	1.51 V	1.8 Ah	1,43 V	1.2 Ah	1.35 V	*	
633	2.1 Ah	1.44 V	2.5 Ah	1.52 V	1.8 Ah	1.44 V	1.4 Ah	1,30 V	0.9 Ah	1.22 V
Average	2.2 Ah	1.43 V	2.4 Ah	1,52 V	1.7 Ah	1,42 V	1.3 Ah	1.34 V	0.9 Ah	1, 21 V

 $^{st}$  Failed on recharge at indicated cycle or after last cycle.

TABLE XLV

PRECYCLING TEST DATA

	Form (0.	Formation (0.6 A)	Cycle 1 (30 mA)	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0,6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
711	2.3 Ah	1,44 V	2.3 Ah	1.51 V	2. 1 Ah	1,44 V	1.7 Ah	1,36 V	1.7 Ab	1,20 V
712	2.3 Ah	1.45 V	2.3 Ah	1.51 V	2.1 Ah	1.44 V	2.0 Ah	1.37 V	1.7 Ah	1.22 V
713	2.3 Ah	1.44 V	2.3 Ah	1.51 V	2.0 Ah	1.44 V	1.4 Ah	1.26 V	0.8 Ah	1, 18 V
721	2.3 Ah	1.45 V	2.3 Ah	1.51 V	1.8 Ah	1.44 V	1.2 Ah	1.30 V	1.1 Ah	1.20 V
722	2.3 Ah	1.44 V	2.3 Ah	1.51 V	1.8 Ah	1.44 V	1.5 Ah	1.33 V	1.2 Ah	1.21 V
723	2.3 Ah	1.44 V	2.3 Ah	1.51 V	2.0 Ah	1.44 V	1.5 Ah	1.32 V	1.4 Ah	1.21 V
731	2.3 Ah	1.45 V	2.3 Ah	1,51 V	1.9 Ah	1.44 V	1.4 Ah	1.34 V	0.5 Ah	1.20 V
732	2.3 Ah	1.45 V	2.3 Ah	1.51 V	2.1 Ah	1.44 V	1.8 Ah	1.36 V	1.6 Ah	1.22 V
733	2.3 Ah	1.45 V	2.4 Ah	1,51 V	1.9 Ah	1.46 V	1.9 Ah	1,39 V	1,3 Ah	1.20 V
Average	2.3 Ah	1.45 V	2.3 Ah	1.51 V	2.0 Ah 1.44 V	1.44 V	1.6 Ah	1.6 Ah 1.34 V	1.3 Ah	1.3 Ah 1.21 V

TABLE XLVI

	Forn (0.	Formation (0.6 A)	Cycle 1 (30 mA)	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0,6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
811*	2.2 Ah	1.45 V	2.4 Ah	1.53 V	*					
812*	2.1 Ah	1.45 V	2.4 Ah	1,53 V	*					
813*	2.2 Ah	1.45 V	2.4 Ah	1.53 V	1.4 Ah	1,43 V	1. 1 Ah	1.25 V	*	
821*	2.0 Ah	1.46 V	2.4 Ah	1.52 V	*	· · · · · · · · · · · · · · · · · · ·				
822*	2.3 Ah	1.45 V	2.4 Ah	1.52 V	1.5 Ah	1.43 V	1.1 Ah	1.22 V	*	<del>Maria da Para da</del>
823*	2.3 Ah	1.45 V	2.4 Ah	1.53 V	1.7 Ah	1.43 V	1.2 Ah	1,30 V	*	
831*	2.2 Ah	1.46 V	2.4 Ah	1,53 V	1.5 Ah	1.44 V	1.1 Ah	1.21 V	*	<u> </u>
832*	2.3 Ah	1.45 V	2.2 Ah	1, 53 V	1.7 Ah	1.43 V	1.7 Ab	1.36 V	*	
833*	2.1 Ah	1.44 V	2.4 Ah	1, 53 V	1.8 Ah	1.46 V	1.4 Ah	1.38 V	*	
Average	2.2 Ah	1.45 V	2.4 Ah	1,53 V	1.6 Ah	1.44 V	1.3 Ah	1.29 V		

 $^{st}$  Failed on recharge at indicated cycle or after last cycle.

TABLE XLVII

Cycle 4 (3 A)	Plateau Voltage	1.21 V		1.24 V		ing and a second	1.20 V	1.21 V		1.22 V	1.22 V
Cyc (3	Output	1.5 Ah	*	1.1 Ah			0.9 Ah	0.9 Ah	*	1.0 Ah	1.30 V 1.1 Ah 1.22 V
Cycle 3 (1.5 A)	Plateau Voltage	1.36 V	1.37 V	1,31 V			1.26 V	1.28 V	1.37 V	1.25 V	1.30 V
$^{\mathrm{Cyo}}_{(1.}$	Output	2.0 Ah	2.0 Ah	1.4 Ah	*	*	1.2 Ah	1.5 Ah	2.2 Ah	1. 1 Ah	1.44 V 1.6 Ah
Cycle 2 (0.6 A)	Plateau Voltage	1,45 V	1.44 V	1.44 V	1.45 V	1.45 V	1.45 V	1.45 V	1.44 V	1.44 V	1.44 V
Cyc (0.6	Output	1.9 Ah	2.1 Ah	1.4 Ah	1.8 Ah	2.0 Ah	1.8 Ah	1.8 Ah	2.0 Ah	1.7 Ah	1.8 Ah
Cycle 1 (30 mA)	Plateau Voltage	1,52 V	1,51 V	1.51 V	1.52 V	1, 52 V	1,52 V	1.52 V	1.52 V	1.52 V	1.52 V 1.8 Ah
Cycle (30 mA	Output	2.6 Ah	2.8 Ah	2.7 Ah	2.7 Ah	2.6 Ah	2.8 Ah	2.7 Ah	2.7 Ah	2.7 Ah	2.7 Ah
Formation (0.6 A)	Plateau Voltage	1.40 V	1.40 V	1,38 V	1.42 V	1.41 V	1.42 V	1.38 V	1.40 V	1.42 V	1.40 V
Form (0.	Output	1.9 Ah	1.3 Ah	1.7 Ah	1.8 Ah	2.0 Ah	1.8 Ah	1.7 Ah	1.2 Ah	1.9 Ah	1.7 Ah
	Cell Number	911	912*	913	921*	922*	923	931	932*	933	Average

 $^{st}$  Failed on recharge at indicated cycle or after last cycle.

TABLE XLVIII

	Form (0.	Formation (0.6 A)	Cycle 1 (30 mA)	le l nA)	Cycle 2 (0.6 A)	Cycle 2 (0.6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
1011*	1.9 Ah	1,41 V	2.5 Ah	1.52 V	1.4 Ah	1,44 V	2.1 Ah	1,38 V	*	
1012	2.0 Ah	1.42 V	2.6 Ah	1.51 V	2.0 Ah	1.45 V	2.0 Ah	1.38 V	1.8 Ah	1.28 V
1013	1.9 Ah	1.43 V	2.6 Ah	1.52 V	2.0 Ah	1.45 V	2.3 Ah	1.38 V	2.0 Ah	1.27 V
.1021	1.9 Ah	1.41 V	2.6 Ah	1.52 V	2.0 Ah	1.45 V	2.3 Ah	1.38 V	1.9 Ah	1.27 V
1022	1.8 Ah	1.41 V	2.8 Ah	1.51 V	2.0 Ah	1.45 V	2.3 Ah	1.38 V	2.0 Ah	1.28 V
1023	2.0 Ah	1.41 V	2.6 Ah	1.52 V	1.6 Ah	1,45 V	*			
1031*	2.1 Ah	1.40 V	2.8 Ah	1,51 V	1.9 Ah	1.45 V	2.0 Ah	1.37 V	*	
1032*	1.9 Ah	1.42 V	2.6 Ah	1.52 V	1.9 Ah	1.45 V	2.1 Ah	1.39 V	*	
1033	2.0 Ah	1.42 V	2.5 Ah	1.52 V	1.8 Ah	1.45 V	*			
Average	1.9 Ah	1.41 V	2.6 Ah	1,52 V	1.9 Ah	1,45 V	2.2 Ah	1,38 V	1.9 Ah	1.28 V

\* Failed on recharge after indicated cycle or last cycle.

TABLE IL
PRECYCLING TEST DATA
Combination No. 11

Cycle 4 (3 A)	Plateau Voltage			1.26 V		,	1.26 V				1.6 Ah 1.26 V
Cyc (3	Output			1.6 Ah		*	1, 5 Ah	*		-	1.6 Ah
Cycle 3 (1.5 A)	Plateau Voltage			1.39 V		1.38 V	1.38 V	1.37 V			1.38 V
Cyo (1.	Output	*	*	2.2 Ah	*	1.7 Ah	2.2 Ah	1.7 Ah	*	*	2.0 Ah
Cycle 2 (0,6 A)	Plateau Voltage	1,45 V	1.45 V	1.45 V	1.45 V	1.45 V	1.45 V	1.45 V	1.45 V	1.45 V	1,45 V
Cyc (0.6	Output	1.9 Ah	2.3 Ah	2. 1 Ah	2.1 Ah	2. 1 Ah	2.3 Ah	2.0 Ah	1.8 Ah	2.3 Ah	2. 1 Ah
Cycle 1 (30 mA)	Plateau Voltage	1,53 V	1.52 V	1.52 V	1.52 V	1.52 V	1.52 V	1.52 V	1.52 V	1.52 V	1, 52 V
Cycle (30 mA	Output	2.5 Ah	2.5 Ah	2.4 Ah	2.5 Ah	2.5 Ah	2.5 Ah	2.5 Ah	2.6 Ah	2.4 Ah	2.5 Ah
Formation (0.6 A)	Plateau Voltage	1.44 V	1.44 V	1.44 V	1.44 V	1.44 V	1.45 V	1.44 V	1.44 V	1.44 V	1.44 V
Form (0.	Output	2. 1 Ah	2.3 Ah	2.2 Ah	2. l Ah	2.1 Ah	2.3 Ah	2.2 Ah	2.1 Ah	2.1 Ah	2.2 Ah
	Cell Number	1111	1112*	1113	1121*	1122*	1123	1131*	1132*	1133*	Average

 $^{st}$  Failed on recharge after indicated cycle or last cycle.

TABLE L

	Form (0.	Formation (0.6 A)	Cycle 1 (30 mA)	le l nA)	Cyc (0.6	Cycle 2 (0,6 A)	Cyc (1.	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Cell Number	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage	Output	Plateau Voltage
1211	2. 1 Ah	1.45 V	2.5 Ah	1. 52 V	1.8 Ah	1.43 V	1.4 Ah	1,31 V	1.2 Ah	1, 19 V
1212*	2.2 Ah	1.45 V	2.5 Ah	1,53 V	1.4 Ah	1.45 V	*			
1213*	2. 1 Ah	1.46 V	2.5 Ah	I, 52 V	1.9 Ah	1.45 V	*			
1.221*	2.0 Ah	1,45 V	2.4 Ah	1, 53 V	1.6 Ah	1.46 V	1. 1 Ah	1.23 V	*	
1222*	2.2 Ah	1,45 V	2.5 Ah	1,53 V	1.6 Ah	1,45 V	*			
$1223^{*}$	2.2 Ah	1.45 V	2.5 Ah	1,53 V	1,8 Ah	1.44 V	1,5 Ah	1.35 V	*	
1231	2.2 Ah	1.46 V	2.5 Ah	1.53 V	1.4 Ah	1,44 V	1.7 Ah	1.34 V	0.9 Ah	1.21 V
1232*	2.3 Ah	1,45 V	2.5 Ah	1, 53 V	2. 1 Ah	1.44 V	*			
1233*	2.2 Ah	1.45 V	2.5 Ah	1, 53 V	1.9 Ah	1,43 V	1.5 Ah	1,32 V	*	
Average	2.2 Ah	1.45 V	2.5 Ah	1, 52 V	1.7 Ah	1,44 V	1.4 Ah	1,31 V	1.1 Ah	1.20 V

 $^{st}$  Failed on recharge after indicated cycle or last cycle.

TABLE LI

PRECYCLING TEST DATA

	Form (0.6	Formation (0.6 A)	Cyc (30	Cycle 1 (30 mA)	Cyc (0. 6	Cycle 2 (0.6 A)	Cyc (1.5	Cycle 3 (1.5 A)	Cyc (3	Cycle 4 (3 A)
Ce 11 No.	Output (Ah)	Plateau Voltage (V)								
1311	2.0 Ah	1,40 V	2.4 Ah	1.52 V	1.7 Ah	1.35 V	1.5 Ah	1.25 V	1.1 Ah	1.18 V
1312	2.0 Ah	1,39 V	2.3 Ah	1.52 V	1.7 Ah	1.37 V	1.4 Ah	1.26 V	1.0 Ah	1.19 V
1313	2.1 Ah	1.41 V	2.3 Ah	1.52 V	1.7 Ah	1.37 V	1.5 Ah	1.27 V	1.2 Ah	1.24 V
1321	2.1 Ah	1.41 V	2.5 Ah	1.52 V	1.7 Ah	1.34 V	1.2 Ah	1.26 V	1. 1 Ah	1.22 V
1322	2.0 Ah	1.37 V	2.3 Ah	1.52 V	1.5 Ah	1.32 V	1.0 Ah	1.22 V	0.5 Ah	1.12 V
1323	2.1 Ah	1.43 V	2.3 Ah	1.51 V	1.6 Ah	1.37 V	1.2 Ah	1.21 V	1.0 Ah	1.19 V
1331	2.2 Ah	1.43 V	2.3 Ah	1.52 V	1.7 Ah	1.33 V	1.5 Ah	1.24 V	1.1 Ah	1.22 V
1332	2.1 Ah	1.42 V	2.4 Ah	1.52 V	1.6 Ah	1.34 V	1.2 Ah	1.21 V	0.8 Ah	1,15 V
1333	2.2 Ah	1,42 V	2.3 Ah	1.52 V	1.7 Ah	1.35 V	1.2 Ah	1.23 V	1.0 Ah	1.22 V
Avg.	2.1 Ah	1,41 V	2.3 Ah	1.52 V	1.52 V 1.7 Ah	1,36 V	1.3 Ah	1.24 V	1.0 Ah 1.19 V	1.19 V

TABLE LII

	Formation (0.6 A)	ation A)	Cycle 1 (30 mA	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cycle 3 (1.5 A)	le 3 A)	Cycle (3 A)	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
1411	2. 1 Ah	1.41 V	2.3 Ah	1.53 V	1.8 Ah	1.38 V	1.5 Ah	1.25 V	1.2 Ah	1.20 V
1412	2.1 Ah	1.42 V	2.3 Ah	1,51 V	1.5 Ah	1.35 V	1.2 Ah	1.21 V	1.0 Ah	1.17 V
1413	2.1 Ah	1.41 V	2.3 Ah	1.52 V	1.7 Ah	1.40 V	1.4 Ah	1.23 V	1.1 Ah	1.17 V
1421	2.1 Ah	1.42 V	2.3 Ah	1,53 V	1.5 Ah	1.32 V	1.1 Ah	1.18 V	0.9 Ah	1.12 V
1422	1.7 Ah	1.32 V	2.4 Ah	1.51 V	1.7 Ah	1.38 V	1.4 Ah	1.21 V	0.8 Ah	1.11 V
1423	1.8 Ah	1.37 V	2.4 Ah	1.52 V	1,5 Ah	1.33 V	1.2 Ah	1.22 V	1.0 Ah	1, 13 V
1431	2.0 Ah	1.39 V	2.3 Ah	1.52 V	1.7 Ah	1.40 V	1.5 Ah	1.25 V	1.1 Ah	1.16 V
1432	2.0 Ah	1.41 V	2.3 Ah	1.52 V	1.7 Ah	1.36 V	1.5 Ah	1.24 V	1.2 Ah	1.17 V
1433	2.0 Ah	1.38 V	2.3 Ah	1,51 V	1.5 Ah	1.35 V	1.2 Ah	1.22 V	0.9 Ah	1.13 V
Avg.	2.0 Ah	1.39 V	2.3 Ah	1,52 V	1.6 Ah 1.36 V	1,36 V	1.3 Ah	1.3 Ah 1.22 V	1.0 Ah	1.15 V

TABLE LIII

PRECYCLING TEST DATA

	Forn (0.0	Formation (0.6 A)	Cyc (30	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cyc.	Cycle 3 (1.5 A)	Cycle (3 A)	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
1511	2.3 Ah	1,44 V	2.5 Ah	1.54 V	2.0 Ah	1.41 V	1.1 Ah	1.27 V	0.7 Ah	1.09 V
1512	2.3 Ah	1.43 V	2.5 Ah	1.54 V	1.8 Ah	1.39 V	1.2 Ah	1.28 V	0.9 Ah	1.17 V
1513	2.3 Ah	1.42 V	2.5 Ah	1.54 V	2.1 Ah	1.40 V	1.7 Ah	1.30 V	1.2 Ah	1.15 V
1521	2.2 Ah	1.43 V	2.5 Ah	1,53 V	2.0 Ah	1.41 V	1.2 Ah	1.28 V	0.9 Ah	1.10 V
1522	2.1 Ah	1.43 V	2.6 Ah	1.54 V	1.8 Ah	1.39 V	1.1 Ah	1.29 V	0.9 Ah	1.14 V
1523	2.3 Ah	1.43 V	2.4 Ah	1.54 V	2.1 Ah	1.41 V	1.9 Ah	1.31 V	1.5 Ah	1.20 V
1531	2.2 Ah	1.42 V	2.5 Ah	1.54 V	2.1 Ah	1.41 V	1.7 Ah	1,33 V	1.2 Ah	1.17 V
1532	2.2 Ah	1.44 V	2.5 Ah	1.54 V	1.9 Ah	1.40 V	1.2 Ah	1.32 V	1.0 Ah	1.16 V
1533	2. 1 Ah	1.42 V	2.6 Ah	1.54 V	2.0 Ah	1.40 V	1.5 Ah	1.32 V	1.0 Ah	1, 18 V
Avg.	2.3 Ah	1.43 V	2.5 Ah	1.54 V	2.0 Ah 1.40 V	1.40 V	1.4 Ah	1.4 Ah   1.30 V   1.0 Ah   1.15 V	1.0 Ah	1.15 V

TABLE LIV

	Form (0.6	Formation (0.6 A)	Cyc (30	Cycle 1 (30 mA)	Cyc (0. 6	Cycle 2 (0.6 A)	Cycle 3 (1.5 A)	le 3 . A)	Cyc (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
1611	2.1 Ah	1.44 V	2.6 Ah	1.55 V	1.9 Ah	1.42 V	1.4 Ah	1,38 V	1.0 Ah	1.21 V
1612	2.1 Ah	1.44 V	2.5 Ah	1, 54 V	1.8 Ah	1.42 V	1.4 Ah	1.34 V	1.0 Ah	1.16 V
1613	2.1 Ah	1.42 V	2.6 Ah	1.55 V	2.0 Ah	1.42 V	1.2 Ah	1.33 V	1.0 Ah	1.16 V
1621	2.1 Ah	1,43 V	2.6 Ah	1.54 V	1.9 Ah	1.43 V	1.4 Ah	1.34 V	1.1 Ah	1.19 V
1622	2.1 Ah	1.43 V	2.5 Ah	1.55 V	1.7 Ah	1.40 V	1.2 Ah	1.30 V	0.9 Ah	1.14 V
1623	2.1 Ah	1.43 V	2.5 Ah	1.55 V	1.8 Ah	1.42 V	1.1 Ah	1.34 V	0.9 Ah	1.17 V
1631	2.2 Ah	1.44 V	2.5 Ah	1.55 V	1.8 Ah	1.42 V	1.2 Ah	1.35 V	0.9 Ah	1.14 V
1632	2.2 Ah	1.45 V	2.5 Ah	1.55 V	2.0 Ah	1.43 V	1.5 Ah	1.34 V	1. 1 Ah	1.17 V
1633	2. 1 Ah	1.44 V	2.6 Ah	1.55 V	2.0 Ah	1.43 V	1.2 Ah	1.38 V	1.0 Ah	1.20 V
Avg.	2. 1 Ah	1.44 V	2.5 Ah	1.55 V	1.55 V 1.9 Ah 1.42 V	1.42 V	1.3 Ah	1.3 Ah 1.34 V 1.0 Ah	1.0 Ah	1.17 V

TABLE LV

## PRECYCLING TEST DATA

## Combination No. 17

10. 6	5 A)	(30	ile 1 mA)	(0, 6	ie 2 5 A)	(1.5	A)	(3 (3	(3 A)
Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
2.0 Ah	1.39 V	2.3 Ah	1.51 V	2.0 Ah	1.40 V	1.5 Ah	1.32 V	1.2 Ah	1.15 V
2.0 Ah	1.39 V	2.2 Ah	1.52 V	1.9 Ah	1.40 V	1.2 Ah	1.34 V	1.1 Ah	1.16 V
2.2 Ah	1.41 V	2.2 Ah	1.52 V	2.0 Ah	1.41 V	1.5 Ah	1.32 V	1.2 Ah	1.16 V
2.2 Ah	1.40 V	2.3 Ah	1.51 V	2.3 Ah	1.42 V	2.0 Ah	1.34 V	1.4 Ah	1.20 V
2.2 Ah	1.39 V	2.3 Ah	1.52 V	2.0 Ah	1.40 V	1.6 Ah	1.33 V	1.1 Ah	1.17 V
2.3 Ah	1.41 V	2.3 Ah	1.52 V	2.2 Ah	1.42 V	1.8 Ah	1.34 V	1.4 Ah	1.20 V
2.0 Ah	1.40 V	2.3 Ah	1.52 V	2.1 Ah	1.41 V	1.5 Ah	1.34 V	1.2 Ah	1.19 V
2.0 Ah	1.39 V	2.2 Ah	1.52 V	2.0 Ah	1.41 V	1.8 Ah	1.32 V	1.4 Ah	1.16 V
2.2 Ah	1.41 V	2.3 Ah	1.51 V	2. 1 Ah	1.41 V	1.6 Ah	1.33 V	1.2 Ah	1.21 V
2. 1 Ah	1.40 V	2.3 Ah	1.52 V	2. 1 Ah	1.41 V	1.6 Ah	1.33 V	1.2 Ah	1. 18 V
	1 Ah  1 Ah  2 Ah  2 Ah  2 Ah  3 Ah  0 Ah  2 Ah  2 Ah  2 Ah  1 Ah		Plateau Outp (V) (Ah 1.39 V 2.3 1 1.40 V 2.2 1 1.40 V 2.3 1	Plateau (30 1)  Plateau (Ah)  1.39 V 2.3 Ah  1.41 V 2.2 Ah  1.39 V 2.3 Ah  1.40 V 2.3 Ah	Plateau (30 mA)  Plateau (Ah) (Voltage (V)  1.39 V 2.2 Ah 1.52 V  1.41 V 2.3 Ah 1.52 V  1.40 V 2.3 Ah 1.52 V  1.40 V 2.3 Ah 1.52 V  1.41 V 2.3 Ah 1.52 V  1.41 V 2.3 Ah 1.52 V  1.40 V 2.3 Ah 1.52 V	Plateau (30 mA) (0.6 FA) (0.6 FA)  Plateau (Ah) (Voltage (Ah) (Voltage (Ah) (Voltage (Ah) (Ah) (Voltage (Ah) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah)	Plateau (30 mA) (0.6 A)  Plateau (0.6 A)  Plateau (Voltage (Ah) (V) (Ah) (V)  1.39 V 2.3 Ah 1.51 V 2.0 Ah 1.40 V 1.5  1.41 V 2.2 Ah 1.52 V 2.0 Ah 1.42 V 2.0  1.40 V 2.3 Ah 1.52 V 2.0 Ah 1.42 V 2.0  1.40 V 2.3 Ah 1.52 V 2.0 Ah 1.42 V 1.6  1.40 V 2.3 Ah 1.52 V 2.0 Ah 1.41 V 1.6  1.40 V 2.3 Ah 1.52 V 2.0 Ah 1.41 V 1.6  1.40 V 2.3 Ah 1.52 V 2.1 Ah 1.41 V 1.5  1.40 V 2.3 Ah 1.52 V 2.1 Ah 1.41 V 1.6  1.40 V 2.3 Ah 1.52 V 2.1 Ah 1.41 V 1.6  1.40 V 2.3 Ah 1.52 V 2.1 Ah 1.41 V 1.6  1.40 V 2.3 Ah 1.52 V 2.1 Ah 1.41 V 1.6  1.40 V 2.3 Ah 1.52 V 2.1 Ah 1.41 V 1.6	Plateau (1.5 A) (1.5 A) (1.5 A)  Plateau (V) (Ah) (V) (Ah) (V) (Ah) (V) (Ah) (V) (Ah) (V) (Ah) (Ah) (V) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah	Plateau Voltage Output Voltage Output (V) (V) (Ah) (V) (V) (Ah) (V) (V) (Ah) (V) (V) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah) (Ah

TABLE LVI

## PRECYCLING TEST DATA Combination No. 18

	Forn (0.6	Formation (0.6 A)	Cyc (30	Cycle. 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cycle 3 (1.5 A)	le 3 A)	Cyc (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
1811	1.8 Ah	1.38 V	2.3 Ah	1.51 V	1.9 Ah	1.40 V	1.5 Ah	1,35 V	1.1 Ah	1.16 V
1812	1.8 Ah	1.38 V	2.3 Ah	1.52 V	1.8 Ah	1.38 V	1.2 Ah	1.33 V	1.0 Ah	1.15 V
1813	1.7 Ah	1.39 V	2.3 Ah	1.51 V	1.8 Ah	1.37 V	1.2 Ah	1.30 V	0.9 Ah	1.10 V
1821	1.8 Ah	1.40 V	2.3 Ah	1.51 V	1.9 Ah	1.40 V	1.5 Ah	1.32 V	1.0 Ah	1.16 V
1822	1.8 Ah	1.39 V	2.3 Ah	1.51 V	1.8 Ah	1.38 V	1.2 Ah	1.31 V	0.9 Ah	1.12 V
1823	2.0 Ah	1.38 V	2.2 Ah	1.52 V	1.8 Ah	1.39 V	1.2 Ah	1.32 V	1. I Ah	1.17 V
1831	1.8 Ah	1.38 V	2.3 Ah	1.51 V	1.8 Ah	1.39 V	1.2 Ah	1.32 V	0.9 Ah	1, 13 V
1832	2.0 Ah	1.40 V	2.3 Ah	1.51 V	1.9 Ah	1.40 V	1.5 Ah	1.31 V	0.9 Ah	1.14 V
1833	2. 1 Ah	1.39 V	2.3 Ah	1.52 V	1.9 Ah	1.39 V	1.2 Ah	1.30 V	1.0 Ah	1, 12 V
Avg.	1.9 Ah	1.39 V	2.3 Ah	1.51 V   1.8 Ah   1.39 V	1.8 Ah	1.39 V	1.3 Ah	1.32 V	1.0 Ah	I. 14 V

TABLE LVII

## PRECYCLING TEST DATA Combination No. 19

	Forn (0.6	Formation (0.6 A)	Cyc (30	Cycle 1 (30 mA)	Cyc (0.6	Cycle 2 (0.6 A)	Cycle 3 (1.5 A)	le 3 A)	Cyc (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
1911	2.2 Ah	1.44 V	2.3 Ah	1.52 V	2.2 Ah	1.43 V	1.5 Ah	1.32 V	0.9 Ah	1.15 V
1912	2.3 Ah	1.44 V	2.3 Ah	1.52 V	2.3 Ah	1.43 V	1.6 Ah	1.35 V	0.9 Ah	1.14 V
1913	2.3 Ah	1.44 V	2.3 Ah	1.52 V	2.0 Ah	1.43 ∨	1.8 Ah	1.32 V	0.9 Ah	1.11 V
1921	2.3 Ah	1.45 V	2.2 Ah	1.53 V	2.3 Ah	1.44 V	1,2 Ah	1.29 V	0.9 Ah	1.13 V
1922	2.3 Ah	1.44 V	2.3 Ah	1.53 V	2.2 Ah	1.44 V	1.9 Ah	1.33 V	0.9 Ah	1, 13 V
1923	2.3 Ah	1.45 V	2.3 Ah	1.52 V	2.2 Ah	1.44 V	1.8 Ah	1.33 V	0.9 Ah	1, 15 V
1931	2.3 Ah	1.44 V	2.2 Ah	1.52 V	2.2 Ah	1.44 V	1.8 Ah	1.32 V	1.0 Ah	1.14 V
1932	2.3 Ah	1.45 V	2.3 Ah	1.52 V	2.2 Ah	1.43 V	1.8 Ah	1.31 V	0.9 Ah	1.11 V
1933	2.3 Ah	1.45 V	2.2 Ah	1.52 V	2.0 Ah	1.44 V	1.8 Ah	1.33 V	1. 1 Ah	1.15 V
Avg.	2.3 Ah	1.44 V	2.3 Ah	1.52 V	2.2 Ah	1.44 V	1.7 Ah	1.32 V	0.9 Ah	1.13 V

TABLE LVIII

## PRECYCLING TEST DATA

Combination No. 20

	Forn (0.6	Formation (0.6 A)	Cyc (30	Cycle 1 (30 mA).	Cyc (0. 6	Cycle 2 (0.6 A)	Cycle 3 (1.5 A)	le 3 . A)	Cyc (3	Cycle 4 (3 A)
Cell No.	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)	Output (Ah)	Plateau Voltage (V)
2011	2.2 Ah	1.43 V	2.3 Ah	1.53 V	2.3 Ah	1.43 V	1.6 Ah	1.28 V	1.1 Ah	1.12 V
2012	2.2 Ah	1.42 V	2.3 Ah	1,53 V	2.0 Ah	1.42 V	1.9 Ah	1.28 V	1.0 Ah	1.07 V
2013	2.2 Ah	1.43 V	2.3 Ah	1.53 V	2.2 Ah	1.40 V	2.0 Ah	1.29 V	1.0 Ah	1.09 V
2021	2.3 Ah	1,43 V	2.3 Ah	1.53 V	2.2 Ah	1.43 V	2.0 Ah	1.32 V	1.2 Ah	1.15 V
2022	2.3 Ah	1.44 V	2.3 Ah	1.52 V	2.3 Ah	1.45 V	2. 1 Ah	1.36 V	1.4 Ah	1.21 V
2023	2.3 Ah	1.44 V	2.3 Ah	1.52 V	2.2 Ah	1.44 V	2.0 Ah	1.34 V	1.4 Ah	1.16 V
2031	2.2 Ah	1.44 V	2.3 Ah	1.52 V	2.1 Ah	1.44 V	1.6 Ah	1.35 V	1.1 Ah	1.18 V
2032	2.2 Ah	1.43 V	2.3 Ah	1.53 V	2.2 Ah	1.42 V	1.9 Ah	1.29 V	1.1 Ah	1.11 V
2033	2.3 Ah	1.43 V	2.3 Ah	1.52 V	2.2 Ah	1.44 V	2.0 Ah	1.32 V	1.2 Ah	1.17 V
Avg.	2.2 Ah	1.43 V	2.3 Ah	1.53 V	2.2 Ah	2.2 Ah 1.43 V	1.9 Ah	1.9 Ah 1.31 V	1.2 Ah	1.14 V

TABLE LIX

TEST DATA ON COMBINATION NO. 13

		Regime 1		M.	Regime 2		4	Regime 3	
N. N.	1311	1312	1313	1321	1322	1323	1331	1332	1333
Capacity Checks  1. N(Q)  2. N(Q)  3. N(Q)  4. N(Q)  5. N(Q)	105 (1.6) 105 215 (1.4) 215 305 (0.6) 305	105 (1.6) 215 (1.3) 305 (0.5)	(1.6) 105 (1.6) (1.3) 215 (1.3) (0.5) 305 (0.4)	(1.6) 105 (1.6) 103 (0.6) 103 (0.8) 103 (0.5) 25 (1.3) 17 (1.2) 23 (1.3) (1.3) 215 (1.3) 203 (0.4) 204 (0.6) 204 (0.4) 233 (0.7) 270 (0.7)	103 (0.8) 204 (0.6) 233 (0.7) 270 (0.7)	103 (0.5) 204 (0.4)	25 (1.3)	17(1.2)	23 (1.3)
Status Cycle	373	373	373	203	270	204	25	17	23
Failure Mode	( <del>+</del> )	(+)	(+)	TF	(+)	TF	TF	TF	TF

TF = Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check.

CF = Catastrophic Failure - Cell cannot accept charge or cycle.

N(Q) = Cycle Number (Capacity)

TABLE LX

TEST DATA ON COMBINATION NO. 14

						1			
		Regime 1		щ	Regime 2		]	Regime 3	
Cell No.	1411	1412	1413	1421	1422	1423	1431	1432	1433
Capacity Checks							<del> </del>		
1. N(Q)	105(1.6)   105	105 (1.7)	105 (2.0)	(1.7) 105(2.0) 103(0.5) 103(0.7)	103 (0.7)	103 (0.7) 26 (1.1) 28 (1.1) 23 (0.9)	26 (1.1)	28(1.1)	23 (0.9)
2. N(Q)	215 (1.4)	215(1.3)	215(1.4)	204(0.5) 204(0.6) 204(0.6)	204 (0.6)	204 (0.6)	<del>, i , ,</del>		
3. N(Q)	305 (0.6)	305 (0.6)	305 (0.4)	297 (0.5)	298(0.5)	299 (0.5)			
4. N(Q)							<del></del>		
5. N(Q)									
6. N(Q)									
Status Cycle	373	373	373	297	298	299	56	28	23
Failure Mode	(+)	(+)	(+)	(+)	(+)	(+)	TF	TF	TF

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. ΤF

Catastrophic Failure - Cell cannot accept charge or cycle. CF

N(Q) = Cycle Number (Capacity)

TABLE LXI

TEST DATA ON COMBINATION NO. 15

	Regime 1		<b>14</b>	tegime 2			Regime 3	
1511	1512	1513	1521	1522	1523	1531	1532	1533
105 (1.6)		105 (2.0)	103 (0.6)	103 (0.6)	103 (1.0)	29 (1.3)	21 (0.9)	15 (1.2)
215 (1.6)	215	215 (1.8)	122 (0.4)	135 (0.5)	204 (0.7)			·
305 (0.6)		305 (0.8)			283 (0.5)			
:								
373	373	373	122	135	283	59	2.1	15
(+)	(+)	(+)	TF	H	TF	TF	TF	TF
	1511 105 (1.6) 215 (1.6) 305 (0.6) 373 (+)	Regi 11 6) 105 6) 215 6) 305 6) 305	Regi 115 105 215 305 305	Regi 115 105 215 305 305	Regi 115 215 305 305	Regi 115 105 215 305 305	Regi 115 215 305 305	Regime 1       Regime 2       Regime 2         1512       1513       1521       1523       1531         105 (1.8)       105 (2.0)       103 (0.6)       103 (1.0)       29 (1.3)       2         215 (1.8)       215 (1.8)       122 (0.4)       135 (0.5)       204 (0.7)       283 (0.5)       3         305 (0.8)       305 (0.8)       122       135 (0.5)       283 (0.5)       29         (+)       (+)       TF       TF       TF       TF

TF = Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check.

Catastrophic Failure - Cell cannot accept charge or cycle. CF =

N(Q) = Cycle Number (Capacity)

TABLE LXII

# TEST DATA ON COMBINATION NO. 16

		Regime 1			Regime 2			Regime 3	
Cell No.	1611	1612	1613	1621	1622	1623	1631	1632	1633
Capacity Checks									
I. N(Q)	105 (1.7) 105	[]	105 (1.4)	103 (0.5)	. 4) 105 (1.4) 103 (0.5) 103 (0.5) 103 (0.5) 22 (0.7) 26 (1.1) 15 (1.2)	103 (0.5)	22 (0.7)	26 (1.1)	15 (1.2)
2. N(Q)	215 (1.2) 215		215 (1.5)	124 (0.4)	. 6) 215 (1.5) 124 (0.4) 123 (0.4) 120 (0.3)	120 (0.3)			
3. N(Q)	305 (1.2) 305		(0.8) 305 (0.7)						
4. N(Q)									
5. N(Q)						-			
6. N(Q)					•				
Status Cycle	373	373	373	124	123	120	22	26	15
Failure Mode	(+)	(+)	(+)	IL	TF	TF	TF	TF	TF

TF = Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check.

Catastrophic Failure - Cell cannot accept charge or cycle. CF =

N(Q) = Cycle Number (Capacity)

TABLE LXIII
TEST DATA ON COMBINATION NO. 17

		Regime 1		Ľ	Regime 2			Regime 3	
Cell No.	1711	1712	1713	1721	1722	1723	1731	1732	1733
Capacity Checks							· · · · · · · · · · · · · · · · · · ·		
1. N(Q)	105 (1.7) 105		105 (1.7)	(1.4) 105 (1.7) 105 (0.5) 105 (0.5)	105 (0.5)	105 (0.5) 15 (1.3) 15 (1.6) 15 (1.5)	15 (1.3)	15 (1.6)	15 (1.5)
2. N(Q)	198 (1.3) 198		198 (1.3)	(1.0)   198 (1.3)   172 (0.4)   171 (0.4)	171 (0.4)	170 (0.5)	<del></del>		
3. N(Q)									
4. N(Q)								<del></del>	
5. N(Q)	<del></del>								
6. N(Q)				?					
Status Cycle	566	566	997	172	171	170	15	15	15
Failure Mode	( <del>+</del> )	(+)	(+)	TF	TF	(±)	TF	(+)	(+)

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. 11 TF

Catastrophic Failure - Cell cannot accept charge or cycle. CF.

N(Q) = Cycle Number (Capacity)

TEST DATA ON COMBINATION NO. 18 TABLE LXIV

		Regime 1			Regime 2			Regime 3	
Cell No.	1811	1812	. 1813	1821	1822	1823	1831	1832	1833
Capacity Checks  1. N(Q)  2. N(Q)  3. N(Q)  4. N(Q)  5. N(Q)  6. N(Q)	105 (1.5) 198 (1.0)	105	105 (1.4) 198 (0.9)	(1.4) 105 (1.4) 105 (0.6) 105 (0.6) 105 (0.5) 14 (1.3) 15 (1.3) 12 (1.3) (0.7) 198 (0.9) 172 (0.5) 172 (0.5) 170 (0.5)	105 (0.6)	105 (0.5) 170 (0.5)	14 (1.3)	15 (1.3)	12 (1.3)
Status Cycle	566	566	566	172	172	170	14	15	12
Failure Mode	(+)	(+)	(+)	(+)	(+)	(+)	TF	TF	TF

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. TF

Catastrophic Failure - Cell cannot accept charge or cycle. CF =

Cycle Number (Capacity) N(Q) =

Cell still cycling at end of program. H (+)

TABLE LXV

TEST DATA ON COMBINATION NO. 19

		Regime 1		Н.	Regime 2			Regime 3	
Cell No.	1911	1912	1913	1921	1922	1923	1931	1932	1933
Capacity Checks  1. N(Q)  2. N(Q)  3. N(Q)  4. N(Q)	105 (1.2) 105 198 (0.5) 198	105 (1.3) 198 (0.6)	*	105 (0.6) 105 (0.5) 170 (0.4) 157 (0.4)		105 (0.5) 14 (1.2) 15 (1.2) 12 (1.4)	14 (1.2)	15 (1.2)	12 (1.4)
5. N(Q) 6. N(Q)									
Status Cycle	799	997	*	170	157	105	14	15	12
Failure Mode	(+)	(+)	*	TF	$\mathtt{TF}$	TF	TF	TF	TF

Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check.

Catastrophic Failure - Cell cannot accept charge or cycle.

N(Q) = Cycle Number (Capacity)

(+) = Cell still cycling at end of program.

Cell failed after five precycling tests; construction deficiency.

TABLE LXVI

# TEST DATA ON COMBINATION NO. 20

		Regime 1		H .	Regime 2			Regime 3	
Cell No.	2011	2012	2013	2021	2022	2023	2031	2032	2033
Capacity Checks									
1. N(Q)	105 (1.4) 105		105 (1.2)	(1.1) 105 (1.2) 105 (0.5) 105 (0.7)	105 (0.7)	*	14 (1.1)	14 (1.1)   14 (1.1)   13 (1.4)	13 (1.4)
2. N(Q)	198 (0.7)	198	198 (0.5)	(0.3) 198 (0.5) 170 (0.5) 169 (0.4)	169 (0.4)	12			
3. N(Q)									
4. N(Q)					<del></del>				
5. N(Q)									
6. N(Q)									
Status Cycle	566	992	997	170	169	*	14	14	13
Failure Mode	(+)	(+)	(+)	(+)	TF	*	TF	TF	TF

= Technical Failure - Cell cannot deliver the cycling requirement output on a capacity check. TF

Catastrophic Failure - Cell cannot accept charge or cycle. CF =

N(Q) = Cycle Number (Capacity)

(+) = Cell still cycling at end of program.

\* = Cell failed after five precycling tests; construction deficiency.

The overall electrode efficiency  $(\eta\%)$  was determined by computing the percentage of residual capacity (q%) of capacity prior to failure cycle with respect to original capacity and dividing this figure by the residual weight percentage  $(\zeta\%)$  calculated above. This is equivalent to the percentage of the final output per gram with respect to the original output per gram, or the final-to-original utilization ratio in %.

To take into account the composition and the process of the zinc electrode, the efficiency of actual zinc metal present in the electrode was determined immediately after charge on the first and second cycles. It was done on two cells using unsintered zinc oxide electrodes and two cells using sintered 90/10 Z mix electrodes. Table LXVII giving the results of the four cells shows that the zinc utilization is in the range of 86% over two cycles, regardless of the mix. It can be postulated that adding an inorganic material and sintering the mix at 850°C have no significant effect on the zinc utilization efficiency.

The dissection, examination, and analysis of failed cells was done on one cell of each group (covering a specific combination and a specific test regime). The data of all cells examined prior to the end of the program are presented in detail in Appendix B. A summary of the pertinent information is given in Tables LXVIII, LXIX, and LXX.

#### Data Evaluation

Although the cycling test data were not complete by the end of the program period, an evaluation may be attempted. Disregarding all combinations 5 through 12 because they used another separator type (3420-25), we shall compare control group A and the other combinations. Most of the data were acquired on group A and combinations 1 to 4. Their average number of cycles are presented in Table LXXI. It appears that combination #1 has more cycles on all three regimes than control group A; combinations #2 and #3 show also better averages, although marginal on regime #3; combination #4 is marginal on all regimes. This shows at least that the 90/10 Z mix, common to all, must be a contributing factor toward improving the electrode. From the cycling data and the failure analyses, it seems also that the Exmet grid has a slight advantage over the Distex grid, although the electrode using a Distex grid has a better shape retention throughout its cycle life. The encapsulated positive design appears also to be beneficial to longer cycle life.

An analysis of variances was performed on control group A and experimental groups 1 through 4. The following conclusions were drawn:

(a) Each test regime datum must be analyzed independently.

TABLE LXVII

ZINC UTILIZATION

		Original		E	, c	Z	Zinc
Mix	Cell No.	ZnO Weight (g)	Cycle No.	Output (Ah)	Zinc (g)	Utilization (Ah/g)	$\text{Efficiency}^{\#}_{(\%)}$
100% ZnO	ZN-47-1	5.88	I	2.0	2.90	69.0	84
	ZN-47-2	5.88	2	2.2	3.18	0.69	84
90/10 Z	ZN-47-3	5.40	-	2.0	2.84	0.70	85
	ZN-47-4	5.40	2	2.2	3.04	0.72	68

 $^*$ With respect to theoretical.

TABLE LXVIII

CELL ANALYSIS SUMMARY
Regime No. 1 = 100°C, Discharge 0.60 A for 0.5 hr
Charge 0.66 A for 0.5 hr

Ident	Identification	no	E	ectrica.	Electrical Characteristics	teristi	cs	Zn	ZnO Content	ent	Final-to- Original
Combination	Cell Code	Mix and Process	Original Qo (Ah)	Wet Life (days)	Cycles	Final Q (Ah)	Residual Capacity (%)	Original (g)	Final (g)	Residual (%)	Utilization Ratio (%)
Ą	A-13	Control	2.0	65	302	0.2	10	5.9	3.6	61	16
,1	112A	90/10-Z, N	2.0	06	200	0.1	ĸ	5.4	2.0	37	14
2	212A		2.1	0.9	568	0.2	10		3.4	63	16
33	313A		2.1	09	568	0.2	10		2.5	46	22
4'	412A		2.1	57	568	0.1	S		2.7	50	10
13	1311		2.0	53	373*	9.0	33		3.2	59	56
14	1411	<b>→</b>	2.1	53	373*	9.0	35		3.1	57	61
15	1512	90/10-Z, PS	2.3	53	373*	0.8	35		3.3	61	57
16	1611	=	2.1	49	373*	1.2	5.7	<b>→</b>	3,3	61	46
17	1711	80/20-Z, N	2.0	47	*992	1.3	92	4.8	2.7	56	100
18	1811	=	1.8	47	\$99Z	1.0	56		2.7	56	100
19	1912	80/20-Z, PS	2.3	47	566*	9.0	38		2.6	54	02
20	2011	=	2.2	47	*992	0.7	32	<b>→</b>	2.6	54	59

\*Not failed.

TABLE LXIX

CELL ANALYSIS SUMMARY
Regime No. 2 = 25°C, Discharge 0.90 A for 0.5 hr
Charge 0.50 A for 1.0 hr

fica	Identification	區	lectrica	Electrical Characteristics	teristi	cs	Zn	ZnO Content	ent	Final-to-
Cell Code	Mix and Process	Original: Qo (Ah)	Wet Life (days)	Cycles N	Final O (Ah)	Residual Capacity (%)	Original (g)	Final (g)	Residual (%)	Utilization Ratio (%)
	A-22 Control	2.0	96	502	0.4	20	5.9	4.5	92	97
	123A 90/10-Z, N	2.0	114	591	0.4	20	5.4	3.7	69	29
7	223A	2.0	98 .	200	0.5	25		3.9	72	35
~	322A	2.1	114	593	0.4	19		3.9	72	56
7	421A	2.2	114	581	0.4	18	· · · · · ·	4.0	74	24
1321		2.1	41	203	0.4	19		3.6	29	28
1422	>	1.7	53	298	0.5	56		3.6	29	43
1521	1 90/10-Z, PS	2.2	34	122	0.4	18		3.8	20	56
1621	-	2.1	30	124	0.4	19	$\rightarrow$	3.6	67	28
1722	2 80/20-Z, N	2.2	47	170	0.4	18	4.8	2.8	58	31
1822	-:	1.8	47	172*	0.5	. 82		3.0	62	45
1923	3 80/20-Z, PS	2.3	40	105	0.5	22		3.1	65	34
2022	2	2.3	47	169	0.4	17	<del></del>	5.6	54	31
-				1		•		-		-

"Not failed.

TABLE LXX

CELL ANALYSIS SUMMARY

Regime No. 3 = 25°C, Discharge I.20 A for I.2 hr Charge 0.07 A for 22.8 hr

Final-to-	Utilization Ratio (%)	74	88 94	06	85	88	62	72	7.7	73	84	68	63	63
ent	Residual (%)	81	69	72	72	74	72	85	74	78	77	81	83	79
ZnO Content	Final (g)	<b>4.</b> 8	3.7	3.9	3.9	4.0	3.9	4.6	4.0	4.2	3.7	3.9	4.0	3.8
uZ	Original (g)	5.9	4		······································	<del></del>				$\rightarrow$	4.8			$\rightarrow$
cs	Residual Capacity (%)	09	61 61	65	61	65	52	61	57	57	65	72	52	50
Electrical Characteristics	Final Q (Ah)	1.2	1.4	1.5	1.4	1.5	1.2	1.1	1.2	1.2	1.3	1.3	1.2	1.1
	Cycles N	09	46 118	62	3.6	52	17	92	15	15	15	14	14	14
	Wet Life (days)	107	90	111	111	06	34	53	34	30	47	47	47	47
	Original Qo (Ah)	2.0	2.3	2.3	2.3	2.3	2.1	2.0	2.1	2.1	2.0	1.8	2.3	2.2
uc	Mix and Process	Control	90/10-Z, N					>	90/10-Z, PS	Ξ	80/20-Z, N	=	80/20-Z, PS	11
Identification	Cell Code	A-32	132 131	232	332	431	1332	1431	1533	1633	1731	1831	1931	2032
Ident	Combination	А		2	3	4	13	14	15	16	17	18	19	20

<u>TABLE LXXI</u>

NUMBER OF CYCLES REACHED ON EACH REGIME

(Average of 3 Cells)

Combination No.	Regime l	Regime 2	Regime 3
A	280	534	60
1	500	606	96 <sup>*</sup>
2	433	605	74
3	424	606	71
4	295	602	50
13	373 <sup>*</sup>	226*	22
14	373*	298*	26
15	373*	180	22
16	373*	122	21
17	266*	171*	15*
18	266*	172*	14
19	266*	144	14
20	266*	170*	14

<sup>\*</sup>Cells still cycling at the end of the program period.

- (b) The factors studied (grid structure, wafer design) were significant for test regime #1, but not for regimes #2 and #3.
- (c) On test regime #1, cells of combination 4 were as good as the control cells, but poorer than cells of any other construction.

The data on all other combinations were not far enough advanced at the end of the program to be fully conclusive. However, the following trends can be noticed:

- (a) Introduction of lead did not seem to help on regime #3.
- (b) The presintered (PS) process seems less advantageous than the normal (N) process. Combinations #15 and #16 reached about 150 cycles contrasted to #13 and #14 which reached about 250 cycles on regime #2.

A very important facet of this evaluation is that all the test cells were zinc limited and consequently possibly overcharged, since they were cycled in series and they might have undergone some imbalance. This set of conditions caused cells to have short cycle life on regimes 1 and 2. On regime 3, the failure mode was mainly inability of the cell to meet the cycling capacity requirement, which was set at 1.44 Ah output. A cell failing at 60 cycles meant only that its capacity dropped below 1.44 Ah.

#### CONCLUSION

The program covered the investigation of physical and electrical characteristics of a zinc electrode of novel construction. The fabrication technique involved adding an inorganic refractory type material to the zinc oxide in a small proportion (up to 20%) and sintering the pressed electrode at 850°C, below the melting point of the silver grid of the collector. The sintering had a bonding effect between all the particles, possibly caused by the formation of a solid solution at the particle surface. The resultant electrode had good structural strength, and was capable of handling and of absorbing a small amount of additive (HgO or PbO in the range of 2%) by a wet process.

Physical characteristics were determined for three different inorganic materials added in various ratios ranging from 2% to 50% and sintered at temperatures ranging from 300°C to 1400°C. Selection among the multiple combinations resulted in one inorganic material (Zirconia) added in three different ratios (5, 10, 20%) sintered at one temperature (850°C), the mix being processed in two different ways (sintering the pressed electrode and sintering the mix prior to sintering the pressed electrode).

The electrical tests were carried out on electrodes combining some features of the above selection. The results were compared with those of the standard (unsintered) zinc oxide electrode on three different automatic cycling regimes after establishing their electrical performance on five total discharge cycles run at various rates.

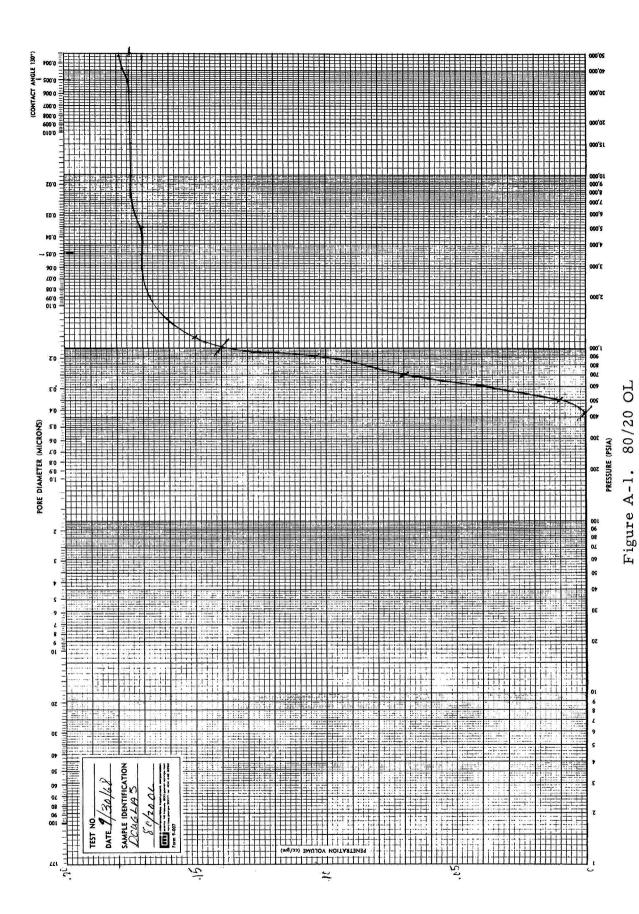
Because of the time and budget limitations of this program, not all electrical data were acquired, but sufficient information was obtained to show a trend and a possible solution to the zinc "slumping" problem. All cells using a sintered ZnO inorganic material mix electrode showed, upon failure analysis, a remarkable zinc shape retention, at least when using a minimum of 10% zirconia in the mix. This fact is associated with the physical integrity of the electrode during fabrication, assembly, cell electrolyte soaking and hence during cycling. These two striking features, structural strength and minimization of shape change during cycling, weigh heavily in favor of such an electrode. It is important to remember that cycle life is not immediately relevant at this time for the following forceful reasons:

This program was designed to quickly screen out and evaluate various zinc electrode constructions (using a sintered mix) on a relative scale on three different test regimes. In order to do this, the test cell was conceived and designed to be zinc limiting for the first cycle, contrary to conventional cell designs where silver is the limiting electrode on charge and discharge and zinc oxide capacity is at least 40 to 60% overdesigned. The test cell was therefore made to reach the full charge of the zinc electrode on every cycle from the very first. This imposes a heavy handicap on the cell from the beginning since this condition promotes zinc penetration and no separator is immune to such severe testing. This explains the relatively short cycle life despite the fact that the zinc electrode still retained good shape, which in a cell of well balanced electrode design with test conditions properly set (no overcharge) would lead to longer cycle life than has been recorded in the previous test cells. It means that a test cell actually starts its cycling under the conditions it would have seen 300 to 500 cycles later, had it been designed in a conventional manner.

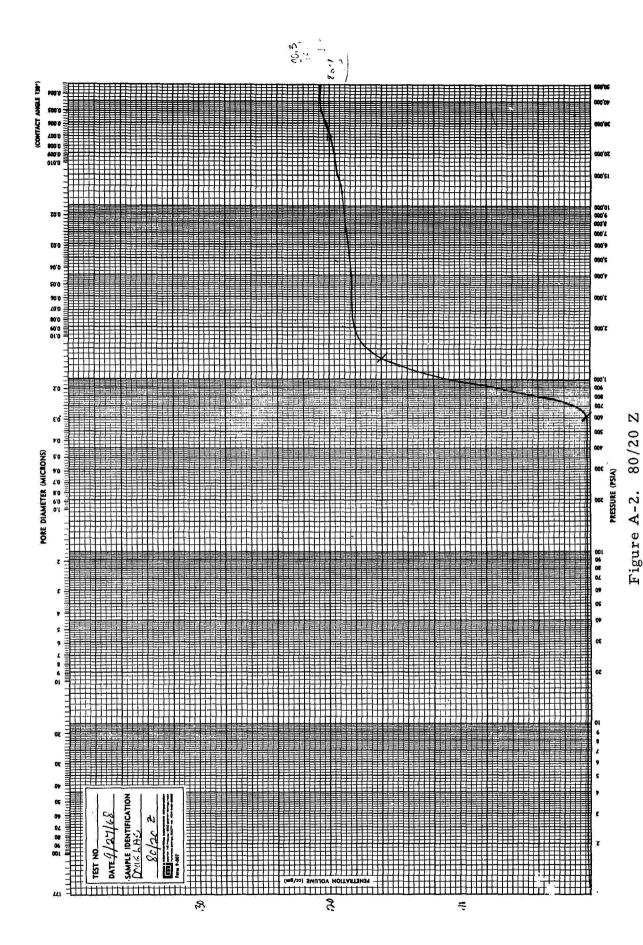
In this light, the sintered zinc oxide electrode is a very promising candidate for test in a 5 Ah silver zinc cell of the model tested on another NASA contract\* for direct comparison. It is recommended that such a program be considered.

A. Himy, "Development and Testing of a 5 Ah Ag-Zn Cell," Final Report NASA CR-72551, NASA Lewis, NAS 3-10924.

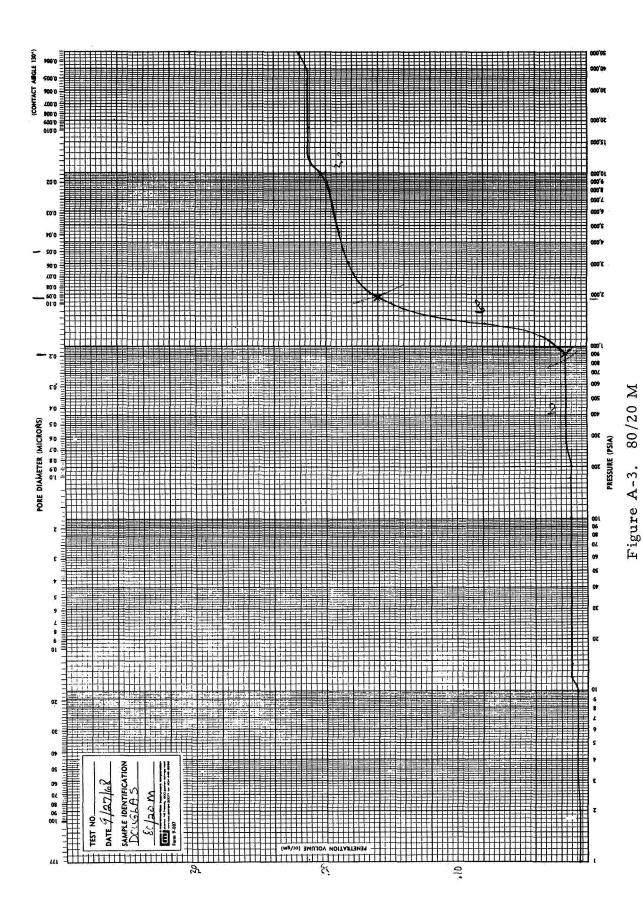
### APPENDIX A PORE SIZE DISTRIBUTION EXPERIMENTAL DATA CURVES



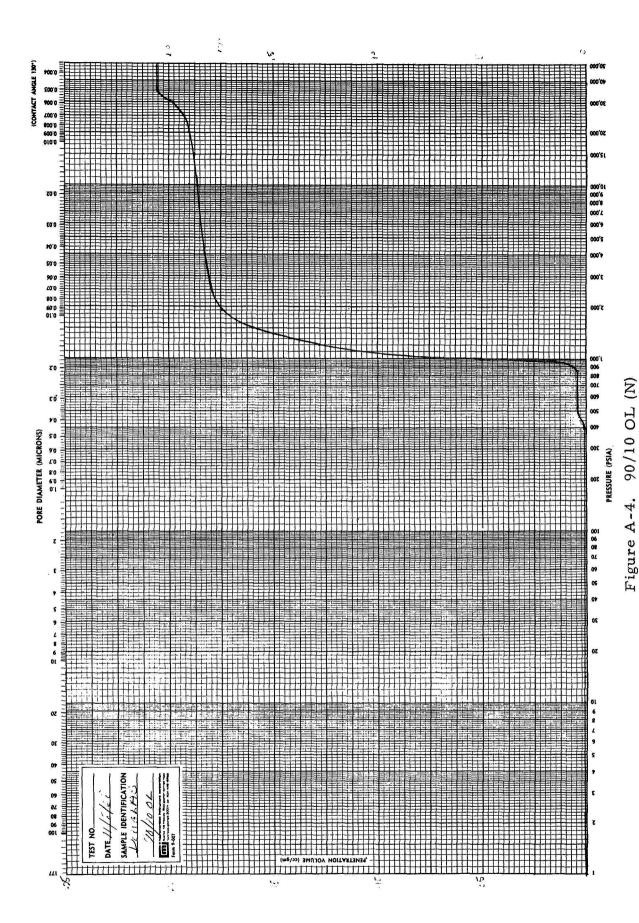
A-1



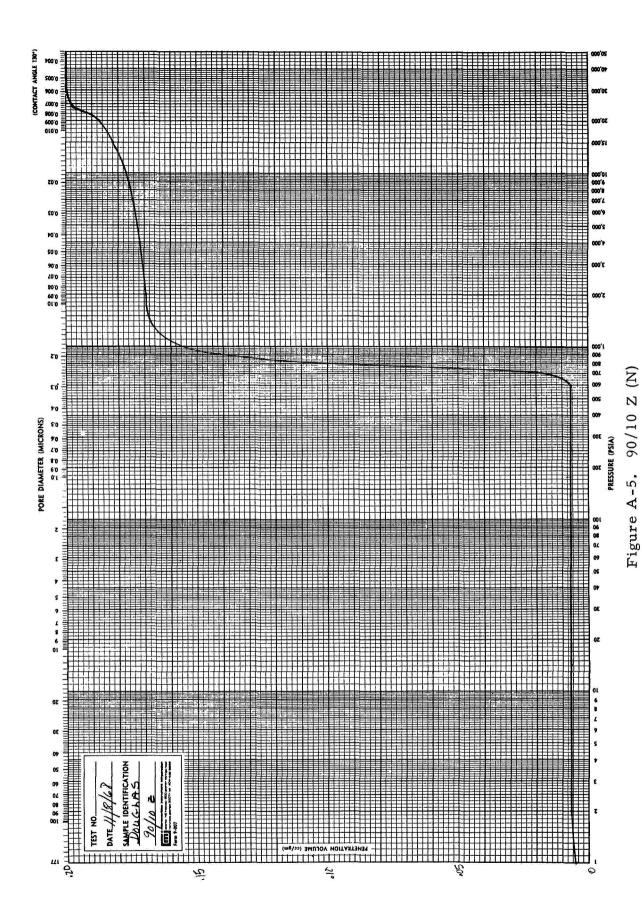
A-2



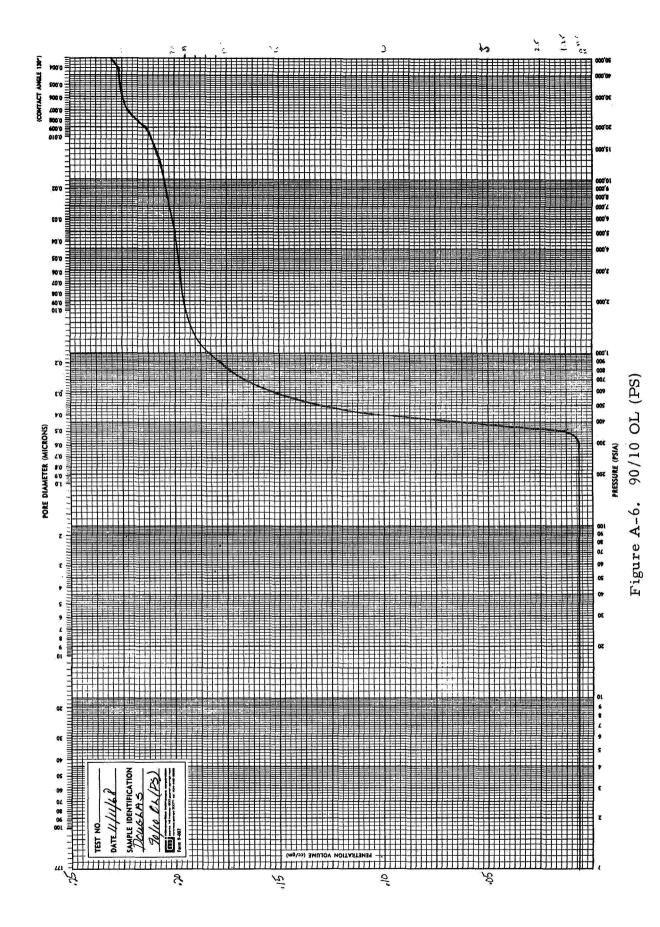
**A-**3

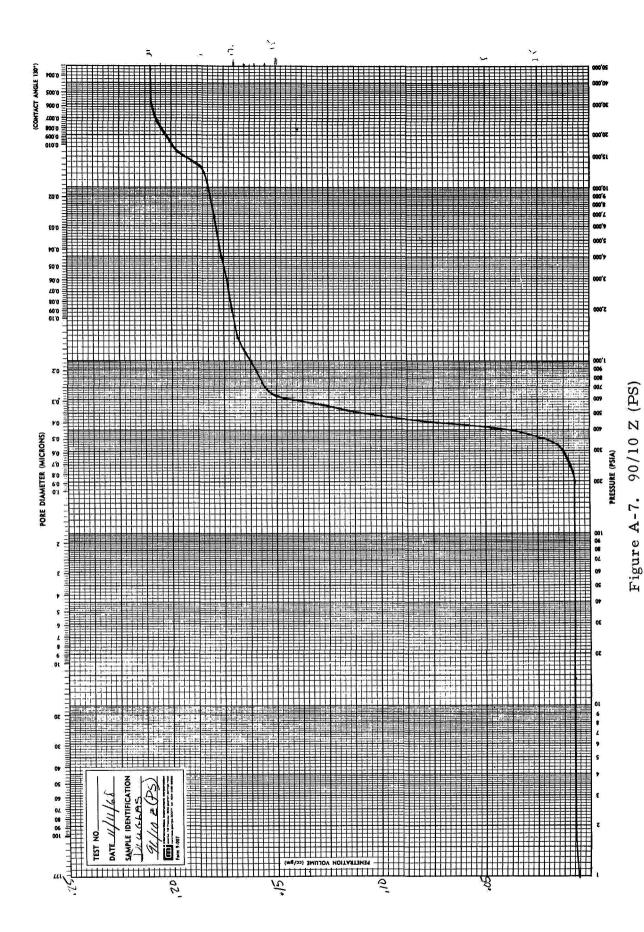


A-4



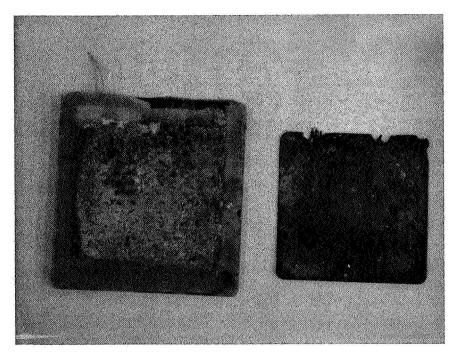
A-5





A-7

### APPENDIX B CELL ANALYSES AND ELECTRODE PICTURES



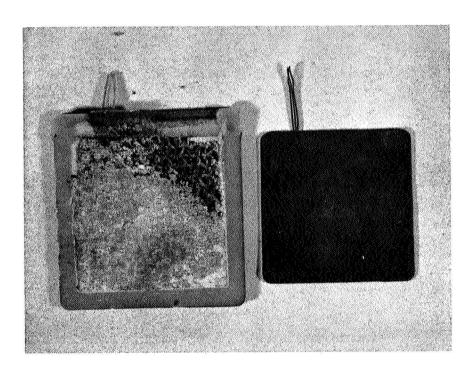
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Figure B-1. Cell Number A-13

#### CELL ANALYSIS

#### Cell No. A-13

Regime 1		Con	nbination (	Control A	
Tomonomore	100°C	Dindon	i — i — i — i — i — i — i — i — i — i —		
Temperature:	· · · · · · · · · · · ·	Binder:		None	
Period:	l hr.	Ratio:		100/0	
Discharge:	0.6 A for 0.5 hr.	Process	:	Not sintered	
Charge:	0.66 A for 0.5 hr.	Additive	(PbO%):	0	
		Grid:		5 Ag 38-1/0	
		Design:		(-) W	
Original Capacity:	Q <sub>.o</sub> =	2.0 Ah			
Last Capacity:	Q =	0.2 Ah			
Capacity Retention %	$6: q = \frac{Q}{Q_0} \times 100 =$	10%			
Failure Cycle:		302			
Wet Life:	days =	<b>6</b> 5			
Inspection:  Separators: No cracks, black stains both sino delam, Zn pen. probable failure cause.  Positive active area: p = N.A.  Negative shape retention: p = 90%  Zinc electrode condition: Good					
	Plate Location	Density	Color	Wetness	
	Тор	Spongy	Gray	Semi-wet	
	Bottom	Spongy	Gray	Semi-wet	
Analysis:	Original ZnO m Residual ZnO m ZnO retention % Final-to-original ratio (%): $\eta = \frac{q}{\zeta}$	hass: $m = \frac{m}{m_0}$ al utilizat	x 100 = 6  ion	6.9 g 6.6 g 61%	



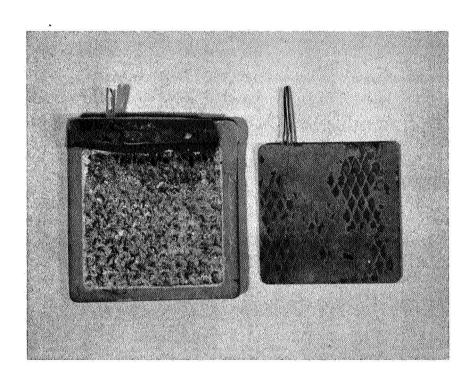
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Figure B-2. Cell Number A-22

#### CELL ANALYSIS

#### Cell No. A-22

Regime 2		Com	bination C	ontrol A		
Temperature: 2	25°C	Binder:	N	one		
Period: 1	.5 hr.	Ratio:	10	00/0		
Discharge: 0	0.9 A for 0.5 hr.	Process	: N	ot sintered		
Charge: 0	0.5 A for 1.0 hr.	Additive	(PbO%): 0			
		Grid:	5	Ag 38-1/0		
		Design:	(-	) W		
Original Capacity:	$Q_0 = 2$	2.0 Ah				
Last Capacity:		0.4 Ah				
Capacity Retention %	$e q = \frac{Q}{Q_0} \times 100 = 2$	20%				
Failure Cycle:	N =	502				
Wet Life:	days =	96				
Inspection:	Separators: No stains, Zn pen.		no delam.,	few dark		
	Positive active	area: p <sup>+</sup>	= N.A.	•		
	Negative shape	retention:	$p^- = 80\%$			
	Zinc electrode	Zinc electrode condition: Fair				
	Plate Location	Density	Color	Wetness		
	Тор	Spongy	Gray	Semi-wet		
	Bottom	Spongy	Gray	Semi-wet		
Analysis:	Original ZnO m Residual ZnO m	U		.9 g .5 g		
	ZnO retention %			6%		
	Final-to-origina					
	ratio (%): $\eta = \frac{q}{\zeta}$			6%		



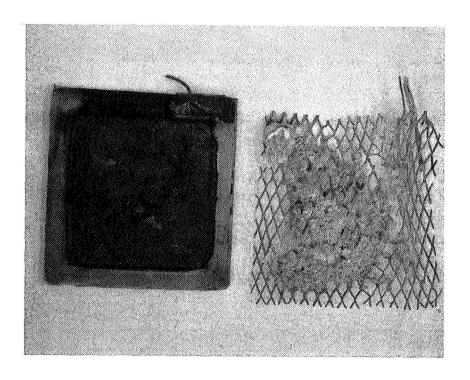
c57//

Figure B-3. Cell Number A-32

#### CELL ANALYSIS

#### Cell No. A-32

Regime 3		Com	nbination C	ontrol A
Temperature: 2	5°C	Binder:	No	one
Period: 2	4 hr.	Ratio:	10	00/0
Discharge: 1	.2 A for 1.2 hr.	Process	: No	ot sintered
Charge: 0	.07 A for 22.8 hr.	Additive	(PbO%): 0	
		Grid:	5	Ag 38-1/0
		Design:	( -	) W
Original Capacity:	$Q_0 = 2$	.0 Ah		
Last Capacity:		.2 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 = 6$	0%		
Failure Cycle:		0		
Wet Life:	days = 1	.07		
Inspection:	Separators: No stains, signs of Positive active Negative shape	Zn pen. area: p <sup>+</sup> retention:	= 100% p = 80%	,
	Plate Location	Density	Color	Wetness
	Тор	Spongy	Gray	Wet
	Bottom	Spongy	Gray	Wet
Analysis:	Original ZnO m Residual ZnO m ZnO retention % Final-to-origina ratio (%): $\eta = \frac{q}{\zeta}$	ass: $m = \frac{m}{m_0}$ al utilizat	100 = 8	9 g . 8 g 1%

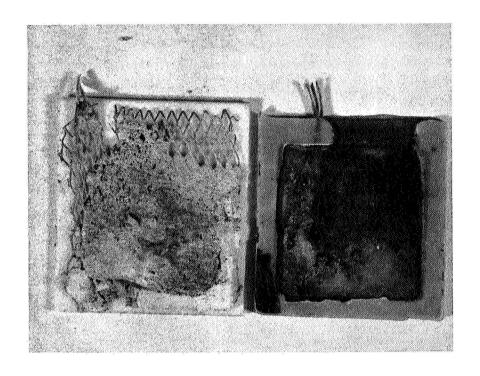


c 57/2

Figure B-4. Cell Number 112A

#### Cell No. 112A

Regime 1	Combination 1			
Temperature: 100	°C	Binder:		Z
Period: 1 hr	:.	Ratio:		90/10
Discharge: 0.6	A for 0.5 hr.	Process: N		
Charge: 0.6	6 A for 0.5 hr.	Additive (PbO%): 0		
		Grid:		5 Ag 14-1/0
		Design:		(+) W
Original Capacity:	Q <sub>0</sub> =	2.0 Ah		
Last Capacity:	Q =	0.1 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	5%		
Failure Cycle:	N = ~0	500		
Wet Life:	days =	90		
Inspection:	Separators: No cracks or delam., dark stain on Ag side, signs of Zn pen.  Positive active area: p = N.A.  Negative shape retention: p = 50%  Zinc electrode condition: Fair			
	Plate Location	Density	Color	Wetness
	Тор	Loose	Gray	Wet
	Bottom	Loose	Gray	Wet
Analysis:	Original ZnO marker Residual ZnO marker ZnO retention % Final-to-original ratio (%): $\eta = \frac{q}{\zeta}$	ass: $m = \frac{m}{m_0}$ if utilizat	x 100 =	5.4 g 2.0 g 37%

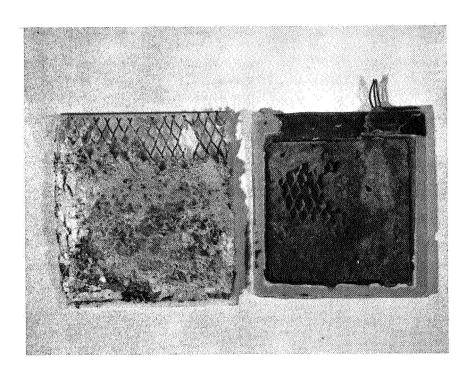


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Figure B-5. Cell Number 123A

### Cell No. 123A

Regime 2	Combination 1			
Temperature: 25	°C	Binder:		Z
Period: 1.	5 hr	Ratio:		90/10
Discharge: 0.	9 A for 0.5 hr.	Process	:	N
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%):	0
		Grid:		5 Ag 14-1/0
		Design:		(+) W
Original Capacity:	Q <sub>0</sub> =	2.0 Ah		
Last Capacity:	_	0.4 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	20%		
Failure Cycle:	-	591		
Wet Life:	days =	114		
Inspection:	Separators: No cracks, no delam., some dark stains, signs of Zn pen.  Positive active area: p = N.A.  Negative shape retention: p = 75%  Zinc electrode condition: Fair			
	Plate Location	Density	Color	Wetness
	Тор	Loose	Gray	Wet
	Bottom	Loose	Gray	Wet
Analysis:	Original ZnO marker Residual ZnO marker ZnO retention % Final-to-original ratio (%): $\eta = \frac{q}{\zeta}$	ass: $m = \frac{m}{m_0}$ $\therefore \zeta = \frac{m}{m_0}$ il utilizat	x 100 =	5.4 g 3.7 g 69%



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Figure B-6. Cell Number 131

#### Cell No. 131

Regime 3		Combination	1
Temperature:	25°C	Binder:	Z
Period:	24 hr.	Ratio:	90/10
Discharge:	1.2 A for 1.2 hr.	Process:	N
Charge:	0.07 A for 22.8 hr	. Additive (PbO%):	0
		Grid:	5 Ag 14-1/0
		Design:	(+) W
Original Capacity:	Q <sub>o</sub> =	2.3 Ah	appears to the second s
Last Capacity:	Q =	1.4 Ah	
Capacity Retention	$q = \frac{Q}{Q_0} \times 100$	= 61%	
Failure Cycle:	N = ~0	118	
Wet Life:	days =	184	

Inspection:

Separators: No cracks or delam., Zn pen signs, some Zn on far side of Ag wafer.

Positive active area: p<sup>+</sup> = 100%

Negative shape retention: p = 90%

Zinc electrode condition: Good

Plate Location	Density	Color	Wetness
Тор	Spongy	Gray	Wet
Bottom	Spongy	Gray	Wet

Analysis:

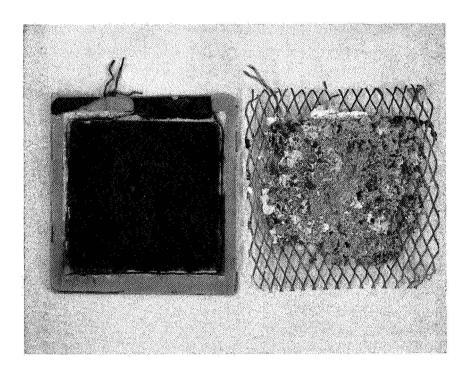
Original ZnO mass: m = 5.4 g

3.5 g Residual ZnO mass: m =

ZnO retention %:  $\zeta = \frac{m}{m_0} \times 100 =$ 65%

Final-to-original utilization

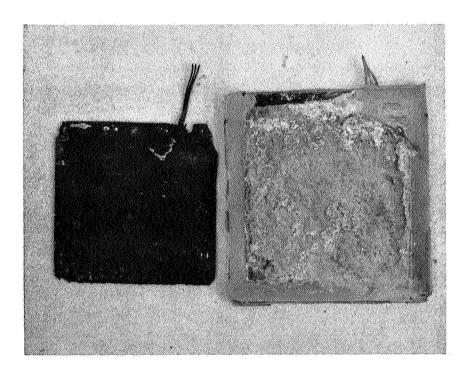
ratio (%):  $\eta = \frac{q}{\zeta} \times 100 =$ 94%



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Figure B-7. Cell Number 132

Regime 3		Con	Combination 1			
Temperature: 2	25°C	Binder:		Z		
Period: 2	24 hr.	Ratio:		90/10		
Discharge: 1	1.2 A for 1.2 hr.	Process	:	N		
Charge: 0	0.07 A for 22.8 hr.	Additive	(PbO%):	0		
		Grid:		5 Ag 14-1/0		
		Design:		(+) W		
Original Capacity:	Q <sub>0</sub> =	2.3 Ah				
Last Capacity:	Q =	1.4 Ah				
Capacity Retention %	$q = \frac{Q}{Q_0} \times 100 =$	61%				
Failure Cycle:	N =	46				
Wet Life:	days =	90				
Inspection:	Separators: No cracks or delam., some dark stains, Zn pen. still gassing.					
	Positive active	area: p <sup>+</sup>	= N.	Α.		
	Negative shape	retention:	$\mathbf{p}^{-} = 90\%$	<i>1</i> <sub>0</sub>		
	Zinc electrode	condition:	Go	od		
	Plate Location	Density	Color	Wetness		
	Тор	Spongy	Gray	Wet		
	Bottom	Spongy	Gray	Wet		
Analysis:	Original ZnO r	nass: m	=	5.4 g		
	Residual ZnO	Residual ZnO mass: m = 3.7 g				
	ZnO retention	$\%$ : $\zeta = \frac{m}{m_0}$	x 100 =	69%		
	Final-to-origin	•				
	ratio (%): $\eta = \frac{1}{2}$	$\frac{1}{2}$ x 100 =		88%		

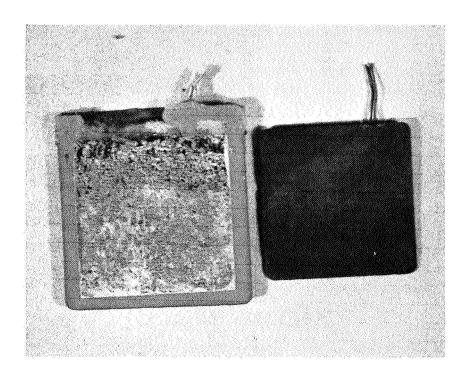


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Figure B-8. Cell Number 212A

## Cell No. 212A

	Con	nbination 2	
)°C	Binder:	Z	
r.	Ratio:	9:	0/10
A for 0.5 hr.	Process	: N	
6 A for 0.5 hr.	Additive	(PbO%): 0	
	Grid:	5	Ag 14-1/0
	Design:	(-	-) W
Q <sub>0</sub> =	2.1 Ah		
Q =	0.2 Ah		
$q = \frac{Q}{Q_0} \times 100 =$	10%		
days =	60		
Separators: One cracked separator, no delam., dark stains, Zn pen. still gassing.			
		_	
		=	o
Zinc electrode	condition:	Good	1
Plate Location	Density	Color	Wetness
Тор	Spongy	Blue-Gray	Semi-wet
Bottom	Spongy	Blue-Gray	Semi-wet
	U		.4 g
			• <del>-</del> g 3%
	~		<i>5</i> /0
rinai-to-origin	ai utiiizat	TOIT	
	Q = q = Q/Qo x 100 = N = days =  Separators: On dark stains, Zn Positive active Negative shape Zinc electrode  Plate Location Top Bottom  Original ZnO m Residual ZnO m ZnO retention %	Binder: Ratio: Ratio: Process A for 0.5 hr. Additive Grid: Design: $Q_{0} = 2.1 \text{ Ah}$ $Q = 0.2 \text{ Ah}$ $Q = \frac{Q}{Q_{0}} \times 100 = 10\%$ $N = 299$ $days = 60$ Separators: One cracked dark stains, Zn pen. still Positive active area: p Negative shape retention: Zinc electrode condition:  Plate Location Density Top Spongy Bottom Spongy  Original ZnO mass: m Residual ZnO mass: m ZnO retention %: $\zeta = \frac{m}{m_{0}}$	Ratio: 99 Process: N 6 A for 0.5 hr. Additive (PbO%): 0 Grid: 5 Design: (-  Qo = 2.1 Ah Q = 0.2 Ah q = Qo x 100 = 10% N = 299 days = 60  Separators: One cracked separator, dark stains, Zn pen. still gassing. Positive active area: p = N. A Negative shape retention: p = 100% Zinc electrode condition: Good Plate Location Density Color Top Spongy Blue-Gray Bottom Spongy Blue-Gray Original ZnO mass: m = 5 Residual ZnO mass: m = 5 Residual ZnO mass: m = 5

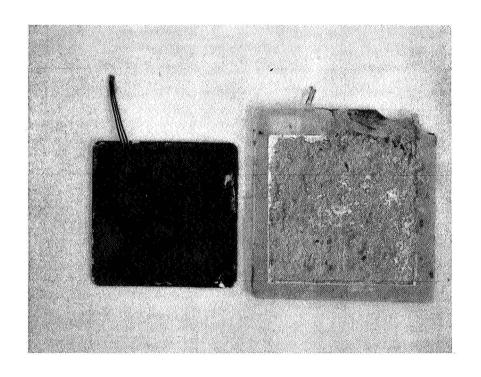


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Figure B-9. Cell Number 223A

#### Cell No. 223A

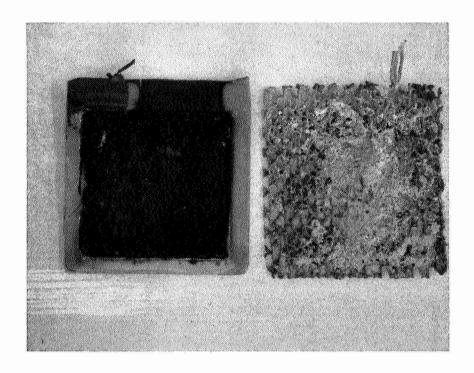
Regime 2	Con	2		
Temperature: 2	5°C	Binder:		Z
	.5 hr.	Ratio:	.C	90/10
Discharge: 0	.9 A for 0.5 hr.	Process	: 1	V.
Charge: 0	.5 A for 1.0 hr.	Additive	(PbO%):	)
		Grid:	5	5 Ag 14-1/0
		Design:	(	-) W
Original Capacity:	Q <sub>0</sub> =	2.0 Ah		
Last Capacity:	Q =	0.5 Ah		
Capacity Retention %	$= q = \frac{Q}{Q_0} \times 100 =$	25%		
Failure Cycle:	N <sub>.</sub> = ~0	500		
Wet Life:	days =	86		
Inspection:	Separators: No cracks or delam., few dark stains, signs of Zn pen.			
	Positive active	area: p <sup>+</sup>	= N.A	١.
	Negative shape	retention:	$p^- = 80\%$	)
	Zinc electrode	condition:	Goo	od
	Plate Location	Density	Color	Wetness
	Тор	Spongy	Gray	Semi-wet
	Bottom	Spongy	Gray	Semi-wet
Analysis:	Original ZnO m	nass: m	<b>=</b> 5	5.4 g
	Residual ZnO n	nass: m =	: 3	3.9 g
	ZnO retention 6	$\delta: \zeta = \frac{m}{mc}$	x 100 =	72%
	Final-to-origin			
	ratio (%): $\eta = \frac{9}{6}$	x 100 =	3	35%
	,			



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Figure B-10. Cell Number 232

Regime 3			Combination 2			
Temperature: 2	25°	С	Binder:		Z	
Period: 2	24 1	hr.	Ratio:		90/10	
Discharge:	1.2	A for 1.2 hr.	Process	:	N	
Charge: (	0.0	7 A for 22.8 hr.	Additive	(PbO%):	0	
			Grid:		5 Ag 14-1/0	
			Design:		(-) W	
Original Capacity:		Q <sub>0</sub> =	2.3 Ah			
Last Capacity:		_	1.5 Ah			
Capacity Retention %	<b>%</b> :	$q = \frac{Q}{Q_0} \times 100 = 0$	65%			
Failure Cycle:		N =	63			
Wet Life:		days =	111			
Inspection:		Separators: No cracks or delam., dark stains, some Zn pen., still gassing.				
		Positive active	area: p <sup>+</sup>	= N.	Α.	
		Negative shape	retention	p = 100	0%	
		Zinc electrode o	ondition:	Go	od	
		Plate Location	Density	Color	Wetness	
		Тор	Loose	Blue-Gra	y Semi-wet	
		Bottom	Spongy	Blue-Gra	y Semi-wet	
Analysis:		Original ZnO m	ass: m	=	5.4 g	
		Residual ZnO m	ass: m =	:	3.9 g	
		ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 =	72%	
		Final-to-origina				
		ratio (%): $\eta = \frac{q}{\zeta}$	x 100 =		90%	

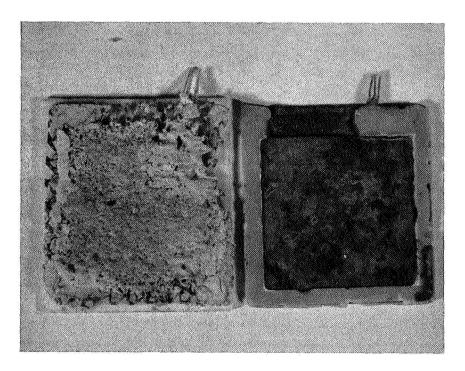


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Figure B-11. Cell Number 313A

### Cell No. 313A

Regime 1	Combination 3			
Temperature: 10	o°C	Binder:	Z	,
Period: 1 h	ar.	Ratio:	9	0/10
Discharge: 0.	6 A for 0.5 hr.	Process	: N	I
Charge: 0.6	6A for 0.5 hr.	Additive	(PbO%): 0	
		Grid:	5	Ag 38-1/0
		Design:	(-	+) W
Original Capacity:	Q <sub>0</sub> = 3	2.1 Ah		
Last Capacity:	_	0.2 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	10%		
Failure Cycle:		299		
Wet Life:	days =	60		
Inspection:	Separators: No cracks or delam., some dark stains, Zn pen., still gassing.  Positive active area: p <sup>+</sup> = N.A.  Negative shape retention: p <sup>-</sup> = 50%  Zinc electrode condition: Fair			
	Plate Location	Density	Color	Wetness
	Тор	Loose	Gray	Semi-wet
	Bottom	Loose	Gray	Semi-wet
Analysis:	Original ZnO m Residual ZnO m ZnO retention % Final-to-origina ratio (%): $\eta = \frac{q}{\zeta}$	ass: $m = \frac{m}{m_0}$ al utilizat	= 2 $ = 100 = 4 $ $ = 4 $ $ = 100$	.4 g .5 g .6%

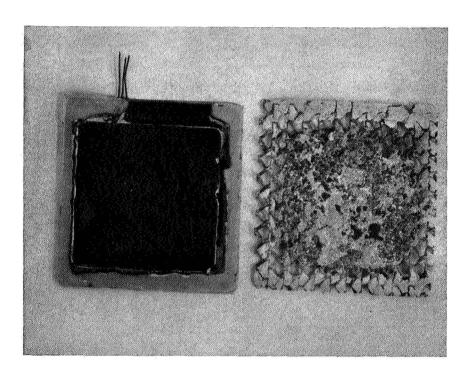


*C5720* 

Figure B-12. Cell Number 322A

Cell No. 322A

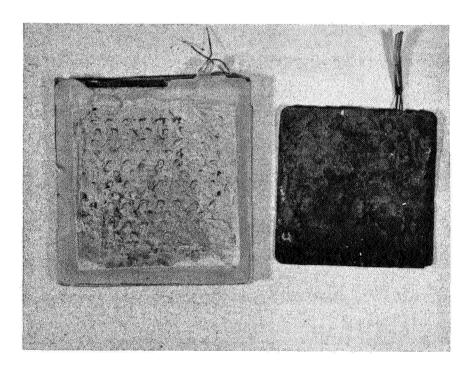
Regime 2		Con	Combination 3		
Temperature: 2!	5°C	Binder:		Z	
Period: 1.	5 hr.	Ratio:		90/10	
Discharge: 0.	9 A for 0.5 hr.	Process	):	N	
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%):	0	
		Grid:		5 Ag 38-1/0	
		Design:		(+) W	
Original Capacity:	Q <sub>0</sub> =	2.1 Ah			
Last Capacity:	Q =	0.4 Ah			
Capacity Retention %	$= q = \frac{Q}{Q_0} \times 100 =$	19%			
Failure Cycle:	N =	593			
Wet Life:	days =	114			
Inspection:	Separators: No cracks or delam., signs of pen.				
	Positive active	area: p <sup>+</sup>	= N.	A.	
	Negative shape	retention	p = 10	0%	
	Zinc electrode	condition:	Go	bod	
	Plate Location	Density	Color	Wetness	
	T' p	Spongy	Gray	Wet	
	Bottom	Spongy	Gray	Wet	
Analysis:	Original ZnO m	ass: m	=	5.4 g	
	Residual ZnO n	nass: m =	<b>:</b>	3.9 g	
	ZnO retention %	$\zeta : \zeta = \frac{m}{m}$	x 100 =	72%	
	Final-to-origin	•			
	ratio (%): $\eta = \frac{q}{\zeta}$			26%	
	, 6				



c572/

Figure B-13. Cell Number 332

Regime 3			Con	nbination	3
Temperature:	25 <sup>0</sup>	С	Binder:		Z
	24		Ratio:	4	90/10
Discharge:	1.2	A for 1.2 hr.	Process	:	N
Charge:	0.0	7 A for 22.8 hr.	Additive	(PbO%):	0
_			Grid:		5 Ag 38-1/0
			Design:		(+) W
Original Capacity:		$Q_0 = 2$	2.3 Ah		
Last Capacity:		Q =	l.4 Ah		
Capacity Retention	%:	$q = \frac{Q}{Q_0} \times 100 = 6$	51%		
Failure Cycle:		N =	36		
Wet Life:		days =	111		
Inspection:	***	Separators: No cracks or delam., dark stains and Zn pen., still gassing.			
		Positive active	area: p	= N.	Α.
		Negative shape	retention	p = 90%	<sup>7</sup> o
		Zinc electrode o	condition:	God	od
		Plate Location	Density	Color	Wetness
		Тор	Spongy	Blue-Gra	y Semi-wet
		Bottom	Spongy	Blue-Gra	y Semi-wet
Analysis:		Original ZnO m	ass: mo	=	5.4 g
		Residual ZnO m	ass: m =	<b>=</b>	3.9 g
		ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 =	72%
		Final-to-origina			
		ratio (%): $\eta = \frac{q}{\zeta}$	x 100 =		85%

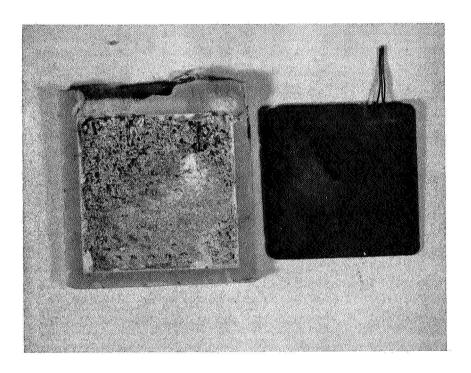


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Figure B-14. Cell Number 412A

## Cell No. 412A

Regime 1		Combination 4		
Temperature: 100	0°C	Binder:		Z
Period: 1 h	ır.	Ratio:		90/10
Discharge: 0.6	A for 0.5 hr.	Process	•	N
Charge: 0.6	66 A for 0.5 hr.	Additive	(PbO%):	0
		Grid:		5 Ag 38-1/0
		Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	2.1 Ah		
Last Capacity:		0.1 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	5%		
Failure Cycle:		299		
Wet Life:	days =	57		
Inspection:	Separators: No cracks or delam., dark stains and some Zn pen.			
	Positive active	area: p	= N.	Α.
	Negative shape	retention:	p = 90%	<b>7</b> 0
	Zinc electrode o	ondition:	Fa	ir
	Plate Location	Density	Color	Wetness
	Тор	Loose	Gray	Wet
	Bottom	Spongy	Gray	Wet
Analysis:	Original ZnO ma	ass: m	=	5.4 g
•	Residual ZnO m	Ó		2.7 g
	ZnO retention %			50%
	Final-to-origina			
	ratio (%): $\eta = \frac{q}{\zeta}$			10% .
	, ,			

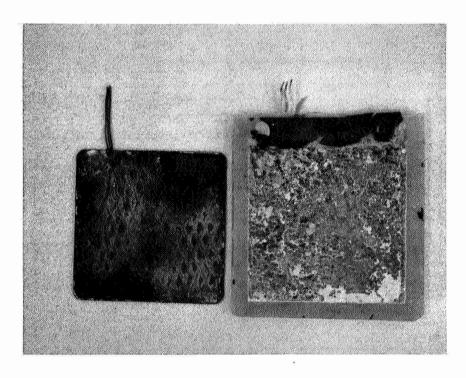


c5723

Figure B-15. Cell Number 421A

#### Cell No. 421A

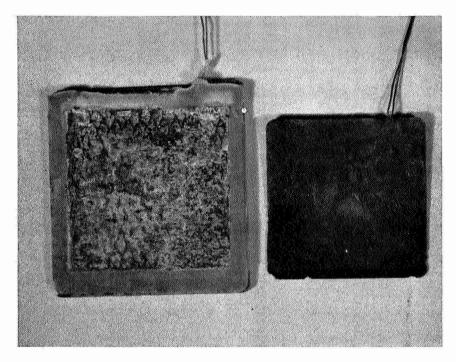
Regime 2	Combination 4			
Temperature: 25	Binder:		Z	
Period: 1.	5 hr.	Ratio:		90/10
Discharge: 0.	9 A for 0.5 hr.	Process	N	
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%): (	0
		Grid:	į	5 Ag 38-1/0
		Design:	(	(-) W
Original Capacity:	Q <sub>0</sub> =	2.2 Ah		
Last Capacity:		0.4 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	18%		
Failure Cycle:	N =	581		
Wet Life:	days =	114		
Inspection:	Separators: No cracks or delam., few stains signs of Zn pen.  Positive active area: p = N.A.  Negative shape retention: p = 80%  Zinc electrode condition: Good			
	Plate Location	Density	Color	Wetness
	Top	Loose	Gray	Semi-wet
	Bottom	Spongy	Gray	Semi-wet
Analysis: Original ZnO mass: m = 5.4				
	Residual ZnO mass: m = 4.0 g			
	ZnO retention %: $\zeta = \frac{m}{m_0} \times 100 = 74\%$			
	Final-to-original utilization			
	ratio (%): $\eta = \frac{q}{\zeta}$	x 100 =	7	24%



c5724

Figure B-16. Cell Number 431

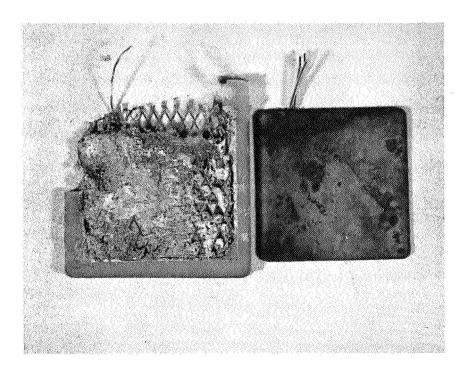
Regime 3	Con	Combination 4		
Temperature: 25	Binder:		Z	
Period: 24	hr.	Ratio:		90/10
Discharge: 1.	2 A for 1.2 hr.	Process:		N
Charge: 0.	07A for 22.8 hr.	Additive	(PbO%):	0
		Grid:		5 Ag 38-1/0
		Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	2.3 Ah		
Last Capacity:	_	1.5 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 = 0$	65%		
Failure Cycle:		52		
Wet Life:	days =	90		
Inspection:	Separators: No cracks or delam., dark blotchy stains, Zn pen. still gassing.  Positive active area: p = N.A.  Negative shape retention: p = 100%  Zinc electrode condition: Excellent			
	Plate Location	Density	Color	Wetness
	Тор	Hard	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO marker Residual ZnO marker ZnO retention % Final-to-original ratio (%): $\eta = \frac{q}{r}$	ass: $m = \frac{m}{m_0}$ $\therefore \zeta = \frac{m}{m_0}$ al utilizat	x 100 =	5.4 g 4.0 g 74%



c5725

Figure B-17. Cell Number 1311

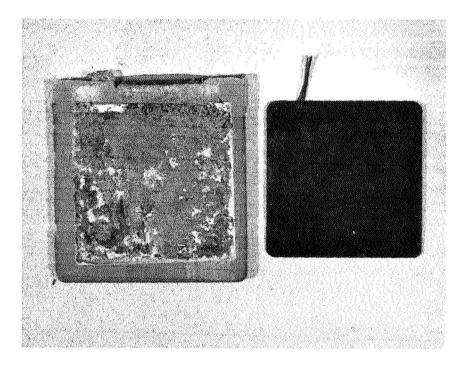
Regime 1	Combination 13			
Temperature: 1	00°C	Binder:		Z
Period: 1	hr.	Ratio:		90/10
Discharge: (	0.6 A for 0.5 hr.	Process	: 1	V
Charge: 0	0.66 A for 0.5 hr.	Additive	(PbO%):	1
		Grid:		5 Ag 14-1/0
		Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	2.0 Ah		
Last Capacity:	Q =	0.6 Ah		
Capacity Retention %	$= \frac{Q}{Q_0} \times 100 =$	33%		
Failure Cycle:	N =	373		
Wet Life:	days =	53		
Inspection:	Separators: One cracked, no delam., dark stains, signs of Zn pen.  Positive active area: p = 100%  Negative shape retention: p = 90%  Zinc electrode condition: Good			
	Plate Location	Density	Color	Wetness
	Тор	Spongy	Blue-Gray	Semi-wet
	Bottom	Spongy	Blue-Gray	Semi-wet
Analysis: Original ZnO mass: m <sub>0</sub> = 5.4				5.4 g
	Residual ZnO mass: $m = 3.2 g$			
	ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 =	59%
	Final-to-original utilization			
	ratio (%): $\eta = \frac{q}{\zeta} \times 100 =$			56%



¢5726

Figure B-18. Cell Number 1321

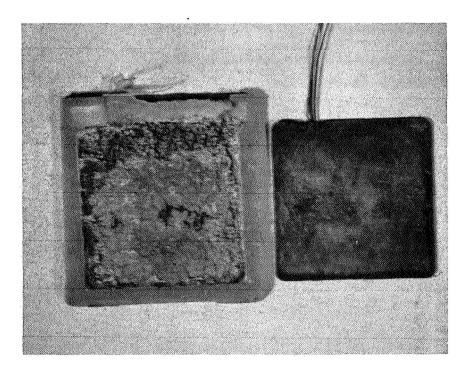
Regime 2	Combination 13			
Temperature: 25	°c	Binder:	<del> </del>	Z
Period: 1.	5 hr.	Ratio:		90/10
Discharge: 0.	9 A for 0.5 hr.	Process	·	N
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%):	1
		Grid:		5 Ag 14-1/0
		Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	2.1 Ah		angan ang ang ang ang ang ang ang ang an
Last Capacity:		0.4 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	19%		
Failure Cycle:		203		
Wet Life:	days =	41		
Inspection:	Separators: No signs of Zn pen.	cracks o	r delam.,	few stains,
	Positive active area: p <sup>+</sup> = N.A.			
	Negative shape	retention:	p = 80	%
	Zinc electrode condition: Good			ood
	Plate Location	Density	Color	Wetness
	Top	Spongy	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO m	ass: m		5.4 g
	Residual ZnO mass: m = 3.6 g			
	ZnO retention %: $\zeta = \frac{m}{m_0} \times 100 = 67\%$			
	Final-to-original utilization			
		atio (%): $\eta = \frac{q}{\zeta} \times 100 = 28\%$		



C5721

Figure B-19. Cell Number 1332

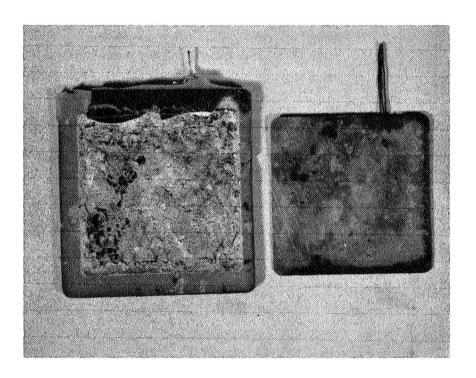
Regime 3			Con	nbination	13
Temperature: 25°C			Binder:		Z
Period:	24 hr.		Ratio:		90/10
Discharge:	1.2	A for 1.2 hr.	Process	3:	N
Charge:	0.0	7 A for 22.8 hr.	Additive	(PbO%):	1
			Grid:		5 Ag 14-1/0
			Design:		(-) W
Original Capacity:		Q <sub>0</sub> =	2.1 Ah	-	
Last Capacity:		Q =	1.2 Ah		
Capacity Retention	%:	$q = \frac{Q}{Q_0} \times 100 =$	57%		
Failure Cycle:		N =	17		
Wet Life:		days =	34		
Inspection:		Separators: No cracks or delam., few stains, signs of Zn pen.  Positive active area: p = N.A.  Negative shape retention: p = 100%  Zinc electrode condition: Excellent			
		Plate Location	Density	Color	Wetness
		Top	Hard	Dark Gra	y Semi-wet
		Bottom	Hard	Dark Gra	y Semi-wet
Analysis:		Original ZnO m Residual ZnO m ZnO retention % Final-to-origina ratio (%): $\eta = \frac{q}{\zeta}$	hass: $m = \frac{m}{m_0}$ al utilizat	x 100 =	5.4 g 3.9 g 72% 79%



c5728

Figure B-20. Cell Number 1411

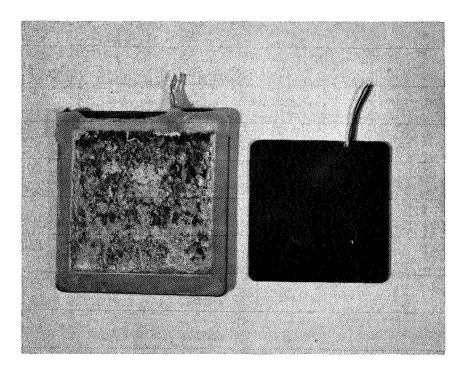
Regime 1	Con	Combination 14			
Temperature: 1	100°C	Binder:		Z	
Period: 1	l hr.	Ratio:	Ç	90/10	
Discharge: (	0.6 A for 0.5 hr.	Process	:: I	N	
Charge: 0	0.66 A for 0.5 hr.	Additive	(PbO%): 2	2	
		Grid:	į	5 Ag 14-1/0	
		Design:	.(	-) W	
Original Capacity:	Q <sub>o</sub> =	2.1 Ah			
Last Capacity:	Q =	0.6 Ah			
Capacity Retention %	$q = \frac{Q}{Q_0} \times 100 = 0$	35%			
Failure Cycle:	N =	373			
Wet Life:	days =	53			
Inspection:	spection: Separators: No cracks or delam., dark signs of Zn pen.				
		Positive active area: p = 100%			
	Negative shape	pe retention: p = 80 %			
	Zinc electrode	Zinc electrode condition: Good			
	Plate Location	Density	Color	Wetness	
	Тор	Spongy	Blue-Gray	Semi-wet	
	Bottom	Spongy	Blue-Gray	Semi-wet	
	• • • • • • • • • • • • • • • • • • •	· · · · · · · · · · · · · · · · · · ·	·	gally in the same and a sequence of the	
Analysis:	Original ZnO mass: $m_0 = 5.4 g$			5.4 g	
		Residual ZnO mass: m = 3.1 g			
	ZnO retention (	$\%: \zeta = \frac{m}{m_0}$	$\times$ 100 =	57%	
	Final-to-origin		ion		
	ratio (%): $\eta = \frac{c}{c}$	ratio (%): $\eta = \frac{q}{\zeta} \times 100 =$			



15729

Figure B-21. Cell Number 1422

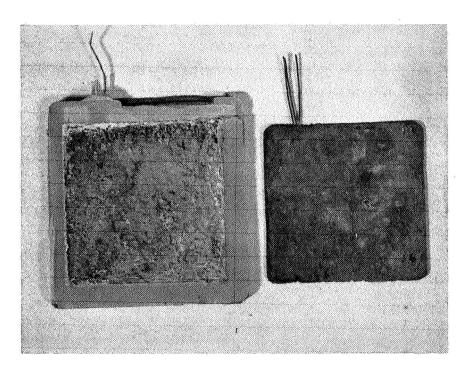
Regime 2	Combination 14			
Temperature: 25	°C	Binder:		Z
Period: 1.	5 hr.	Ratio:		90/10
Discharge: 0.	9 A for 0.5 hr.	Process	:	N
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%):	2
		Grid:		5 Ag 14-1/0
		Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	1.7 Ah	· · · · · · · · · · · · · · · · · · ·	
Last Capacity:	_	0.5 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	29%		
Failure Cycle:	:=	298		
Wet Life:	days =	53		
Inspection:	Separators: No cracks or delam., few stains, signs of Zn pen.  Positive active area: p = 100%  Negative shape retention: p = 90%  Zinc electrode condition: Good			
	Plate Location	Density	Color	Wetness
	Тор	Hard	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO m Residual ZnO m ZnO retention % Final-to-origina ratio (%): $\eta = \frac{q}{\zeta}$	lass: $m = \frac{m}{m_0}$ al utilizat	x 100 =	5.4 g 3.6 g 67% 43%



c5730

Figure B-22. Cell Number 1431

Regime 3	Combination 14			
Temperature: 25	°C	Binder:	2	<del>, , , , , , , , , , , , , , , , , , , </del>
Period: 24	hr.	Ratio:	ç	0/10
Discharge: 1.	2 A for 1.2 hr.	Process	:	1
Charge: 0.0	07 A for 22.8 hr.	Additive	(PbO%): 2	
		Grid:	.5	Ag 14-1/0
		Design:	(	-) W
Original Capacity:	Q <sub>0</sub> =	2.0 Ah		
Last Capacity:		1.1 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	61%		
Failure Cycle:		26		
Wet Life:	days =	53		
Inspection:	Separators: No signs of Zn pen.		r delam.,	few stains,
	Positive active	area: p <sup>+</sup>	= 1.00	%
	Negative shape	retention	p = 100	%
	Zinc electrode	condition:	Exc	ellent
	Plate Location	Density	Color	Wetness
	Тор	Hard	Blue-Gray	Semi-wet
	Bottom	Hard	Blue-Gray	Semi-wet
Analysis:	Original ZnO m	ass: mo	= !	5.4 g
	Residual ZnO mass: $m = 4.6 g$			4.6 g
	ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 = 8	35%
	Final-to-origina			
	ratio (%): $\eta = \frac{q}{r}$	ratio (%): $\eta = \frac{q}{R} \times 100 =$		



¢\$73/

Figure B-23. Cell Number 1512

Regime 1			Con	nbination	1.5	5
Temperature:	100	°C	Binder:		Z	
Period:	l h	r,	Ratio:		90	0/10
Discharge:	0.6	A for 0.5 hr.	Process	; <b>;</b>	P	S
Charge:	0.6	6 A for 0.5 hr.	Additive	(PbO%):	1	
			Grid:		5	Ag 14-1/0
			Design:		(-	) W
Original Capacity:		Q <sub>0</sub> =	2.3 Ah	***************************************		
Last Capacity:			0.8 Ah			
Capacity Retention	%:	$q = \frac{Q}{Q_0} \times 100 =$	35%			
Failure Cycle:		0	373			
Wet Life:		days =	53			
Inspection:	Separators: One cracked, no delam., dark stain, signs of Zn pen.			, dark		
		Positive active	area: p <sup>+</sup>	= 10	0%	)
		Negative shape	retention	p'' = 10	0%	)
		Zinc electrode	condition:	Go	ood	Į
		Plate Location	Density	Color		Wetness
		Top	Spongy	Blue-Gra	аy	Semi-wet
		Bottom	Spongy	Blue-Gra	аy	Semi-wet
Analysis:		Original ZnO m	_			. 4 g
		Residual ZnO m				, 3 g
		ZnO retention %	$\zeta : \zeta = \frac{m}{m_0}$	$\times$ 100 =	6.	1%
		Final-to-originario (%): $\eta = \frac{q}{\zeta}$		ion	5	7%

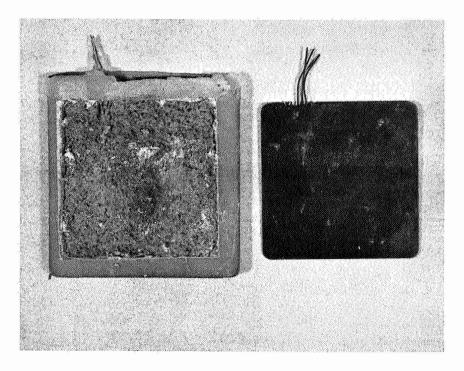


Figure B-24. Cell Number 1521

Regime 2			Combination 15		
Temperature: 2	25°C		Binder:		Z
<del>-</del>	.5 hr.	1	Ratio:		90/10
	).9 A for 0.	5 hr.	Process	:	PS
	.5 A for 1.0	1	Additive	(PbO%):	1
G			Grid:		5 Ag 14-1/0
			Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	2	2.2 Ah		
Last Capacity:	Q =		0.4 Ah		
Capacity Retention %	$q = \frac{Q}{Q_0} \times \frac{Q}{Q_0}$	100 =	18%		
Failure Cycle:	N = ~0		122		
Wet Life:	days =	Š	34		
Inspection:	signs of 2	Zn pen.			few stains,
	Positive				. A.
	Negative	_			0%
	Zinc elec	trode c	ondition:	Ez	ccellent
	Plate Lo	cation	Density	Color	Wetness
	Top		Hard	Gray	Semi-wet
	Botto	om	Hard	Gray	Semi-wet
Analysis:	Original	ZnO ma	ass: m		5.4 g
•	Residual		•	:	3.8 g
	ZnO rete	ZnO retention %: $\zeta = \frac{m}{m_0} \times 100 = 70\%$			
	Final-to-				
	ratio (%):	-			26%

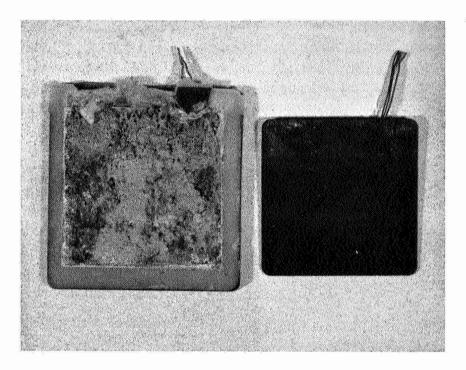


Figure B-25. Cell Number 1533

Regime 3			Con	nbination	15
Temperature:	25°	CC	Binder:		Z
Period:	24	hr.	Ratio:		90/10
Discharge:	1.2	A for 1.2 hr.	Process	:	PS
Charge:	0.0	7 A for 22.8 hr.	Additive	(PbO%):	1
			Grid:		5 Ag 14-1/0
			Design:		(-) W
Original Capacity:		Q <sub>0</sub> =	2.1 Ah		
Last Capacity:			1.2 Ah		
Capacity Retention	%:	$q = \frac{Q}{Q_0} \times 100 =$	57%		
Failure Cycle:			15		
Wet Life:		days =	34		
Inspection:		Separators: No cracks or delam., few stain signs of Zn pen.			
		Positive active	area: p <sup>+</sup>	= 10	0%
		Negative shape	retention:	$p^2 = 10$	0%
		Zinc electrode o	condition:	Ex	cellent
		Plate Location	Density	Color	Wetness
		Top	Hard	Gray	Semi-wet
		Bottom	Hard	Gray	Semi-wet
Analysis: Original ZnO ma			-	<del>=</del>	5.4 g 4.0 g
		Residual ZnO m			74%
m <sub>o</sub>				. 170	
		Final-to-original ratio (%): $\eta = \frac{q}{\zeta}$		TOU	77%

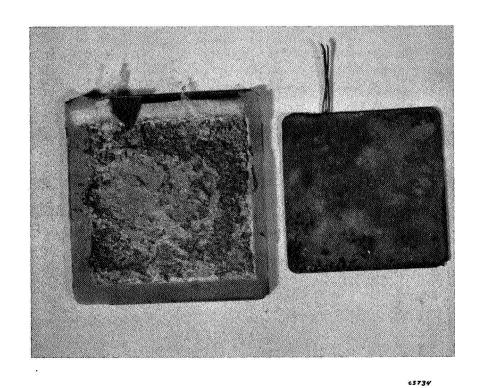


Figure B-26. Cell Number 1611

Regime 1	Combination 16			
Temperature: 10	00°C	Binder:	adinaming jajajanan di sepanj	Z
Period: 1	hr.	Ratio:		90/10
Discharge: 0.	.6 A for 0.5 hr.	Process	:	PS
Charge: 0.	.66 A for 0.5 hr.	Additive	(PbO%):	2
		Grid:		5 Ag 14-1/0
		Design:		(-) W
Original Capacity:	Q <sub>0</sub> =	2.1 Ah		
Last Capacity:	Q =	1.2 Ah		
Capacity Retention %	$= \frac{Q}{Q_0} \times 100 =$	57%		
Failure Cycle:	N = ~~	373		
Wet Life:	days =	49		
Inspection:	Separators: No cracks or delam., dark sta signs of Zn pen.  Positive active area: p = 100%  Negative shape retention: p = 90%  Zinc electrode condition: Good			
	Plate Location	Density	Color	Wetness
	Тор	Hard	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO m Residual ZnO m ZnO retention % Final-to-origina ratio (%): $\eta = \frac{q}{\zeta}$	hass: $m = \frac{m}{m_0}$ al utilizat	x 100 =	5.4 g 3.3 g 61%

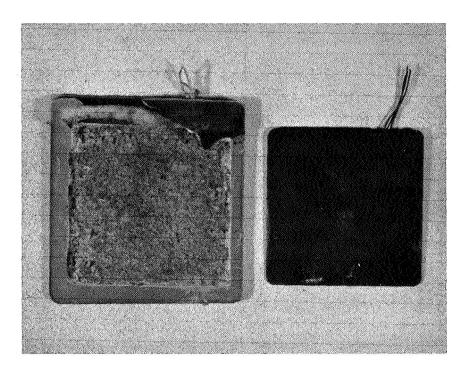
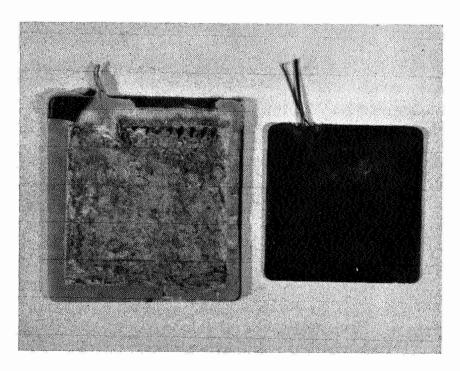


Figure B-27. Cell Number 1621

Regime 2	Con	abination 1	6	
Temperature: 25	°C	Binder:	2	Z
Period: 1.	5 hr.	Ratio:	9	0/10
Discharge: 0.	9 A for 0.5 hr.	Process	: I	PS
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%): 2	
		Grid:	5	Ag 14-1/0
		Design:	(	-) W
Original Capacity:	Q <sub>0</sub> =	2.1 Ah		
Last Capacity:	Q =	0.4 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	19%		
Failure Cycle:	N = ~~	124		
Wet Life:	days =	30		
Inspection:	Separators: No signs of Zn pen.		r delam.,	few stains,
	Positive active	area: p <sup>+</sup>	= N.A	٠.
	Negative shape	retention:	$p^- = 1000$	%
	Zinc electrode	condition:	Exc	ellent
	Plate Location	Density	Color	Wetness
	Top	Hard	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO m	ass: m	= 5	5.4 g
	Residual ZnO mass: $m = 3.6 g$			3.6 g
	ZnO retention %: $\zeta = \frac{m}{m_0} \times 100 = 67\%$			
	Final-to-origina			
	ratio (%): $\eta = \frac{q}{\zeta}$	x 100 =	2	28%



C5736

Figure B-28. Cell Number 1633

Regime 3		Combination 16		
Temperature: 25	°C	Binder:		Z
	hr.	Ratio:		90/10
•	2 A for 1.2 hr.	Process		PS
_				
Charge: 0.	07 A for 22.8 hr.		(PbO%):	
		Grid:		5 Ag 14-1/0
		Design:	<del></del>	(-) W
Original Capacity:	$Q_{o} =$	2.1 Ah		
Last Capacity:		1.2 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	57%		
Failure Cycle:		15		
Wet Life:	days =	30		
Inspection:	Separators: No cracks or delam., few stains, signs of Zn pen.			
	Positive active	area: p	= 10	0%
	Negative shape	retention:	p = 10	0%
	Zinc electrode o	ondition:	Ex	cellent
	Plate Location	Density	Color	Wetness
	Тор	Hard	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO m Residual ZnO m	ass: m =		5.4 g 4.2 g
	ZnO retention %: $\zeta = \frac{m}{m_0} \times 100 = 78\%$			
	Final-to-original utilization ratio (%): $\eta = \frac{q}{\zeta} \times 100 = 73\%$			

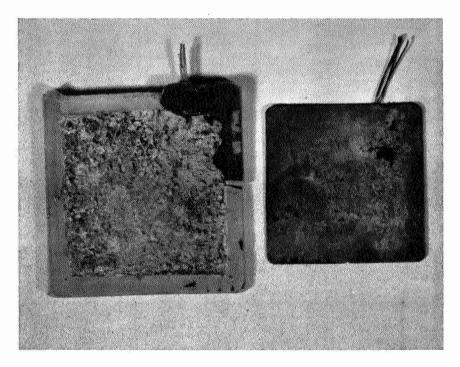


Figure B-29. Cell Number 1711

Regime 1		Combination 17		
Temperature: 10	00°C	Binder:		Z
Period: 1	hr.	Ratio:		80/20
Discharge: 0.	6 A for 0.5 hr.	Process	:	N
Charge: 0.	66 A for 0.5 hr.	Additive	(PbO%):	1
		Grid:		5 Ag 14-1/0
		Design:		(-) W
Original Capacity:	Q <sub>o</sub> =	2.0 Ah		
Last Capacity:	Q =	1.3 Ah		
Capacity Retention $\%$ :	$q = \frac{Q}{Q_0} \times 100 =$	65%		
Failure Cycle:	N =	266		
Wet Life:	days =	47		
Inspection:	Separators: No signs of Zn pen.		r delam.,	some stains
	Positive active	area: p <sup>+</sup>	= 100	1%
	Negative shape	retention	p = 90%	<b>%</b>
	Zinc electrode	condition:	Go	bo
	Plate Location	Density	Color	Wetness
	Тор	Spongy	Blue-Gray	Semi-wet
	Bottom	Spongy	Blue-Gray	Semi-wet
Analysis:	Original ZnO m	•		4.8 g
	Residual ZnO mass: m = 2.7 g			
	ZnO retention %	$ \zeta = \frac{m}{m_0} $	$\times$ 100 =	56%
	Final-to-origina		ion	
	ratio (%): $\eta = \frac{q}{\zeta}$	x 100 =		100%

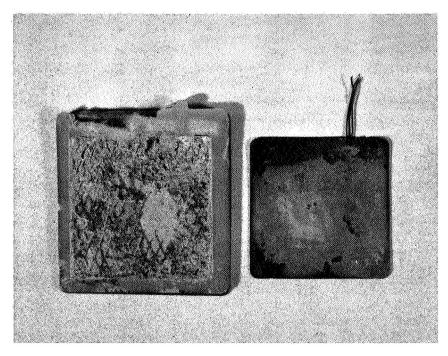


Figure B-30. Cell Number 1722

Regime 2		Con	nbination	17	
Temperature: 2	25°C	Binder:		Z	
	.5 hr.	Ratio:	4	80/20	
Discharge:	0.9 A for 0.5 hr.	Process	`. \$	N	
Charge:	0.5 A for 1.0 hr.	Additive	(PbO%):	l	
		Grid:		5 Ag 14-1/0	
	<u> </u>	Design:		(-) W	
Original Capacity:	Q <sub>0</sub> =	2.2 Ah			
Last Capacity:	Q =	0.4 Ah			
Capacity Retention %	$q = \frac{Q}{Q_0} \times 100 =$	18%			
Failure Cycle:	N = ~0	170			
Wet Life:	days =	47			
Inspection:	signs of Zn pen. Positive active Negative shape	Separators: No cracks or delam., few stains, signs of Zn pen.  Positive active area: p <sup>+</sup> = N.A.  Negative shape retention: p <sup>-</sup> = 80%  Zinc electrode condition: Good			
	Plate Location	Density	Color	Wetness	
	Тор	Spongy	Blue-Gray	Semi-wet	
	Bottom	Hard	Blue-Gray	Semi-wet	
Analysis:	Original ZnO m Residual ZnO m ZnO retention $\%$ Final-to-origin ratio (%): $\eta = \frac{q}{\zeta}$	hass: $m = \frac{m}{m_0}$ al utilizat	x 100 =	4.8 g 2.8 g 58%	

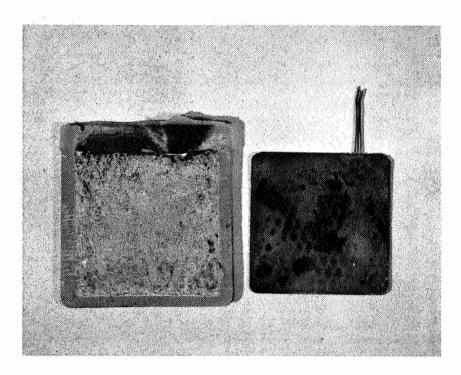


Figure B-31. Cell Number 1731

Cell No. 1731

Regime 3		Combination	17
Temperature:	25°C	Binder:	Z
Period:	24 hr.	Ratio:	80/20
Discharge:	1.2 A for 1.2 hr.	Process:	N
Charge:	0.07 A for 22.8 hr.	Additive (PbO%):	1
		Grid:	5 Ag 14-1/0
		Design:	(-) W
Original Capacity:	Q <sub>0</sub> =	2.0 Ah	
Last Capacity:	Q =	1.3 Ah	
Capacity Retention	%: $q = \frac{Q}{Q} \times 100 =$	65%	
Failure Cycle:	N =	15	
Wet Life:	days =	47	
		*	1-1

Inspection:

Separators: One minute crack, no delam., few stains, signs of Zn pen.

Positive active area: p = = 100%

Negative shape retention: p = 100%

Zinc electrode condition: Excellent

Plate Location	Density	Color	Wetness
Тор	Hard	Blue-Gray	Semi-wet
Bottom	Hard	Blue-Gray	Semi-wet

Analysis:

Original ZnO mass: m = 4.8 g

3.7 g Residual ZnO mass: m =

ZnO retention %:  $\zeta = \frac{m}{m_0} \times 100 =$ 77%

Final-to-original utilization

ratio (%):  $\eta = \frac{q}{\zeta} \times 100 =$ 84%

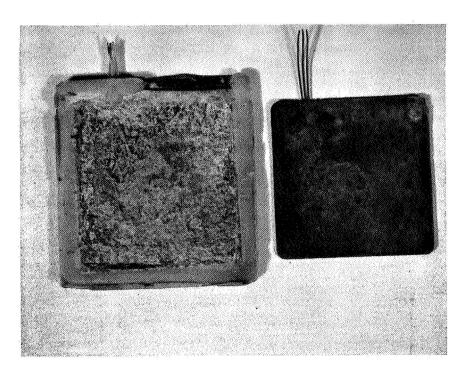


Figure B-32. Cell Number 1811

Cell No. 1811

Regime 1		Combination	18		
Temperature:	100°C	Binder:	Z		
Period:	l hr.	Ratio:	80/20		
Discharge:	0.6 A for 0.5 hr.	Process:	·N		
Charge:	0.66 A for 0.5 hr.	Additive (PbO%):	2		
		Grid:	5 Ag 14-1/0		
		Design:	(-) W		
Original Capacity:	Q <sub>o</sub> =	1.8 Ah			
Last Capacity:	Q =	1.0 Ah			
Capacity Retention	$q = \frac{Q}{Q_0} \times 100 =$	56%			
Failure Cycle:	N =	266			
Wet Life:	days =	47			
Inspection:	Separators: No signs of Zn per	cracks or delam.	, some stain		
	Positive active	Positive active area: p <sup>+</sup> = 100%			
	Negative shape	retention: n = 90	)%		

Positive active area:  $p^{T} = 100\%$ Negative shape retention:  $p^{T} = 90\%$ Zinc electrode condition: Good

Plate Location	Density	Color	Wetness
Top	Spongy	Gray	Semi-wet
Bottom	Spongy	Gray	Semi-wet

Analysis: Original ZnO mass:  $m_0 = 4.8 \text{ g}$ Residual ZnO mass: m = 2.7 gZnO retention %:  $\zeta = \frac{m}{m_0} \times 100 = 56\%$ Final-to-original utilization
ratio (%):  $\eta = \frac{q}{\zeta} \times 100 = 100\%$ 

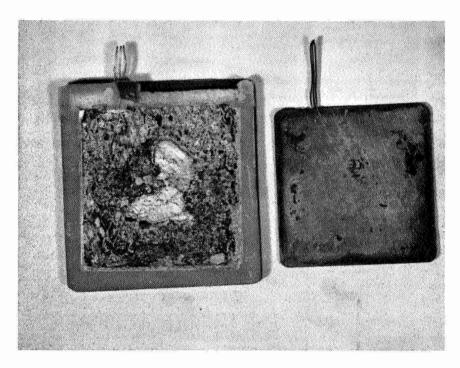


Figure B-33. Cell Number 1822

Cell No. 1022					
Regime 2		Con	nbination	18	
Temperature: 25	Temperature: 25°C			Z	
Period: 1.	5 hr.	Ratio:		80/20	
Discharge: 0.	9 A for 0.5 hr.	Process	:	N	
Charge: 0.	5 A for 1.0 hr.	Additive	(PbO%):	2	
		Grid:		5 Ag 14-1/0	
		Design:		(-) W	
Original Capacity:	Q <sub>o</sub> =	1.8 Ah			
Last Capacity:		0.5 Ah			
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 =$	28%			
Failure Cycle:	• •	172			
Wet Life:	days =	47			
Inspection:	Separators: No cracks or delam., few stains, signs of Zn pen.				
	Positive active area: p <sup>+</sup> = 100%				
	Negative shape	retention:	$p^{-} = 75$	%	
	Zinc electrode	condition:	Fa	iir	
	Plate Location	Density	Color	Wetness	
	Тор	Spongy	Gray	Semi-wet	
	Bottom	Hard	Gray	Semi-wet	
Analysis:	Original ZnO m	ass: m	=	4.8 g	
	Residual ZnO mass: $m = 3.0 g$				
	ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 =	62%	
	Final-to-origina	al utilizat			
	ratio (%): $\eta = \frac{q}{\xi}$	$\times$ 100 =		45%	

Cell No. 1831

Regime 3		Combination	18
Temperature:	25°C	Binder:	Z
Period:	24 hr.	Ratio:	80/20
Discharge:	1.2 A for 1.2 hr.	Process:	N
Charge:	0.07 A for 22.8 hr	Additive (PbO%):	2
		Grid:	5 Ag 14-1/0
		Design:	(-) W
Original Capacity:	Q <sub>0</sub> =	1.8 Ah	
Last Capacity:	Q =	1.3 Ah	
Capacity Retention	$\%: q = \frac{Q}{Q_0} \times 100 =$	72%	
Failure Cycle:	N =	14	
Wet Life:	days =	47	

Inspection:

Separators: No cracks or delam., few stains.

Positive active area: p = 100% Negative shape retention: p = 80% Zinc electrode condition: Good

Plate Location	Density	Color	Wetness
Тор	Spongy	Blue-Gray	Semi-wet
Bottom	Hard	Blue-Gray	Semi-wet

Analysis:

Original ZnO mass:  $m_0 = 4.8 g$ Residual ZnO mass: m = 3.9 gZnO retention %:  $\zeta = \frac{m}{m_0} \times 100 = 81\%$ Final-to-original utilization

ratio (%):  $\eta = \frac{q}{\zeta} \times 100 = 89\%$ 

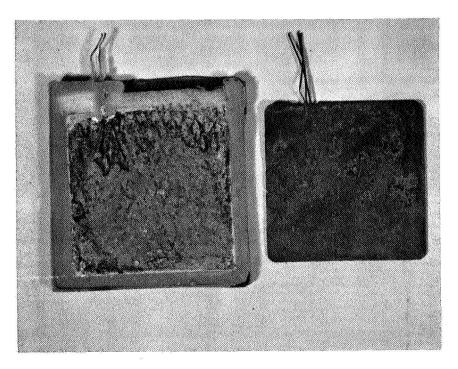


Figure B-35. Cell Number 1912

Regime 1			Combination 19			
Temperature:	100	)°C	Binder:		Z	
Period:	1 h	r.	Ratio:		80/20	
Discharge:	0.6	A for 0.5 hr.	Process	) <b>:</b>	PS	
Charge:	0.6	66 A for 0.5 hr.	Additive	(PbO%):	1	
			Grid:		5 Ag 14-1/0	
			Design:		(-) W	
Original Capacity:	······································	Q <sub>0</sub> =	2.3 Ah			
Last Capacity:		Q =	0.6 Ah			
Capacity Retention	%:	$q = \frac{Q}{Q_0} \times 100 =$	38%			
Failure Cycle:		N =	266			
Wet Life:		days =	47			
Inspection:		Separators: Both cracked near edge, no delam some stains, signs of Zn pen.				
		Positive active area: p <sup>+</sup> = 100%				
		Negative shape retention: p = 100%				
		Zinc electrode	condition:	God	od	
		Plate Location	Density	Color	Wetness	
		Тор	Spongy	Blue-Gray	y Semi-wet	
		Bottom	Spongy	Blue-Gray	y Semi-wet	
Analysis:		Original ZnO m	ass: m		4.8 g	
		Residual ZnO mass: m =			2.6 g	
		ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 =	54%	
		Final-to-originario (%): $\eta = \frac{q}{\zeta}$	al utilizat	ion	70%	

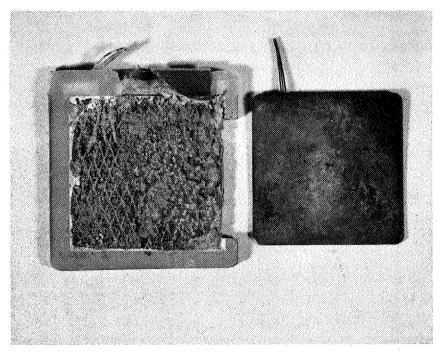


Figure B-36. Cell Number 1923

Regime 2		Con	nbination l	9
Temperature: 25	Binder:	Z		
Period: 1.	5 hr.	Ratio:	8	0/20
Discharge: 0.	9 A for 0.5 hr.	Process	: F	PS
Charge: 0.		Additive	(PbO%): 1	
-		Grid:	5	Ag 14-1/0
		Design:	(.	-) W
Original Capacity:	Q <sub>0</sub> =	2.3 Ah		
Last Capacity:	_	0.5 Ah		
Capacity Retention %	$= \frac{Q}{Q_0} \times 100 =$	22%		
Failure Cycle:		105		
Wet Life:	days =	40		
Inspection: Separators: No cracks or delam., few starsigns of Zn pen.				few stains,
	Positive active	area: p <sup>+</sup>	= N.A	•
	Negative shape			
	Zinc electrode	condition:	Goo	d
	Plate Location	Density	Color	Wetness
	Top	Hard	Gray	Semi-wet
	Bottom	Hard	Gray	Semi-wet
Analysis:	Original ZnO m Residual ZnO n ZnO retention %	hass: $m = \frac{m}{m_0}$	x 100 = 6	4.8 g 3.1 g 55%
	Final-to-origin ratio (%): $\eta = \frac{q}{\zeta}$			34%

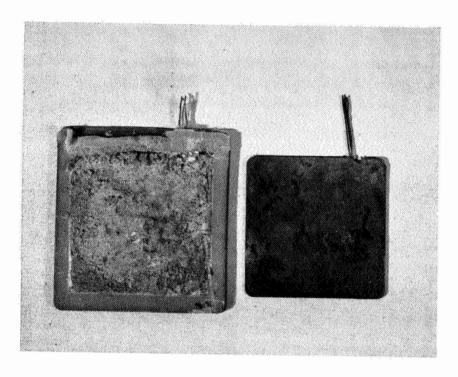


Figure B-37. Cell Number 1931

Regime 3			Combination 19		
Temperature:	25°(	C	Binder:		Z
Period:	24 h	ır.	Ratio:	;	80/20
Discharge:	1.2	A for 1.2 hr.	Process	:	PS
Charge:	0.0	7 A for 22.8hr.	Additive	(PbO%):	1
			Grid:	;	5 Ag 14-1/0
			Design:	(	(-) W
Original Capacity:		Q <sub>0</sub> =	2.3 Ah		
Last Capacity:		•	1.2 Ah		
Capacity Retention	%:	$q = \frac{Q}{Q_0} \times 100 =$	52%		
Failure Cycle:		, -0	14		
Wet Life:		days =	47		
Inspection: Separators: No crassigns of Zn pen.				r delam.,	few stains,
		Positive active	area: p <sup>+</sup>	= 100	%
		Negative shape	retention	p = 100	1%
		Zinc electrode	condition:	Exc	cellent
		Plate Location	Density	Color	Wetness
		Тор	Hard	Blue-Gra	y Semi-wet
		Bottom	Hard	Blue-Gra	y Semi-wet
Analysis:		Original ZnO m	ass: m	-	4.8 g
		Residual ZnO m			4.0 g
		ZnO retention %	$\zeta = \frac{m}{mc}$	x 100 =	83%
		Final-to-origin			
		ratio (%): $\eta = \frac{q}{\zeta}$	x 100 =		63%

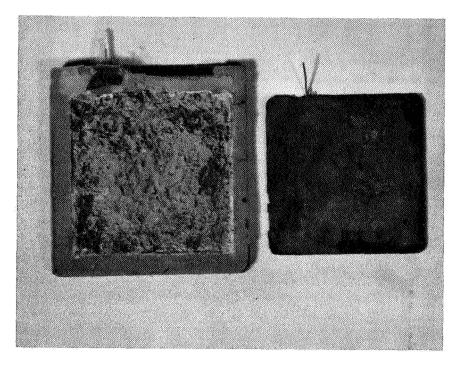


Figure B-38. Cell Number 2011

#### Cell No. 2011

Regime 1		Combination 20		
Temperature:	100°C	Binder:	Z	
Period:	l hr.	Ratio:	80/20	
Discharge:	0.6 A for 0.5 hr.	Process:	PS	
Charge:	0.66 A for 0.5 hr	Additive (PbO%):	2	
		Grid:	5 Ag 14-1/0	
		Design:	(-) W	
Original Capacity:	Q <sub>0</sub> =	2.2 Ah		
Last Capacity:	Q =	0.7 Ah		
Capacity Retention	%: $q = \frac{Q}{Q_0} \times 100 =$	32%		
Failure Cycle:	N =	266		
Wet Life:	days =	47		
Inspection:	Separators: F	Both cracked near ed	lge, no delam	

Separators: Both cracked near edge, some stains, signs of Zn pen.

Positive active area: p+= 100% Negative shape retention: p = 100%

Zinc electrode condition: Good

Plate Location	Density	Color	Wetness
Top	Spongy	Blue-Gray	Semi-wet
Bottom	Spongy	Blue-Gray	Semi-wet

Analysis:

Original ZnO mass: m<sub>o</sub> = 4.8 g

2.6 g Residual ZnO mass: m =

ZnO retention %:  $\zeta = \frac{m}{m_0} \times 100 =$ 54%

Final-to-original utilization

ratio (%):  $\eta = \frac{q}{\zeta} \times 100 =$ 59%

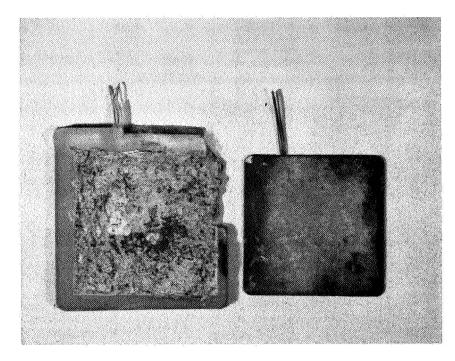


Figure B-39. Cell Number 2022

Regime 2		Con	nbination 2	0
Temperature: 25°	Temperature: 25°C			······································
	hr.	Ratio:	8	0/20
Discharge: 0.9	A for 0.5 hr.	Process	: F	PS
Charge: 0.5	6 A for 1.0 hr.	Additive	(PbO%): 2	
		Grid:	5	Ag 14-1/0
		Design:	.(	-) W
Original Capacity:	$Q_{o} = 2$	2.3 Ah		
Last Capacity:		0.4 Ah		
Capacity Retention %:	$q = \frac{Q}{Q_0} \times 100 = 1$	17%		
Failure Cycle:	N =	169		
Wet Life:	days =	17		
Inspection:	Separators: No signs of Zn pen.	cracks o	r delam.,	few stains,
	Positive active	area: p <sup>+</sup>	= N.A	•
	Negative shape	retention	p = 90%	
	Zinc electrode o	ondition:	Goo	d
	Plate Location	Density	Color	Wetness
	Тор	Spongy	Blue-Gray	Semi-wet
	Bottom	Hard	Blue-Gray	Semi-wet
				_
Analysis:	Original ZnO m	U		. 8 g
	Residual ZnO m	***		.6 g
	ZnO retention %	0		4%
	Final-to-origina			
	ratio (%): $\eta = \frac{q}{\xi}$	$\times$ 100 =	3	1%

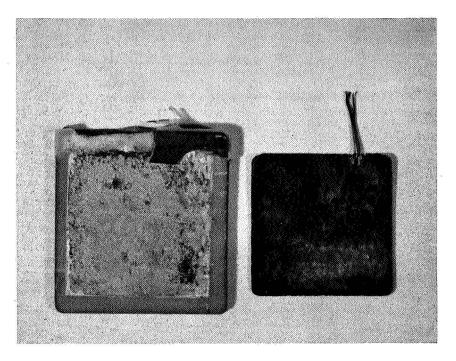


Figure B-40. Cell Number 2032

Regime 3	Combination 20			
Temperature:	25°C	Binder:		Z
Period:	24 hr.	Ratio:	80	0/20
Discharge:	1.2 A for 1.2 hr.	Process	: P	S
Charge:	0.07 A for 22.8 hr.	Additive	(PbO%): 2	
		Grid:	5	Ag 14-1/0
		Design:	(-	) W
Original Capacity:	Q <sub>o</sub> =	2.2 Ah		
Last Capacity:	Q =	1.1 Ah		
Capacity Retention	$\%: q = \frac{Q}{Q_0} \times 100 =$	50%		
Failure Cycle:	N =	14		
Wet Life:	days =	47		
Inspection:	Separators: On stains, some Z		crack, no d	elam., few
	Positive active	area: p <sup>+</sup>	= 100%	0
	Negative shape	retention	p = 100%	o
	Zinc electrode	condition:	Exce	ellent
	Plate Location	Density	Color	Wetness
	Top	Spongy	Blue-Gray	Semi-wet
	Bottom	Spongy	Blue-Gray	Semi-wet
Analysis:	Original ZnO m Residual ZnO n	U		.8g
	ZnO retention %	$\zeta = \frac{m}{m_0}$	x 100 = 7	9%
	Final-to-origin	Ÿ		
	ratio (%): $\eta = \frac{q}{\zeta}$	× 100 =	6	3%

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